児

ROCKET RÉSEARCH CORPORATION

(PAGES)

(PAGES)

(PAGES)

(CATEGORY)

(CATEGORY)

Seattle, Washington

Reproduced by
NATIONAL TECHNICAL
INFORMATION SERVICE
U.S. Department of Commerce
Springfield VA 22151

162/1.

DEVELOPMENT OF DESIGN AND SCALING CRITERIA FOR MONOPROPELLANT HYDRAZINE REACTORS EMPLOYING SHELL 405 SPONTANEOUS CATALYST RRC -66-R-76 - Volume 1

Final Report Prepared under NASA Contract NAS 7-372

Submitted To:

NASA Western Operations Office Santa Monica, California

Ву

Rocket Research Corporation Seattle, Washington

Approved by:

B. W. Schmitz, Project Manager

W. W. Smith, Manager Hydrazine Programs

NATIONAL TECHNICAL INFORMATION SERVICE
U.S. DEPARTMENT OF COMMERCE SPRINGFIELD, VA. 22161

January 19, 1967

	-		

TABLE OF CONTENTS

			Page
	SUMMARY		
1.0	INTRODUCTIO	٧	1
2.0	CONTRACT SC	OPE OF WORK	3
	2.1 General		3
-	2.2 Phase I		3
	2.3 Phase II		5
3.0	TEST PLAN	<u>.</u>	7
	3.1 General		7
	3.2 Phase I Te	st Plan	. 7
4.0	REACTOR DESIG	9N	. 11
	4.1 Injector C	Optimization Tests	11
	4.2 Catalyst B	ed Parameter Studies	18
5.0	TEST APPARATU	S AND TEST PROCEDURES	33
	5.1 Propellant	Supply System	33
	5.2 Thrust Star	nd	33
	5.3 Instrument	ation	33
	5.4 Test Proce	dures	45
6.0	INJECTOR OPT	MIZATION TEST RESULTS	49
	6.1 Data Redu	ction Techniques	49
	6.2 Test Resul	rts	51
	6.3 Summary of	of Injector Optimization Testing	106
7.0	CATALYST BED	DESIGN PARAMETER STUDIES	111
	7.1 Test Cond	tions Studied	111
	7.2 Test Resul	rs	111
	7.3 Summary of	of Test Data	123
8.0	CATALYST DEG	RADATION MEASUREMENTS	139
9.0	100 lbf ENGINE		143
	9.1 Design		143
	9.2 Test Resul	rs	143
0.0	FLIGHTWEIGHT	5 lbf ENGINE	151
	10.1 Design		151
	10.2 Low Freez	ing Point Propellant Mixture Tests	158

LIST OF FIGURES

Figure Number		Page
1	5 lbf Thrust Engine Showerhead Injector Test Matrix	8
2	Typical Test Matrix for Bed Loading, Chamber Pressure, and Bed Length Tests	10
3	Cross-Sectional View 0.5 lbf Engine	12
4	Cross-Sectional View 5 lbf Engine	13
5	Cross-Sectional View 50 lbf Engine	14
6	50 lbf Engine Rigimesh and Showerhead Injector Plates	20
7	Test Set – 50 lbf Hydrazine Reactor – RRC Drawing 24199, (2 Sheets)	21
8	Test Bed – Rocket Motor – RRC Drawing 24671	27
9	0.5 lbf Engine Assembly	31
10	Test Cell Schematic	34
11	Thrust Stand Assembly – .5 lbf Hydrazine Reactor, RRC Drawing 24233, (3 Sheets)	35
12	Test Installation & Flexure Assembly - 50 lbf Rocket Engine RRC Drawing 24255, (2 Sheets)	41
13	Data Recording System	46
14	0.5 lbf Engine Showerhead Injector Scatter Diagram	54
15	0.5 lbf Engine Showerhead Injector Average Cold Bed Response Time vs. Injector Pressure Drop	55
16	0.5 lbf Engine Showerhead Injector Average Ignition Delay vs. Injector Pressure Drop	56
17	0.5 lbf Engine Showerhead Injector Average Chamber Pressure Roughness vs. Injector Pressure Drop	57
18	0.5 lbf Engine Rigimesh Injector Scatter Diagram	58
19	0.5 lbf Engine Rigimesh Injector Average Cold Bed Response Time vs. Injector Pressure Drop	59
20	5 lbf Engine Showerhead Injector Scatter Diagram Cold Bed Response Time	65
21	5 lbf Engine Showerhead Injector Scatter Diagram Decay Time	66
22	5 lbf Engine Showerhead Injector Scatter Diagram Ignition Delay	67
23	5 lbf Engine Showerhead Injector Scatter Diagram Chamber	68

LIST OF FIGURES (Cont'd)

Figure Number		Page
24	5 lbf Engine Showerhead Injector Average Cold Bed Response Time vs. Injector Pressure Drop	72
25	5 Ibf Engine Showerhead Injector Average Cold Bed Response vs. Distance from Catalyst Bed	73
26	5 lbf Engine Showerhead Injector Average Cold Bed Response Time vs. Number of Orifices	74
27	5 lbf Engine Showerhead Injector Average Ignition Delay vs. Number of Orifices	76
28	5 Ibf Engine Showerhead Injector Average Ignition Delay vs. Distance from Catalyst Bed	77
29	5 Ibf Engine Showerhead Injector Average Chamber Pressure Decay Time vs. Number of Orifices	78
30	5 lbf Engine Rigimesh Injector Scatter Diagram Cold Bed Response Time	81
31	5 lbf Engine Rigimesh Injector Scatter Diagram Ignition Delay	82
32	5 lbf Engine Rigimesh Injector Scatter Diagram Decay Time	83
33	5 lbf Engine Rigimesh Injector Scatter Diagram Chamber Pressure Roughness	84
34	5 lbf Engine Rigimesh Injector Cold Bed Response Time vs. Injector Pressure Drop	85
35	50 lbf Engine Showerhead Injector Scatter Diagram Cold Bed Response Time	90
36	50 lbf Engine Showerhead Injector Scatter Diagram Chamber Pressure Roughness	91
37	50 lbf Engine Showerhead Injector Scatter Diagram Ignition Delay	92
38	50 lbf Engine Showerhead Injector Scatter Diagram	93
39	50 lbf Engine Showerhead Injector Cold Bed Response Data vs. Injector Pressure Drop	94
40	50 lbf Engine Showerhead Injector Cold Bed Response Time vs. Injector Pressure Drop	95
41	50 lbf Engine Showerhead Injector Chamber Pressure Roughness vs. Injector Pressure Drop	96
42	50 lbf Engine 60 Hole Showerhead Injector Chamber Pressure Roughness vs. Injector Pressure Drop	97

LIST OF FIGURES (Cont'd)

Figure Number		Page
43	50 lbf Engine Rigimesh Injector Scatter Diagram Cold Bed Response Time	100
44	50 lbf Engine Rigimesh Injector Scatter Diagram Ignition Delay	101
45	50 lbf Engine Rigimesh Injector Scatter Diagram Decay Time	102
46	50 lbf Engine Rigimesh Injector Scatter Diagram Chamber Pressure Roughness	103
47	50 lbf Engine Rigimesh Injector Average Cold Bed Response Time vs. Injector Pressure Drop	104
48	0.5 Ibf Engine Test Matrix for Bed Loading, Chamber Pressure, and Bed Length Studies	112
49	5 Ibf Engine Test Matrix for Bed Loading, Chamber Pressure, and Bed Length Studies	113
50	50 lbf Engine Test Matrix for Bed Loading, Chamber Pressure, and Bed Length Studies	114
51	Corrected Characteristic Velocity vs. Ammonia Dissociation for 5 lbf Engine	117
52	Sea Level Thrust Coefficient vs. Chamber Pressure for 5 lbf Engine	118
53	Corrected Characteristic Velocity vs. Ammonia Dissociation for 50 lbf Engine	124
54	Sea Level Thrust Coefficient vs. Chamber Pressure for = 2.0:1 50 lbf Engine	125
55	Corrected Characteristic Velocity vs. Ammonia Dissociation for 0.5 lbf Engine	126
56	Sea Level Thrust Coefficient vs. Chamber Pressure for = 20:1 0.5 lbf Engine	127
57	Correlation of Ammonia Dissociation Data for a Diffusion Controlled Reaction	132
58	General Correlation of Ammonia Dissociation Data	134
59	Correlation of Catalyst Bed Length Requirements	135
60	Correlation of Catalyst Bed Pressure Drop Data with Grant's Equation	13 <i>7</i>
61	Rocket Engine – 100 lbf Hydrazine, Showerhead Injector	145
62	100 lbf Monopropellant Hydrazine Engine	147

LIST OF FIGURES (Cont'd)

Figure Number		Page
63	Reactor Assembly – 5 lbf Flightweight – RRC Drawing 24600 (2 Sheets)	153
64	5.0 lbf Flightweight Engine Assembly	159
65	Performance of Ternary Propellant Mixtures	160
66	Hydrazine–Hydrazine Nitrate–Water Ternary Diagram Showing Freezing Point and Vacuum Specific Impulse	161
67	Ignition Delay Time vs. Propellant Freezing Point for 5 lbf Flightweight Engine	164
68	Chamber Pressure Roughness vs. Propellant Freezing Point for 5 lbf Flightweight Engine	165

LIST OF TABLES

Table Number		Page
I	Task I – Engine Design Summary	15
11	Showerhead Injector Design Summary	1 <i>7</i>
#1	Rigimesh Injector Design Summary	19
IV	0.5 lbf Engine - Test Data Summary - Showerhead Injector	52
Ÿ	0.5 lbf Engine – Test Data Summary – Rigimesh Injector	60
VI	5 lbf Engine – Test Data Summary – Showerhead Injector	69
VII	5 lbf Engine – Test Data Summary – Rigimesh Injector	86
VIII	Summary of 50 lbf Engine Catalyst Particle Size Studies	88
IX	50 lbf Engine – Test Data Summary – Showerhead Injector	98
X	50 lbf Engine – Test Data Summary – Rigimesh Injector	105
XI	Instrumentation List for Reactor Design Parameter Studies	115
XII	Summary of 5 lbf Engine Catalyst Particle Size Studies	119
XIII	Summary of 1.205 Diameter Reactor Bed Loading, Chamber Pressure, and Bed Length Tests	120
XIV	Summary of 3.010 Diameter Reactor Bed Loading, Chamber Pressure, and Bed Length Tests	128
XV	Summary of 0.5 lbf Engine Bed Loading, Chamber Pressure, and Bed Length Studies	129
ΧVI	Catalyst Surface Area Changes	141
XVII	100 lbf Engine Design Parameters	148
XVIII	Summary of 100 lbf Engine Test Data	149
XIX	5 lbf Flightweight Engine Design	157
XX	Low Freezing Point Propellant Mixtures	162
XXI	Summary of 5 lbf Flightweight Engine Propellant Mixture Tests	166

SUMMARY

Under NASA Contract NAS 7-372, issued by NASA OART and technically directed by the Jet Propulsion Laboratory, Rocket Research Corporation, Seattle, Washington, undertook a program for development of design and scaling criteria for monopropellant hydrazine reactors employing Shell 405 spontaneous catalyst. The contract effort was initiated April 17, 1965. This document represents the final report on Contract NAS 7-372 and is contained in two volumes; Volume I presents the contract scope of work, test plan, engine design employed and summarizes the test data obtained; Volume II presents the correlation of the test data into design and scaling formulae and represents a design manual for monopropellant hydrazine reactors employing the Shell 405 catalyst.

Initial tests on the program were conducted to determine the effects of injector parameters on engine operation. A showerhead injector and a rigimesh injector were evaluated. Injector pressure drop, propellant mass distribution onto the catalyst bed, and injector height from the catalyst bed were varied in a systematic manner. Tests were carried out at thrust levels of 0.5, 5, and 50 lbf. The results indicate that the showerhead injector is superior to the rigimesh injector on the basis of smoother operation.

With the showerhead injector it was found that smooth start transients and steady state operation could be obtained with low pressure drop injectors. As a design guideline the injector pressure drop can be held at 10 to 20% of chamber pressure. Reactor operation was rather insensitive to the number of injector orifices (propellant mass distribution onto the catalyst bed) but it does appear that approximately 6 orifices per square inch of catalyst bed cross-sectional area results in optimum performance. Under certain conditions smooth operation could be obtained with the injector away from the catalyst bed, but better overall performance was obtained with the injector flush with the top of the catalyst bed.

During initial engine testing, large chamber pressure oscillations were encountered. It was found that these oscillations could be reduced and/or eliminated through the use of a layer of fine mesh catalyst on the top of the catalyst bed. This provides higher catalyst surface area per unit volume of catalyst and apparently stabilizes the flame front near the top of the catalyst bed on ignition.

Subsequent testing on the program investigated the effects of reactor design parameters on engine operation and performance. Chamber pressure was varied from 50 to 1,000 psia,

bed loading from 0.01 to 0.045 lbm/in²-sec, and catalyst bed length from that required for satisfactory (smooth) engine performance to a value which resulted in approximately 85% ammonia dissociation. Tests were carried out at thrust levels of 0.5, 5, and 50 lbf. This data, correlated with theoretical models of reactor operation, served as a basis for development of design and scaling formulae for monopropellant hydrazine reactors. Equations and design criteria were developed to define catalyst bed configuration, ammonia dissociation, catalyst bed pressure drop, and chamber pressure rise time as a function of the reactor design parameters.

The design and scaling criteria developed at the 0.5 to 50 lbf thrust level were used to design a 100 lbf engine. This engine was fabricated and tested to demonstrate the applicability of the scaling formula to higher thrust levels. Performance of this engine was as predicted by the scaling criteria and demonstrated the validity of the design and scaling criteria over a 200:1 thrust range.

A 5 lbf flightweight engine was designed and fabricated as a final task of the program. This engine was subjected to testing with propellant mixtures of hydrazine, hydrazinium nitrate, and water with the mixtures so selected that they had the same theoretical flame temperature but reduced freezing points as neat hydrazine. Three mixtures, which had freezing points of +20°F, 0°F, and -20°F, were successfully tested with very little difference noted in reactor operation between the three propellant mixtures.

Changes in catalyst carrier surface area and active metal surface area with accrued test time were measured during the program. It was found that the surface areas drop to approximately 70% of their original value after a short period of time and stabilize at that point. No change in reactor operation was noted as a result of this surface area change.

1.0 INTRODUCTION

This document constitutes Volume I of the Final Report of the Rocket Research Corporation "Development of Design and Scaling Criteria for Monopropellant Hydrazine Reactors Employing Shell 405 Spontaneous Catalyst" program conducted under Contract to the NASA Western Operations Office, Santa Monica, California, Contract NAS 7-372. This volume covers the contract scope of work, program test plan, engine design used in the study, and summarizes test data obtained during the program.

.

2.0 CONTRACT SCOPE OF WORK

2.1 General

The objective of NASA Contract NAS 7-372 was to determine and demonstrate the design techniques and to develop the empirical scaling formulae necessary for the design of monopropellant hydrazine reactors over a thrust range of 0.5 to 100 lbf. All of the reactor designs and tests employed the Shell 405 spontaneous catalyst developed under NASA Contract NAS 7-97. The design techniques and scaling formulae developed are applicable to the design of either rocket engines or gas generators. An additional part of the contract was the demonstration of a flightweight 5 lbf engine operating under pulsed and throttled modes of operation and also operating with hydrazine mixtures (hydrazine, hydrazinium nitrate, and water) which have low freezing points.

To develop the necessary scaling and design criteria, an experimental and analytical program was performed which includes the design, test, and evaluation of several engine configurations. Based on these evaluations, the design and scaling formulae were developed. The program was divided into two main phases which are summarized in the following sections.

2.2 Phase I

The work performed in Phase I provided the necessary data for development of design and scaling formulae. This work was divided into the three following tasks:

2.2.1 <u>Task I</u>

The Task I effort involved the evaluation of several catalyst bed and injector configurations at thrust levels of 0.5, 5, and 50 pounds. The engines were designed for a nominal chamber pressure of 150 psia. At each thrust level at least the following parameters were varied in a systematic manner to determine their influence on reactor operation:

- a. Chamber pressure
- b. Catalyst bed loading
- c. Catalyst bed length

- Injector design parameters such as pressure drop, orifice types, uniformity of flow distribution in catalyst bed, and injector location from catalyst bed
- f. Catalyst bed porosity.

The influence of each of the variables were judged by determination of the following:

- a. Injector and chamber configuration(s) which minimize ignition delay time, chamber pressure rise and decay times, and prevent excursions of chamber pressure from the design level
- b. Minimum residence time required for reliable ignition
- c. Ammonia dissociation as a function of bed loading, chamber pressure, characteristic length, catalyst bed porosity, and catalyst particle size, shape, and roughness
- d. Determination of catalyst bed pressure loss as a function of bed loading, chamber pressure, catalyst bed porosity, catalyst particle size, shape and roughness, and catalyst bed length
- e. Reactor operation as a function of catalyst bed pressure loss
- f. Factors which significantly degrade catalyst life. In particular the change in surface area and activity as a function of engine run time
- g. Characteristic velocity and specific impulse as a function of chamber pressure, characteristic length, bed loading, injector configuration, and catalyst bed configuration.

2.2.2 Task II

Based on the design and scaling criteria developed in Task 1, a 100 lbf engine was designed, fabricated, and evaluated to validate the scaling formulae developed at the thrust levels of 0.5, 5, and 50 pounds.

The evaluation was based on determination of the following minimum reactor performance factors:

- a. Characteristic velocity
- b. Ignition delay time and repeatability
- c. Chamber pressure rise and decay time and repeatability
- d. Catalyst degradation
- e. Combustion stability.

2.2.3 Task !!!

Based on the data obtained in Tasks I and II, the appropriate design and scaling formulae were developed to define the design of rocket engines and gas generators with the following items being developed:

- a. Formulae defining catalyst bed configuration as a function of the reactor design parameters including chamber pressure, bed loading, and catalyst size.
- b. Formulae or guidelines which define the pertinent injector design parameters necessary for reactor design
- c. Equations which predict catalyst bed pressure loss as a function of the physical properties of the catalyst, chamber pressure, bed loading, and catalyst bed length
- d. Physical properties of the catalyst bed such as porosity and specific surface area as a function of reactor configuration and catalyst particle size, shape, and roughness
- e. Formulae or curves defining ammonia dissociation as a function of the catalyst physical and chemical properties, residence time, and chamber pressure.

2.3 Phase II

The results of the Phase I effort provided design criteria for the optimum design of rocket engines and gas generators within the limits of the variables tested. Based on these design techniques, a flightweight 5 lbf engine was designed, fabricated,

and tested. The engine was to be subjected to three types of testing described below.

Pulse mode testing in a vacuum environment for two conditions as specified below:

- a. A duty cycle of 100 ± 10 milliseconds on a 500 ± 10 milliseconds off for a total elapsed time of one and one-half hours (approximately 13,500 pulses).
- b. A duty cycle of 100 ± 10 milliseconds on and 15 to 30 minutes off for 3 days of continuous operation (144 to 288 pulses).

Using the same engine design, throttling tests were to be conducted at a variety of throttled conditions. The tests were to utilize a variable area valve, located immediately upstream of the propellant valve, which would create pressure loss upstream of the injector. Tests were to be conducted over at least a 10:1 ratio of thrust.

Additional steady state tests were conducted with propellant mixtures of hydrazine, hydrazinium nitrate, and water. The mixtures were selected such that the flame temperature was equal to or less than that of anhydrous hydrazine. Testing was conducted with mixtures having freezing points of -20°F, 0°F, and +20°F.

The aforementioned pulse mode and throttling tests were not conducted on the program due to funding limitations.

3.0 TEST PLAN

3.1 General

To accomplish the objectives of the scope of work contained in Section 2.0, a series of experiments were developed at varied thrust levels to explore the effects of operating conditions, catalyst characteristics, and geometry of injector and reactor on the performance of monopropellant hydrazine rocket engines and gas generators employing the Shell 405 spontaneous catalyst.

During the experimental test program, theoretical reactor models were developed which attempted to define both the transient and steady state phases of reactor operation. These models served as a basis for correlating the experimental test data and development of the design and scaling criteria.

Details of the test plan for the program are presented in Rocket Research

Corporation document 65-R-36 "Contract NAS 7-372 Program Plan" dated May 24,

1965. The highlights of this test plan are covered in the ensuing sections for each of the phases of the contract.

3.2 Phase I Test Plan

3.2.1 Task | Test Plan

In order to minimize the number of test variables occurring at any one time, the test plan for Task I was divided into three separate subtasks. Each of the subtasks is described in the following paragraphs.

3.2.1.1 Subtask I

The first part of the program was an investigation of two injector designs and the effect of the injector design variables on reactor performance and operation. For these tests, bed loading, chamber pressure, bed length, and catalyst particle size and shape were held constant at each thrust level. The injector designs are described in Section 4.1. A typical test matrix used for the injector testing is shown in Figure 1. Testing in such a manner allowed independent determination of the effects of injector pressure drop, mass distribution, and injector distance from the catalyst bed. It

5 LBF THRUST ENGINE SHOWERHEAD INJECTOR TEST MATRIX

			70				
			75 psid	81 <i>-</i> 9	B1-18	81-27	
	6		45 psid	B1-8	81-17	B1-26	
			15 psid	81-7	B1-16	81-25	
rifices		e Drop	75 psid	81-6	81-15	B1-24	
Number of Orifices	9	Injector Pressure Drop	45 psid 75 psid	B1-5	81-14	B1-23	
Ž		Injec	15 psid	B1-4	81-13	B1-22	
			75 psid	81-3	81-12	81-21	
	3		15 psid 45 psid	81-2	81-11	81-20	
			15 psid	81-1	91-10	81-19	
				o inches	sədəni S.O	sədəni 4.0	
			Height from Catalyst Bed				

is emphasized that this portion of the study was not necessarily aimed at determination of the optimum injector for use with the Shell 405 catalyst. Rather it was aimed at defining rational injector design criteria that could be effectively employed in the latter phases of the program.

3.2.1.2 Subtask II

Subtask II of the test program is concerned with optimizing the catalyst size and shape. The injector type and configuration, bed loading, bed loading, bed length, and chamber pressure were held constant at each thrust level for these tests. Tests were conducted with a variety of catalyst sizes to determine that required for smooth and stable engine operation.

3.2.1.3 Subtask III

Having determined injector and catalyst particle size and shape effects, the third Subtask was concerned with determining the effects of chamber pressure, bed loading, and catalyst bed length on reactor operation. Chamber pressure was investigated over a range of 50 to 1,000 psia, bed loading over a 4.5:1 range (approximately 0.010 to 0.045 lbm/in²-sec), and bed length from the minimum required for ignition to that required for approximately 90% ammonia dissociation. A typical test matrix used for this phase of the testing is shown in Figure 2.

3.2.2 Task II Test Plan

Upon completion of the Phase I testing, the design data was extended to the design, fabrication, and evaluation of a 100 lbf engine. The evaluation criteria for this engine are as described in Paragraph 2.2.2.

3.2.3 Task III Test Plan

Throughout the first two phases of the program, theoretical reactor models were generated and the test data fit to the models. Upon completion of the Phase I and II test program, the final design and scaling criteria were developed based on correlation of the test data to fit the theoretical models.

TYPICAL TEST MATRIX FOR BED LOADING, CHAMBER PRESSURE, AND BED LENGTH TESTS

		1000	A-15	A-30	A-45	A-60																									
				475 1	A-14 A	A-29 A	A-44 A	A-59 A																							
			4																												
	0.0447		225	A-13	A -28	A-43	A-58																								
)		105	A-12	A-27	A-42	A-57																								
			50	A-11	A-26	A-41	A-56																								
) ()			1000	A-10	A-25	A-40	A-55																								
m/in ² -se		(0	475	A-9	A-24	A-39	A-54																								
NG (Ib	2115	0.02115 CHAMBER PRESSURE (psid)	2115 5URE (ps	225	A-8	A-23	A-38	A-53																							
BED LOADING (lbm/in ² -sec)	0.0		105	A-7	A-22	A-37	A-52																								
BED			50	A-6	A-21	A-35 A-36	A-51																								
			1000	A-5	A-20	A-35	A-50																								
			475	A-4	A-19	A-34	A-49																								
	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.01	0.0							225	A-3	A-18	A-33	A-48
																	105	A-2	A-17	A-32	A-47										
			50	A-1	A-16	A-31	A-46																								
				1	L ₂	الع	۲4																								
			l		HTƏV	131 Q38																									

4.0 REACTOR DESIGN

4.1 Injector Optimization Tests

4.1.1 Thrust Chamber Assembly

The engine designs used for the injector optimization testing are summarized in Table I with the pertinent design parameters being listed for each engine. A cross sectional view of the 0.5, 5, and 50 lbf engines is shown in Figures 3, 4, and 5 respectively.

The chamber and nozzle assembly of the 0.5 and 5 lbf engines are machined from 347 stainless steel bar stock. On the 50 lbf engine, the chamber is made of Haynes Alloy No. 25 sheet stock. The nozzle and chamber flange are made of 347 stainless steel and are welded to the Haynes Alloy No. 25 chamber. The chamber walls of all three engines are coated with a 0.020 inch thickness of Rokide Z (zirconium oxide) to minimize heat losses.

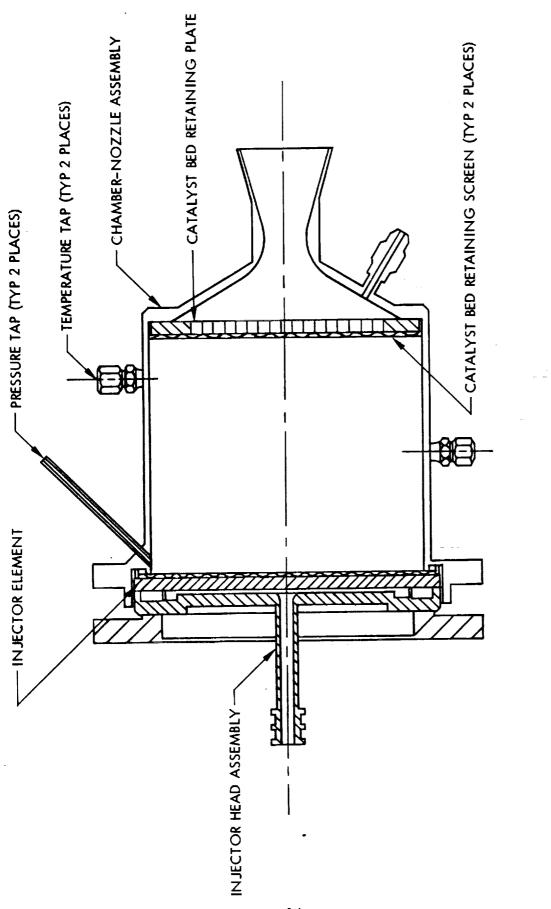
The injector is flanged to the chamber to facilitate changes of injector configurations and catalyst particles sizes and shapes. A retaining plate-screen assembly is used to retain the catalyst at the downstream end of the chamber. The retaining plate is made of 347 stainless steel. The lower screen for the 0.5 and 5 lbf engines is 60 x 60 mesh molybdenum screen of 0.005 inches wire diameter. The lower screen for the 50 lbf engine is 10 x 10 mesh molybdenum screen of 0.025 inches wire diameter. At the upstream end of the chamber, a screen, held in place by the chamber and injector flanges, retains the catalyst bed. The size of the upper screen for all three thrust levels is 60 x 60 mesh molybdenum screen of 0.005 inches wire diameter.

The injector consists of a flat plate in which various orifice sizes (to vary hydraulic pressure drop) and various numbers of orifices (to vary mass distribution) are machined.

Propellant is fed to a distribution manifold through a single tube for all three thrust levels.

Either K-seals or copper-asbestos gaskets are used for the injector to chamber gas seal.

CROSS-SECTIONAL VIEW 5 16 ENGINE



CROSS-SECTIONAL VIEW 50 16 ENGINE

SCALE: FULL SIZE

FIGURE 5

TABLE I

TASK I - ENGINE DESIGN SUMMARY

Design Parameters	0.5 lbf Thrust Engine	5.0 lbf Thrust Engine	50 lbf Thrust Engine
Vacuum Thrust, lbf at €= 50:1	0.5	5.0	50.0
Predicted Sea Level Thrust, lbf at ∈= 4:1	0.34	3.4	34.0
Chamber Pressure, psia	150	150	150
Engine Flow Rate, Ibm/sec	0.0022	0.0213	0.213
Chamber Diameter, in	0.544	1.205	3.010
Catalyst Bed Length, in	0.880	1 <i>.7</i> 85	2.680
Characteristic Length ⁽¹⁾ , in	100	100	100
Throat Diameter, in	0.050	0.156	0.492
Exit Diameter, in	0.100	0.312	0.984
Chamber Wall Thickness, in	0.022	0.050	0.035

⁽¹⁾ Based on empty catalyst bed volume.

4.1.2 Showerhead Injector

The showerhead injector consists of a flat plate in which orifices of various size (to vary pressure drop) and of various numbers (to vary mass distribution) are drilled. The following criteria was used in the analysis and design of the showerhead injector elements:

- a. The orifices shall be located in circular rows
- The minimum orifice diameter shall be approximately 0,010 inches
- c. The distance between the chamber wall and the outer orifice row shall be equal to the spacing between orifices
- d. The orifices shall cover equal areas of the catalyst bed.

Analysis of criteria (a), (c), and (d) above results in the following equation for determination of the spacing between orifices:

$$S = \frac{\pi n D_c}{N_T + \pi n^2 + \pi n}$$

Where:

S = Spacing between orifices

D_c = Catalyst bed diameter

n = Number of rows of orifices

 N_{T} = Total number of orifices

 $\pi = 3.1416$

A summary of the showerhead injector design details used in the testing is presented in Table II.

4.1.3 Rigimesh Injector

The rigimesh injector is basically a modified showerhead type injector in which the local bed loading (bed loading under each orifice) is

TABLE II
SHOWERHEAD INJECTOR DESIGN SUMMARY

0.5 Ibf THRUST ENGINE

Pressure Drop psid	Number Orifices	Orifice Dia., in.	Orifice Spacing
15	1	0.0145	Single Orifice in Center
45	1	0.0112	Single Orifice in Center
75	1	0.0097	Single Orifice in Center
		5.0 lbf THRUST	ENGINE
15	3	0.0275	Equally Spaced on 0.377 Diameter B.C.
45	3	0.021	Equally Spaced on 0.377 Diameter B.C.
<i>7</i> 5	3	0.0185	Equally Spaced on 0.377 Diameter B.C.
15	6	0.0182	Equally Spaced on 0.569 Diameter B.C.
45	6	0.0140	Equally Spaced on 0.569 Diameter B.C.
<i>7</i> 5	6	0.0123	Equally Spaced on 0.569 Diameter B.C.
15	9	0.015	Equally Spaced on 0.685 Diameter B.C.
45	9	0.0114	Equally Spaced on 0.685 Diameter B.C.
75	9	0.0100	Equally Spaced on 0.685 Diameter B.C.
		50 lbf thrust i	ENGINE
15	20	0.0320	13 on 2.036 Diameter B.C.
45	20	0.0243 }	7 on 1.062 Diameter B.C.
75	20	0.0213	7 on 1.002 Diameter B.C.
15	40	0.0225	20 on 2.276 Diameter B.C.
45	40	0.0172 }	13 on 1.542 Diameter B.C.
<i>7</i> 5	40	0.0151	7 on 0.808 Diameter B.C.
15	60	0.0183	24 on 2.394 Diameter B.C.
45	60	0.0140	18 on 1.778 Diameter B.C.
75	60	0.0123	12 on 1.162 Diameter B.C.
)	6 on 0.546 Diameter B.C.

appreciably less than the injector described in Paragraph 4.1.2. The rigimesh injector consists of a number of circular rigimesh discs which were press fit into a retaining plate. Each disc is approximately 0.25 inches in diameter.

The spacing criteria utilized for the showerhead injector described in Paragraph 4.1.2 was also used for the rigimesh injector.

Table III summarizes the design of the rigimesh injectors for each engine thrust level. Figure 6 shows a photograph of typical rigimesh and showerhead injectors tested on the 50 lbf engine.

4.2 Catalyst Bed Parameter Studies

The reactor designs for the catalyst bed parameter studies were designed to be capable of independent variations in bed loading, chamber pressure, and catalyst bed length. Various length chambers were manufactured for variations of catalyst bed length. Each chamber had removable nozzles so that bed loading and/or chamber pressure could be varied. The nozzles were sized to permit bed loading studies at 0.01, 0.021, and 0.045 lb/in²-sec and chamber pressure studies at 50, 105, 225, 475, and 1,000 psia.

A showerhead injector was utilized for all of the tests with the design criteria for the injector based on the results of the injector optimization tests. At all conditions the injector pressure drop was maintained at 10 to 20% of steady state chamber pressure.

The following sections describe the details of the engine designs at the 0.5, 5, and 50 lbf thrust levels.

4.2.1 50 lbf Engine

The 50 lbf engine design is shown in Figure 7. The injector design criteria is based on the results of the injector optimization testing and is as follows:

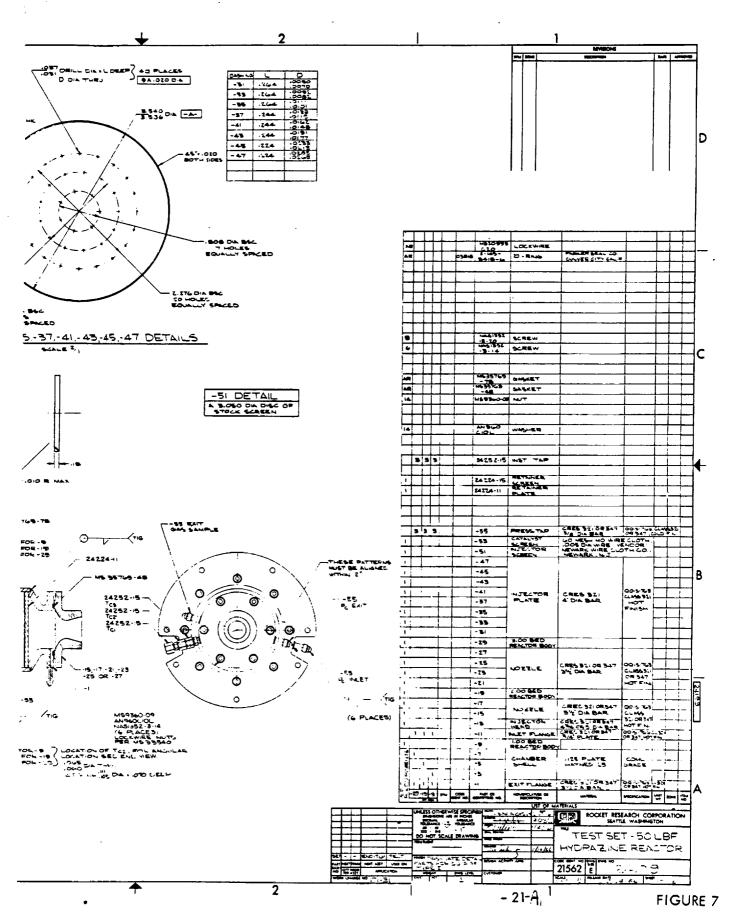
a. 40 orifices with 7 holes on a 0.808 inch diameter, 13 holes on a 1.542 inch diameter, and 20 holes on a 2.276 inch diameter.

TABLE III RIGIMESH INJECTOR DESIGN SUMMARY

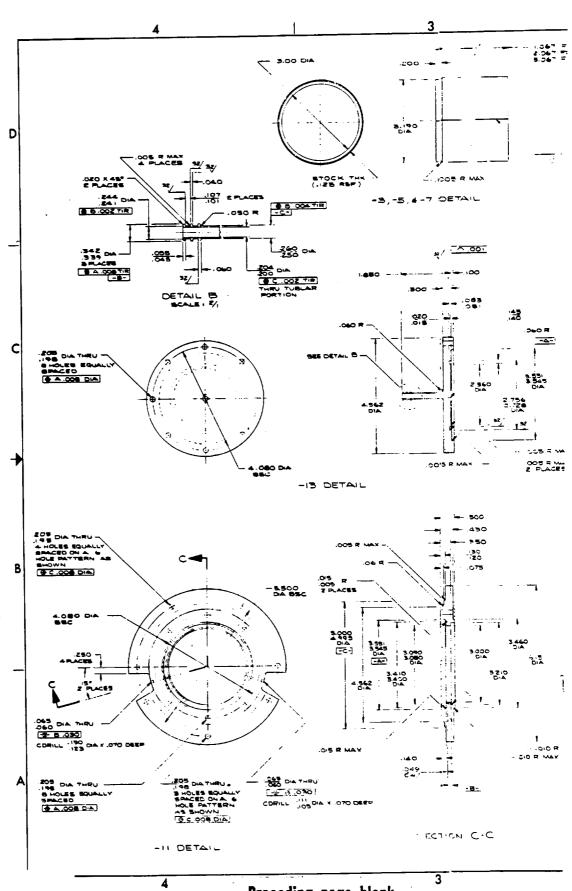
0.5 Ibf THRUST ENGINE

Pressure Drop psid	Number Discs	Rigimesh Disc Spacing				
15	1	Single Disc in Center				
45	1	Single Disc in Center				
75	1	Single Disc in Center				
	5.0	bf THRUST ENGINE				
15	1	Single Disc in Center				
45	1	Single Disc in Center				
7 5	1	Single Disc in Center				
15	4	Equally Spaced on 0.469 Diameter B.C.				
45	4	Equally Spaced on 0.469 Diameter B.C.				
75	4	Equally Spaced on 0.469 Diameter B.C.				
15	7	Equally Spaced on 0.635 Diameter B.C.				
45	7	Equally Spaced on 0.635 Diameter B.C.				
75	7	Equally Spaced on 0.635 Diameter B.C.				
	50 lb	of THRUST ENGINE				
15	7	Equally Spaced on 1.586 Diameter B.C.				
45	7	Equally Spaced on 1.586 Diameter B.C.				
75	7	Equally Spaced on 1.586 Diameter B.C.				
15	13	Four Equally Spaced on 0.638 Diameter B.C.				
45	13	Nine Equally Spaced on 1.824 Diameter B.C.				
75	13	Time address, observe on 1,024 promotor b.C.				
15	19	Six Equally Spaced on 1.014 Diameter B.C.				
45	19	Thirteen Equally Spaced on 2.012 Diameter B.C.				
75	19	quarry spaced on 2,012 Didnierer B.C.				

·			

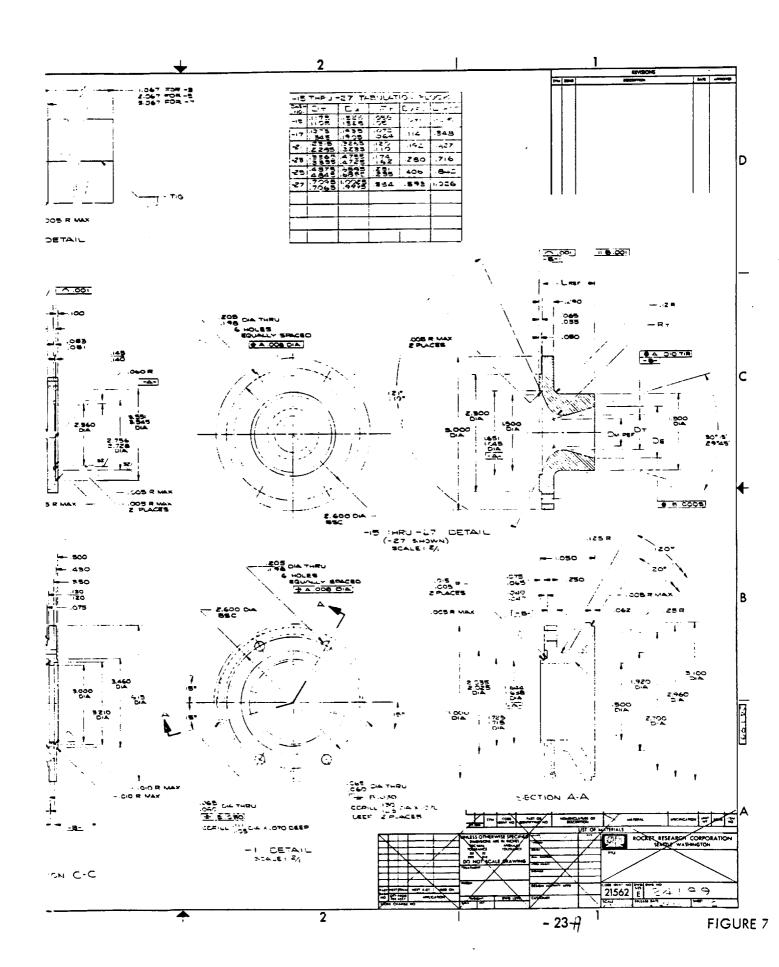


		·	
,			
	·		
	-		



					-
			-		
	•				
		•			•
	-				

•



				-
			·	
	•			

- b. Injector pressure drop to be approximately 10 to 20% of steady state chamber pressure.
- The injector is to be mounted flush with the top of the catalyst bed.

The chamber of 3.01 inches diameter is flanged on both ends to permit removal and replacement of various injectors and nozzles as required for the test program. The chamber is made of Haynes Alloy Number 25 Sheet Stock. All remaining parts are made of 321 or 347 stainless steel.

Three thermocouple taps are utilized on the engine. Two measure catalyst bed temperatures and the third measures exit gas temperature. Pressure taps are utilized to measure upstream and downstream chamber pressure. An additional tap is utilized for taking gas samples.

A Marotta solenoid valve MV-100 is used as the propellant valve.

4.2.2 <u>5 lbf Engine</u>

An assembly drawing of the 5 lbf engine is shown in Figure 8. A showerhead injector design is used with the following design parameters:

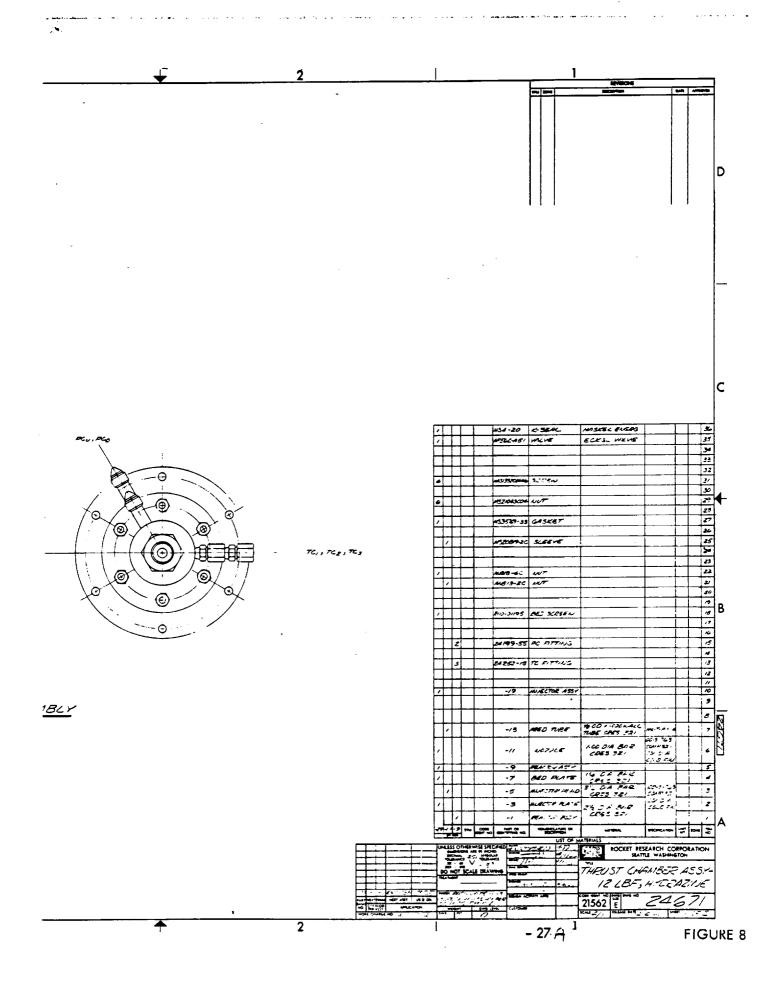
- a. Six orifices machined on a 0.569 diameter
- Injector pressure drop is maintained at 10 to 20% of chamber pressure
- c. The injector is mounted flush with the top of the catalyst bed.

The chamber of 1,205 inches diameter is flanged at the upper end to permit removal and replacement of injector plates. The outlet of the reactor consists of an AN fitting to which various sized nozzles, machined in AN 929 fittings, are attached. All parts are made of 321 or 347 stainless steel. Thermocouple taps are located along the chamber to measure catalyst bed and gas outlet temperatures. Three pressure taps are utilized to measure upstream and downstream chamber pressure and to take gas samples downstream of the catalyst bed.

An Eckel solenoid valve Model No. AF 56C-A51 is used as the propellant valve.

Preceding page blank

•			
		•	
	-		



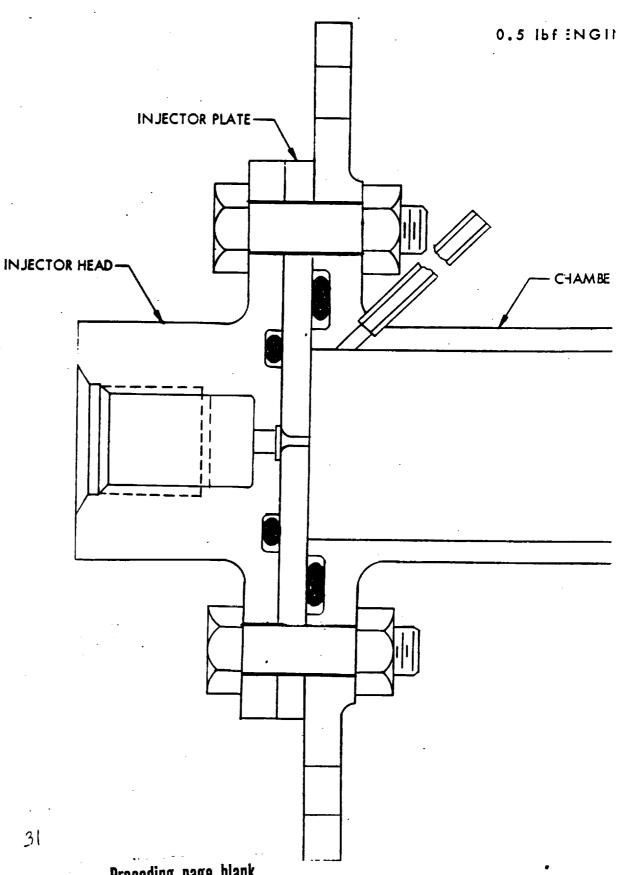
4.2.3 0.5 lbf Engine

An assembly drawing of the 0.5 lbf engine is shown in Figure 9. A single element showerhead injector is utilized which is mounted flush with the top of the catalyst bed.

The chamber of 0,544 inches diameter is flanged at the upper end to permit removal and replacement of injector plates. The outlet of the reactor consists of an AN fitting to which various sized nozzles, machined in AN 929 fittings, are attached. Pressure taps are utilized to measure upstream and downstream chamber pressure and to take gas samples. Because of the smallness of the chamber no thermocouple taps are used on the engine.

An Eckel solenoid valve Model Number AF 56C-A53 is used as the propellant valve.

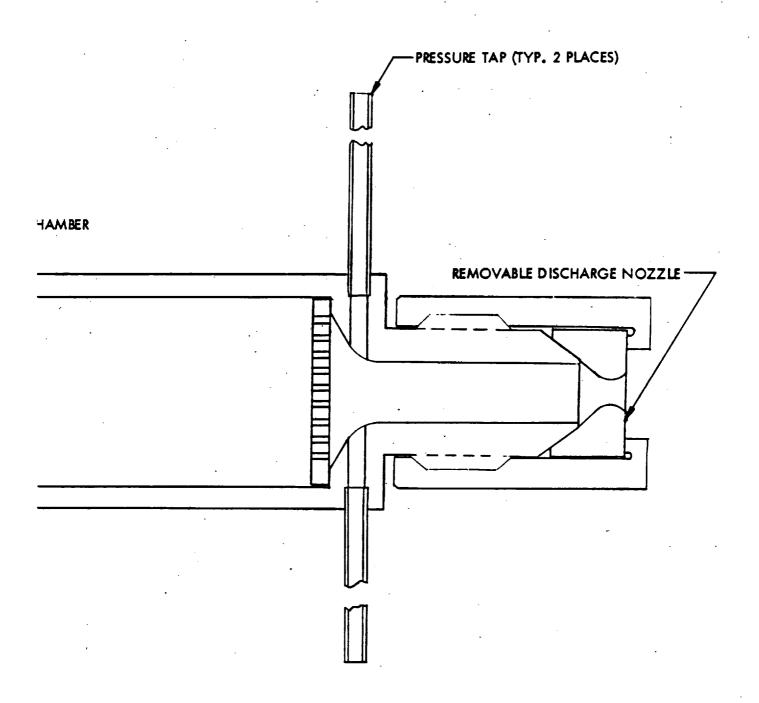
•				
		*		
				•
		•		
	•			
			•	
			•	



11804

Preceding page blank

			•	
•				
·				



•		
		•
	·.	
	·,	

5.0 TEST APPARATUS AND TEST PROCEDURES

5.1 Propellant Supply System

A schematic of the test cell setup for engine testing is shown in Figure 10. A line supply for each engine thrust level feeds off of a common hydrazine supply tankage. Flow meters are contained in series for each thrust level to obtain higher accuracy in measurement of flow rate. All valving is actuated remotely from the firing console. Teflon-lined stainless steel flexible lines are used to attach the propellant supply to the engine fire valve in order to provide a negligible resistance to the thrust measurement.

5.2 Thrust Stand

The thrust stands utilized for testing are of the parallelogram type. The stand consists of a reactor mount, suspended by four flexures from an inverted "L" shaped support. For the 0.5 and 5 lbf thrust stands (Figure 11) the flexures are stainless steel sheet stock 0.005 inches thick. For the 50 lbf engine thrust stand (Figure 12) Bendix Flexural Pivots are used. The axial thrust load is taken out by a Schaevitz-Bytrex load cell. The load from the thrust stand to the load cell is transmitted by a spherical load button acting on a flat plate in the 0.5 and 5 lbf thrust designs and by a flexure in the 50 lbf stand design. These designs eliminate application of side loads to the load cell to ensure high accuracy measurements.

Calibration of the stand is accomplished by application of known weights acting over a low friction pulley or a Bendix Flexural Pivot. The estimated friction error of the pulley is less than 0.06 percent of rated thrust.

5.3 Instrumentation

The contract specified that the reduced measurement error in pressure, flow rate and thrust measurements shall be less than 0.5 percent 3 σ . In order to accomplish this high accuracy all measurement devices procured had a specified error source of not greater than 0.25 percent. The gauge types used in the testing are described below. High accuracy recording equipment is used to assure that the total measurement error is less than 0.5 percent 3 σ .

ECD4 ...

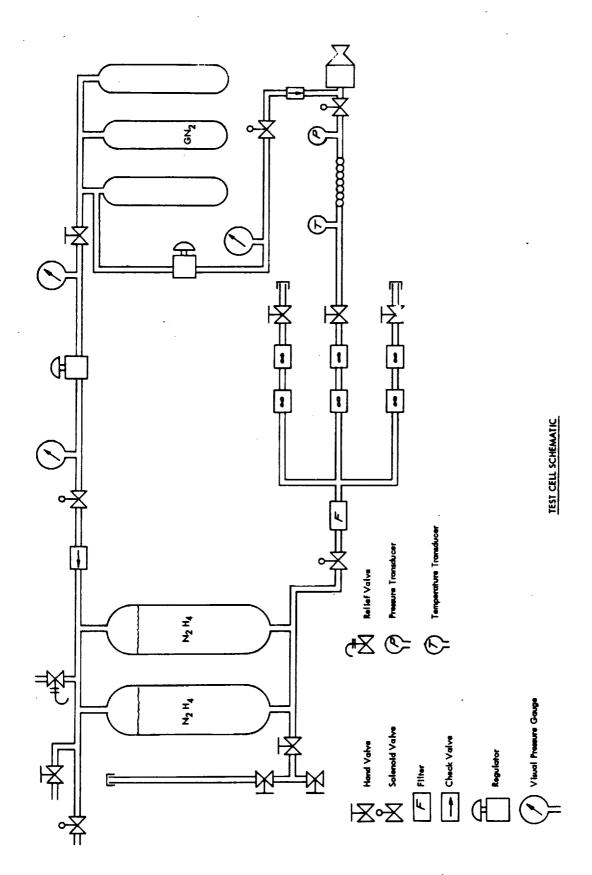
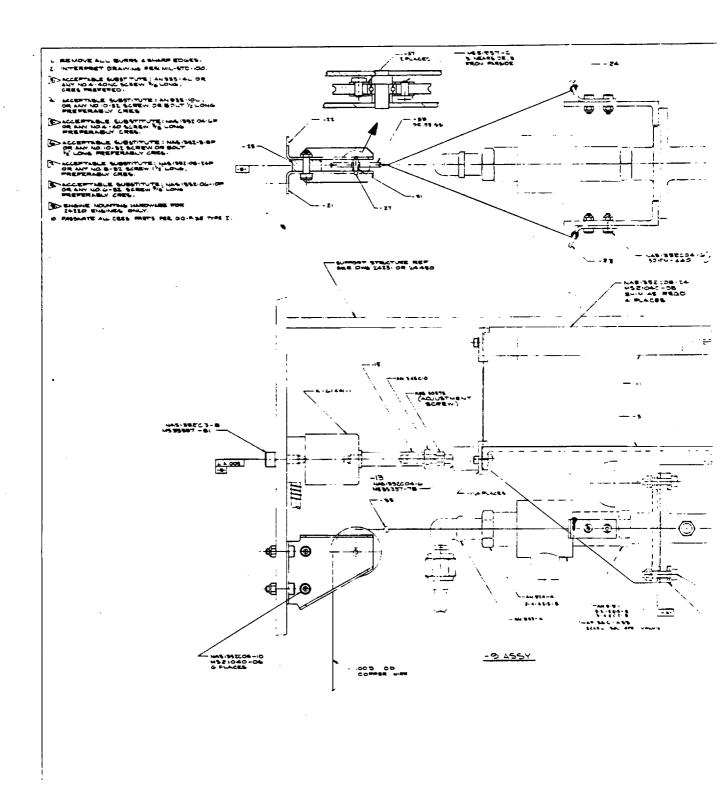
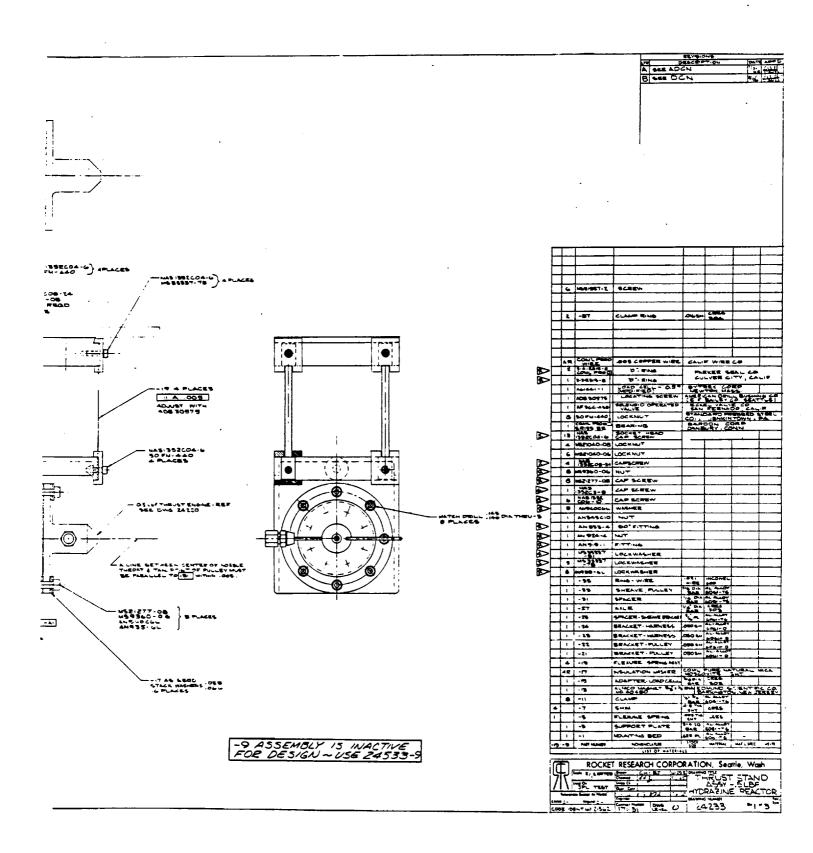


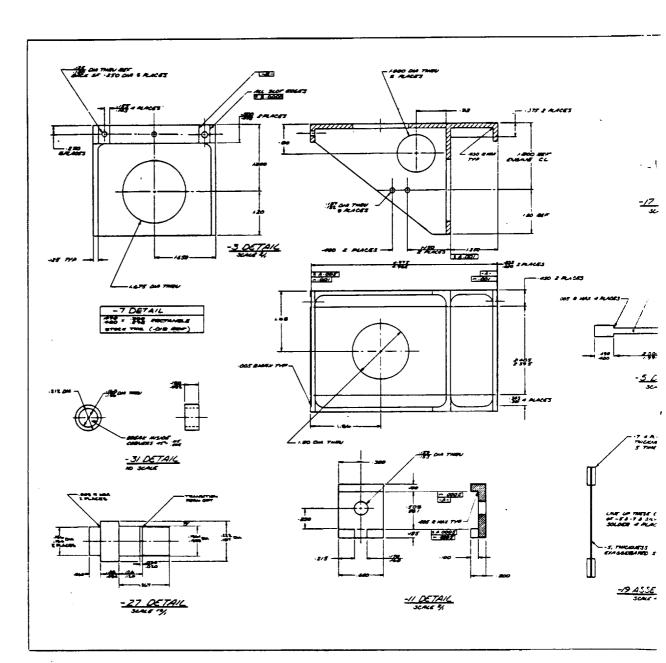
FIGURE 10



	•			
			•.	

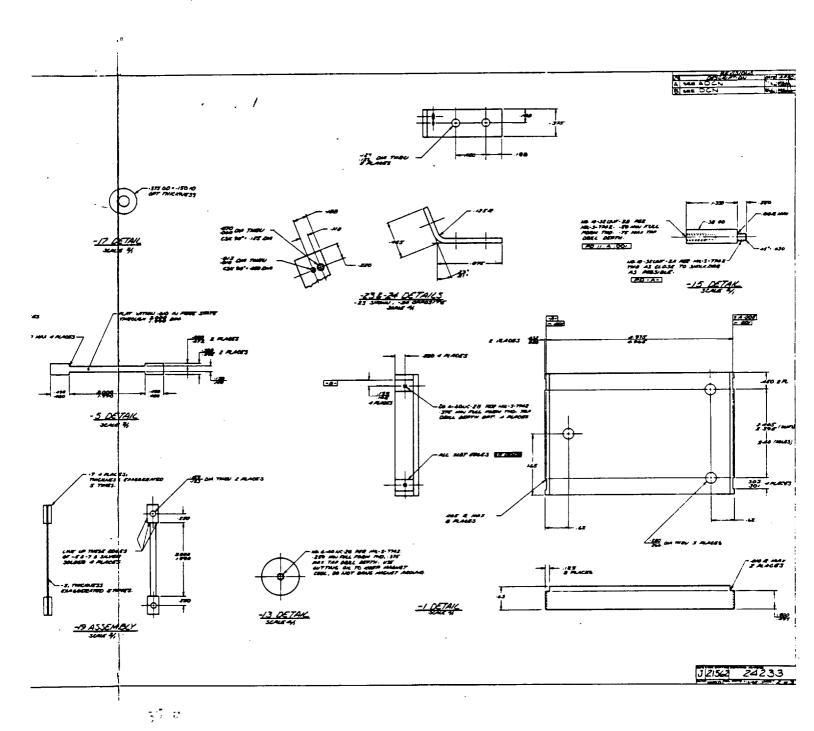


 <u> </u>		



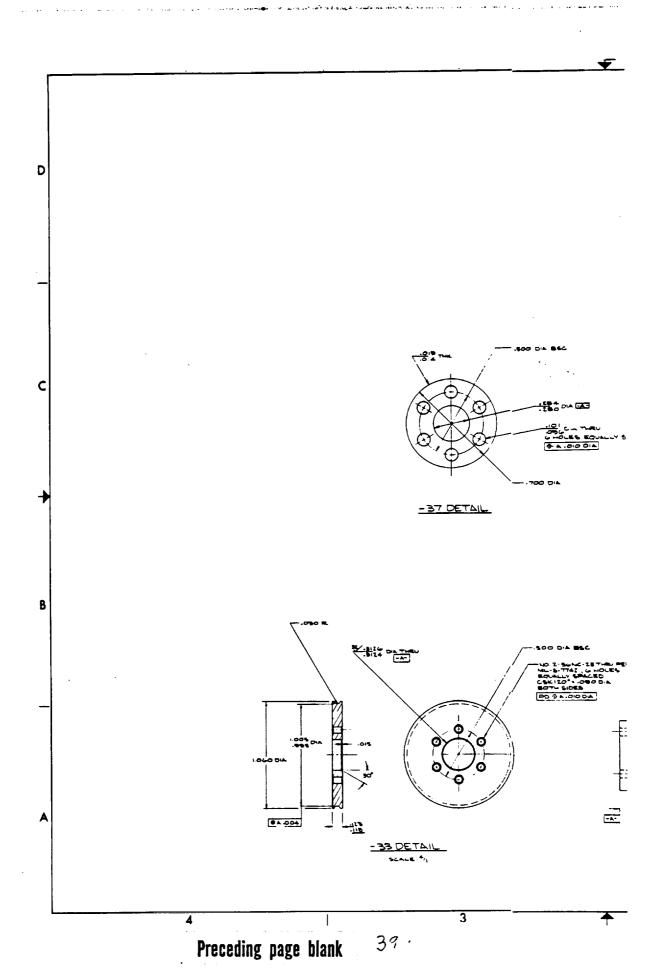
37. . .

			·
	. ·		
		·	

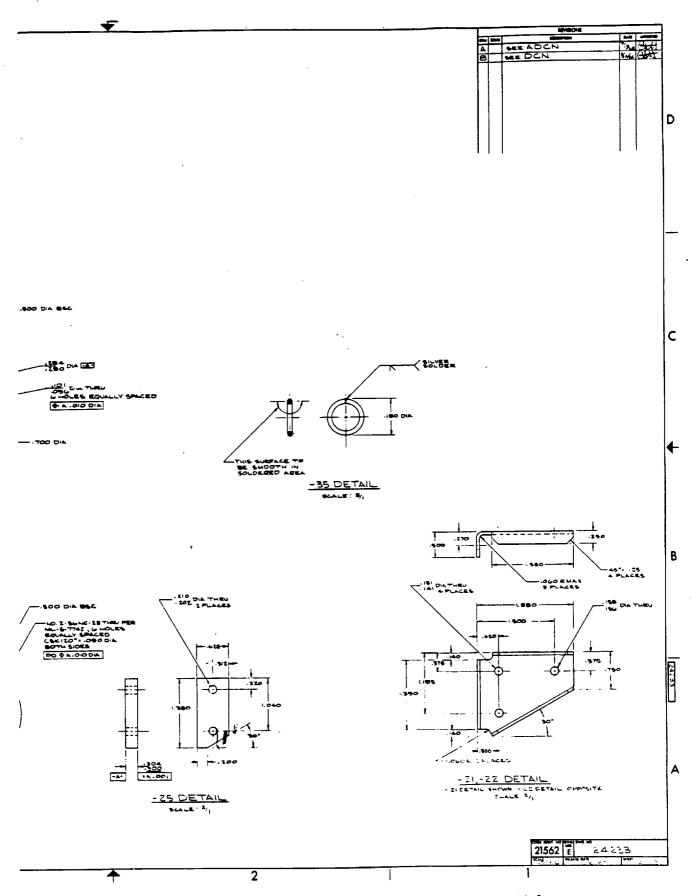


- 37 - A FIGURE 11

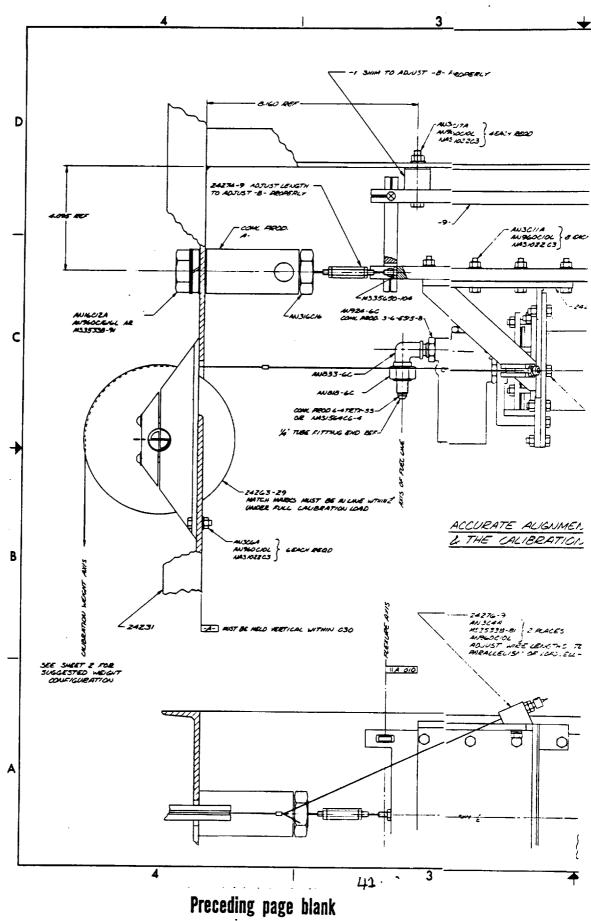
			•	
	·			



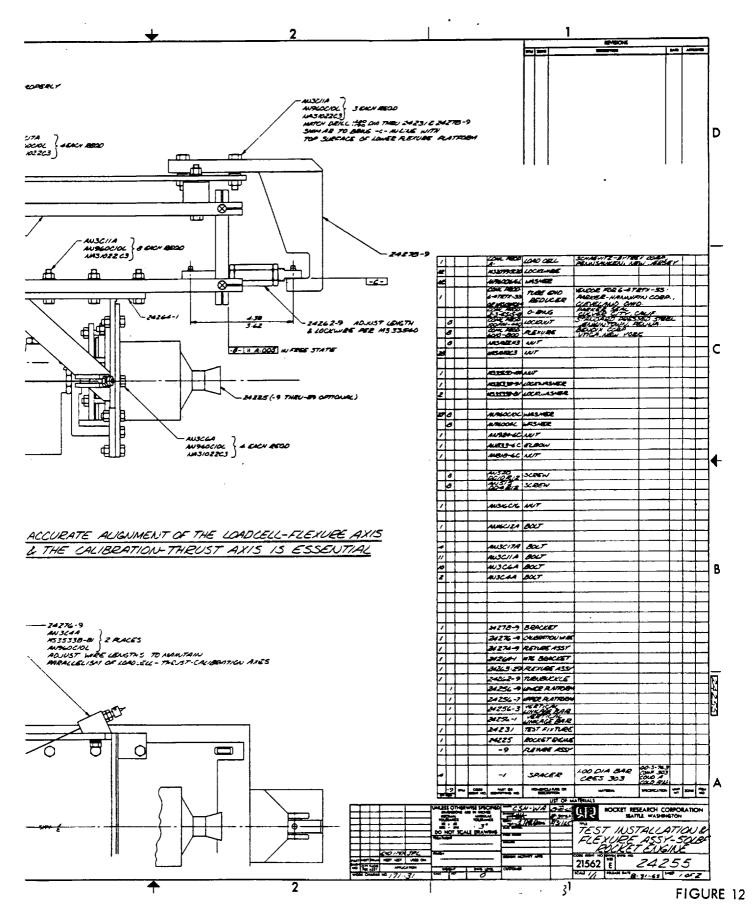
	•			
·				
			• .	
			÷	



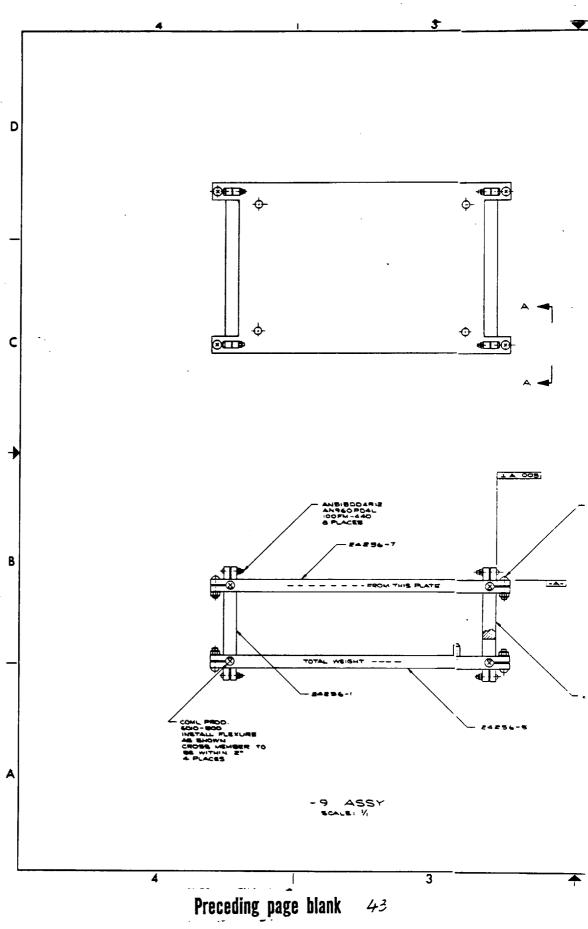
	·		
٠			
			•



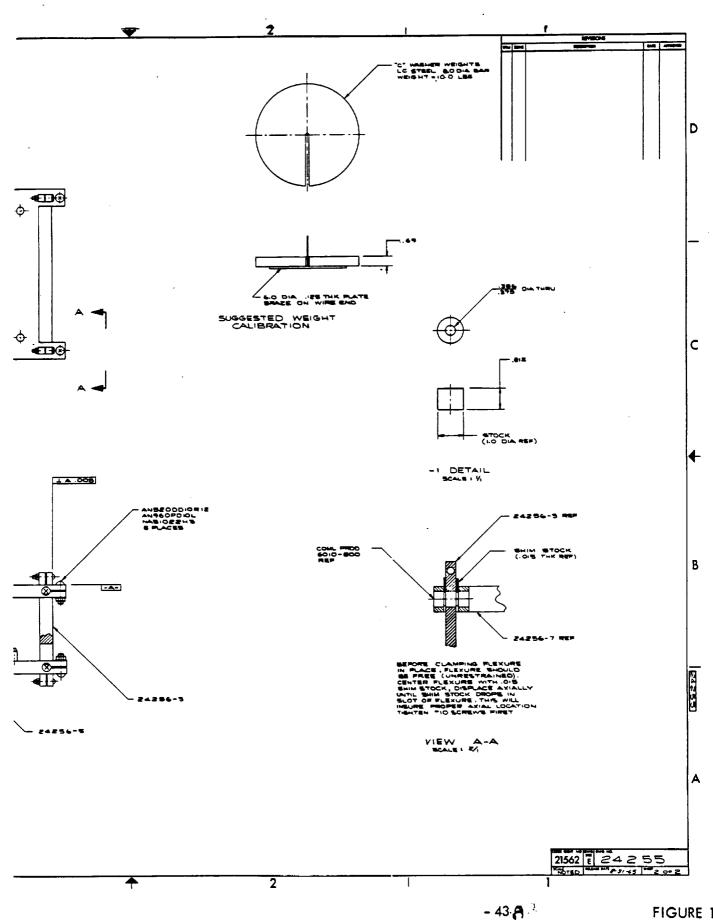
	•			
			•.	
·				
		·		



	•	



•				
		·		
			•	



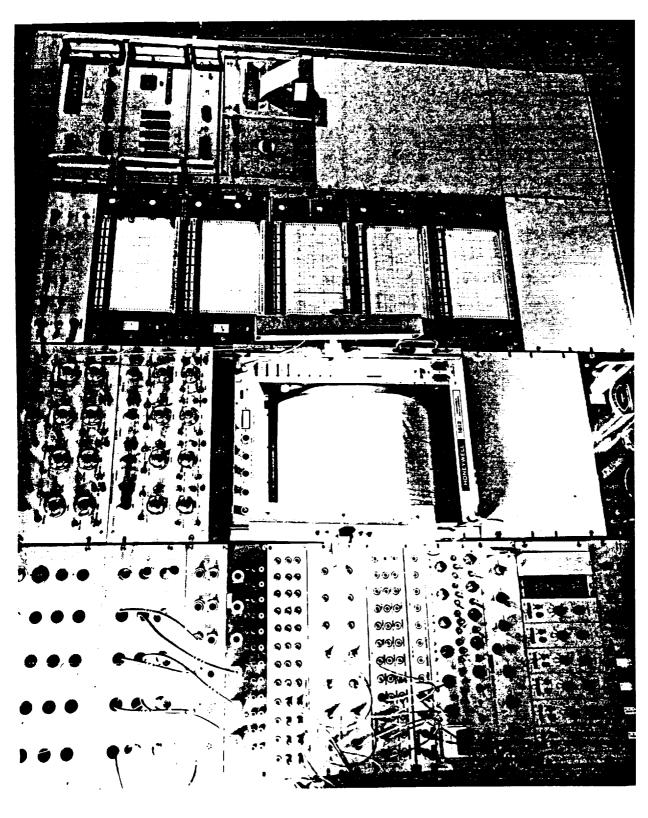
Instrumentation used for measurement of the indicated engine performance parameter is summarized below:

- a. Turbine flowmeters (two (2) in-series meters) manufactured by Cox Instrument Division, Lynch Corporation, were used for engine flow rate measurement. The following model numbers were used:
 - 1. 0.5 lbf Engine Model No. LF6-00
 - 2. 5.0 lbf Engine Model No. LF6-3
 - 3. 50 lbf Engine Model No. AN8-6
- b. Alinco pressure transducers manufactured by M. B. Electronics are used for chamber pressure and tank pressure measurement. The following ranges and model numbers were used:
 - 1. 0 200 psia Model No. 151-BAA-1
 - 2. 0 500 psia Model No. 151-BAA-1
 - 3. 0 1500 psia Model No. 151-AAA-1
- c. Load cells manufactured by Schaevitz-Bytrex Corporation are used for measurement of engine thrust. The following load cells were used:
 - 1. 0.5 lbf Engine Model No. A-61441-1
 - 2. 5.0 lbf Engine Model No. A-6144-4
 - 3. 50 lbf Engine Model No. A-61441-8
- d. Catalyst bed temperature is measured using chromel-alumel thermocouples of 0.040 inches wire diameter with ungrounded tips. The same thermocouple is also used for propellant temperature measurement.

Three data recovery systems are utilized for recording of the data from the engine tests. All pressures, thrust, flow rate, and valve sequencing are recorded on a 36 channel Honeywell Model 1612 oscillograph. All pressure, thrust, and temperature measurements are recorded on Moseley strip charts. Additionally, pressure and temperature measurements are recorded and printed out on a Dymec Model 2010A digital system. The data recording system is shown in Figure 13.

5.4 Test Procedures

Prior to engine hot firings each injector was water flow calibrated to determine its pressure drop-flowrate characteristics. Additionally, random orifices



46 - FIGURE 13

were individually sampled to assure that no gross maldistribution of flow existed from individual orifices. In no case did the flow out of any orifice deviate more than 5% from the average.

The catalyst bed was packed in a random dense manner (see Volume II, Section 5.0) in the chamber for all tests. The weight of catalyst packed was accurately measured and compared with the predicted values based on previous catalyst bed packing studies. If gross differences existed, the bed was repacked.

Each test was conducted under ambient temperature and pressure conditions. All tests represented steady state runs of 30 to 40 seconds duration.

For each test conducted during the study of reactor design variables, a gas sample of the decomposition products was obtained. Specifically, when the catalyst bed and gas temperature reached steady state, a gas sample, taken immediately downstream of the catalyst bed, was drawn into an evacuated Hoke gas sample cylinder. The gas was then analyzed for the mole percent of ammonia, nitrogen and hydrogen by use of a gas chromatograph.

The hydrazine decomposition can be expressed as:

$$3N_2H_4 \longrightarrow 4(1-X) NH_3 + (2X+1) N_2 + 6XH_2$$

Three mole ratios, i.e., ratio of ammonia to hydrogen, ammonia to nitrogen, and nitrogen to hydrogen may be related to fractional ammonia dissociation, X, on the basis of the above equation; this permits calculation of fractional ammonia dissociation from gas sample analysis data. Ammonia dissociation is reported as the average of that determined from the ammonia to hydrogen and ammonia to nitrogen mole ratios. The deviation between these two calculated values was, in most cases, less than 2%.

Periodically a sample of the catalyst was removed from the reactor and measurements were made of the carrier and active metal surfaces areas to determine changes with use. Carrier surface area was measured by nitrogen adsorption techniques and active metal surface area was measured by hydrogen chemisorption.

All granular and cylindrical pellet size catalyst used in the injector optimization testing was manufactured from the Harshaw Alumina Carrier. For the catalyst bed design parameter studies the granular catalyst was manufactured from the Reynolds Alumina Carrier.

·				
·		-		
,				
·				

6.0 INJECTOR OPTIMIZATION TEST RESULTS

6.1 Data Reduction Techniques

Data reduction for the injector optimization tests consisted of determination of engine ignition delay time, chamber pressure rise time to 80% of steady state value, chamber pressure decay time to 10% of steady state value, chamber pressure roughness, characteristic velocity, specific impulse, and thrust coefficient. In addition, catalyst bed, injector head, and propellant temperatures were measured during each test. The techniques used in the data reduction are explained in the ensuing paragraphs.

Ignition delay is defined as the time from entry of propellant into the chamber until the chamber pressure downstream of the catalyst bed attains 1% of its steady state value. On engine start, the feed pressure (measured just upstream of the propellant valve) drops off momentarily as the ullage volume between the valve and injector is filled. The point at which this pressure begins to rise after dropping off is defined as the time when propellant begins to enter into the chamber. Ignition delay is then the time increment between the beginning of feed pressure rise and downstream chamber pressure rise. This parameter is obtained from the oscillograph record.

Chamber pressure rise time is defined as the time from propellant entry into the chamber to achievement of 80% steady state chamber pressure. The 80% value is taken as a percentage of the steady state chamber pressure downstream of the catalyst bed expressed in absolute units. Rise time to 80% of steady state chamber pressure was selected in lieu of 90% because it appeared to be a more consistent parameter. During the engine testing rise times to 90% chamber pressure averaged 2.7 times those to 80%. Chamber pressure decay time is defined as the time from downstream chamber pressure start decay to 10% of the steady state value measured in psig units.

Chamber pressure roughness is defined as the peak-to-peak variations in the chamber pressure downstream of the catalyst bed. The data is taken off the oscillograph at a run time between 20 and 30 seconds unless otherwise noted.

Characteristic velocity is calculated from the equation:

$$c^* = \frac{P_{cd} A_{tg}}{\dot{w}}$$

Where:

Characteristic velocity, ft/sec

Engine throat area, in²

Gravitational constant, 32.17 ft/sec²

Propellant flow rate, lbm/sec

Chamber pressure downstream of the catalyst bed, psia.

The engine throat area used in the calculations represents the average geometric area with corrections made for the thermal expansion and nonuniform flow conditions in the throat region caused by nozzle wall effects. The correction for thermal expansion was made assuming the throat diameter expands freely based on the metal temperature at the throat. The correction for nonuniform flow at the throat is treated by Rao (Reference 1) and results in a decrease in the geometric area of 0.75%. The flow rate used in the equation is an average of two flowmeters in series in the propellant supply line.

Engine specific impulse is calculated from the equation:

$$I_{sp} = \frac{F_m}{x_i}$$

Where:

Engine specific impulse, lbf-sec/lbm Measured thrust, lbf

Propellant flow rate, lbm/sec

The propellant flow rate used in the above equation is again an average of two flowmeters in series.

The engine thrust coefficient is calculated from the equation:

$$C_f = \frac{F_m}{P_{cd} A_t}$$

Where:

C_f = Engine thrust coefficient

F = Measured thrust, lbf

 P_{cd} = Chamber pressure downstream of the catalyst bed, psia

 A_{+} = Engine throat area, in²

Again, the same corrections are applied to the throat area as discussed under the characteristic velocity calculations.

Characteristic velocity, specific impulse, and the thrust coefficient are all calculated from average values of measurements taken from 29 to 30 seconds into the test.

As a first step in determination of the effect of injector variables on cold bed response times, ignition delay, chamber pressure decay time, and chamber pressure roughness scatter diagrams of the data were plotted (Reference 2). In the scatter diagram each separate factor is plotted without considering any other factor. The scatter diagram points out significant trends without lengthy correlation analysis. Subsequently, statistical tests were made of the data for determination of levels of significance in trends noted from the scatter diagram. If a complete test matrix was completed, a factorial analysis of variance was performed on the data to determine levels of significance and to determine interactions which may exist between the injector variables (Reference 2). When a complete test matrix was not completed, "F" tests were conducted to determine levels of significance (Reference 2).

6.2 Test Results

6.2.1 0.5 lbf Showerhead Injector

Testing of the 0.5 lbf showerhead injector engine is summarized in Table IV. Tests were conducted at pressure drops of 15, 45, and 75 psid with the injector flush with the catalyst bed and at 15 and 45 psid with the injector 0.2 inches from the bed. For all of these tests, 20-25 mesh granular catalyst was used in the catalyst bed. The test results are plotted in a scatter diagram in Figure 14 and are described in the ensuing paragraphs.

Chamber Pressure Roughness	% Peak-to-peak	÷ 4.60	± 4.30	±7.20	± 2.50	± 2.60	± 2.68	± 2.36	.+ 1.80	÷ 1.60	+ 1.50	± 1.65	÷ 1.85	+ 3.6	+3.6	± 13.2	± 6.63
Thrust Coefficient R	€	1.154	1.156	1.159	1.152	1.142	1.155	1.168	1.152	1.157	1.157	. 166	191.1	1.158	1.158	ව	<u> </u>
Specific Impulse	(bf-sec, (lbm	149.6	150.8	149.2	150.2	146.9	149.4	150.6	146.1	151.2	149.2	152.4	150.2	150.7	149.9	<u>(c)</u>	<u>.</u>
Characteristic Velocity	fl/sec	4171	4195	4140	4193	4139	4160	4147	4078	4203	4150	4205	4162	4186	4165	ල	ල
Steady-State Catalyst Bed Temperature	٠ ١	1428	1494	1560	1407	1424	1396	1409	1490	ļ	1472	1494	1481	1430	1506	1486	1566
St C Flow Rate T	lbm/sec	0.002366	0.002620	0.002622	0.002550	0.002600	0.002613	0.002640	0.002561	0.002526	0.002553	0.002559	0.002537	0.002548	0.002608	ල	ව
Though	<u>ā</u>	0.354	0.3%	0.391	0.383	0.382	0.390	0.393	0.374	0.382	0.381	0.390	0.381	0.384	0.391	ව	ව
Chamber Pressure	ğ	137.1	152.7	150.7	148.7	149.5	151.0	150.5	145.1	147.5	147.2	149.5	146.7	148.2	150.9	152.2	150.9
Injection Pressure	g	165.0	176.7	173.0	210.7	210.7	214.5	213.2	240.2	242.7	242.7	244.2	241.0	174.2	1.271	214.0	210.2
Decay Time	Ę	ł	ţ	167	<u> </u>	<u>₹</u>	118	128	143	116	9	130	118	\$	1	2	387
Response	Ę	8	83	118	245	4 54	245	285	410	637	510	630	550	240	35	730	089
lgnition Delay	Ė	4	5	9	4	. ⊖	7	2	13	22	15	13	81	42	5 6	\$	23
Initial Catalyst Bed Ignition Temperature Delay	¥	56	29	3	3	3	29	8	3	જ	7.	/9	3	62	3	ĸ	71
Fuel	4	59	67	3	79	3	3	3	প্ত	3	69	.	3	3	3	r	3
T sp	ε	5.0	15.0	15-0	9	6 5	45.0	5	75.0	25 0-25	75~	75-0	5. 0.57	152	15-,2	452	452
Test No.		171-31-2	171-31-12	171-31-13	171-31-3	171-31-4	171-31-7	8-17-121	171-31-5	171-31-6	171-31-9	171-31-10	171-31-11	171-31-14	171-31-15	171-31-16	171-31-17

(1) First number refers to nominal injector pressure drop. Second number refers to distance of injector from top of catalyst bed.

⁽²⁾ Nozzle Expansion Ratio is 3.5:1

⁽³⁾ Chamber excursions too large to obtain steady-state data.

Examination of the scatter diagram in Figure 14 indicates that the cold bed response times increase as the injector pressure drop is increased. The average response time (average of data at each pressure drop) is plotted versus injector pressure drop in Figure 15. It is also noted from the scatter diagram that ignition delay increases as the injector pressure drop is increased. A plot of average ignition delay versus injector pressure drop is shown in Figure 16. Chamber pressure roughness declines as injector pressure drop is increased. This trend is shown in Figure 17. Chamber pressure decay time does not appear to be affected by injector pressure drop.

Significant changes in reactor operation were noted when the injector was moved 0.2 inches from the top of the catalyst bed. Cold bed response, ignition delay, and chamber pressure decay times increased markedly as is seen from the data in Table IV. At 15 psid pressure drop fairly smooth (± 3.6% peak-to-peak chamber oscillations) operation was obtained. However, at 45 psid injector pressure drop, chamber pressure oscillations were large. Because of these large oscillations in chamber pressure no tests were conducted at 75 psid injector drop.

No observable change in performance was noted as the injector parameters were varied. Characteristic velocity averaged 4,164 feet per second, specific impulse averaged 149.7 lbf-sec/lbm, and the thrust coefficient averaged 1.157.

6.2.2 0.5 lbf Engine Rigimesh Injector

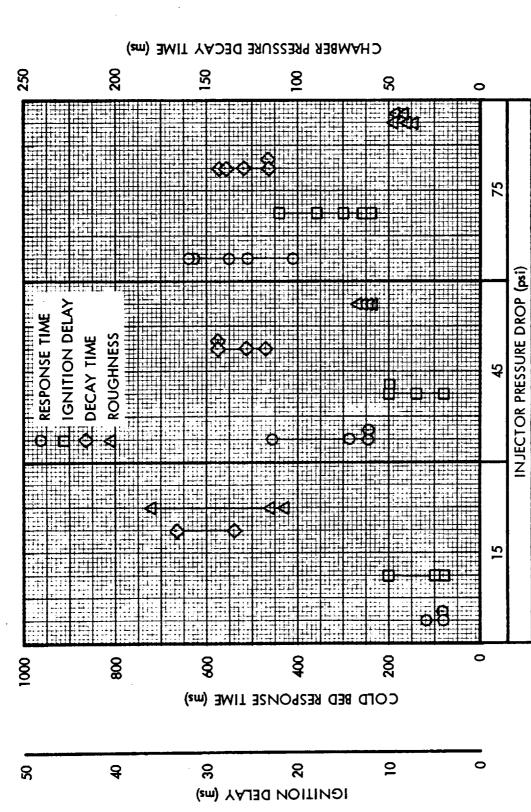
Testing of the 0.5 lbf rigimesh injector engine is summarized in Table V. Tests were conducted at pressure drops of 15, 45, and 75 psid with the injector flush with the catalyst bed and at 75 psid with the injector away from the catalyst bed. Data obtained from the testing is plotted in the scatter diagram in Figure 18. The results of this testing are described in the following paragraphs.

Examination of the scatter diagram indicates an increase in cold bed response time with pressure drop. The average response time is plotted in Figure 19, versus injector pressure drop. The scatter diagram in Figure 18 indicates ignition delay times are lower at 15 psid injector pressure drop 0.5 Ibf ENGINE SHOWERHEAD IN JECTOR SCATTER DIAGRAM

01 -

φ,

INJECTOR VARIABLE



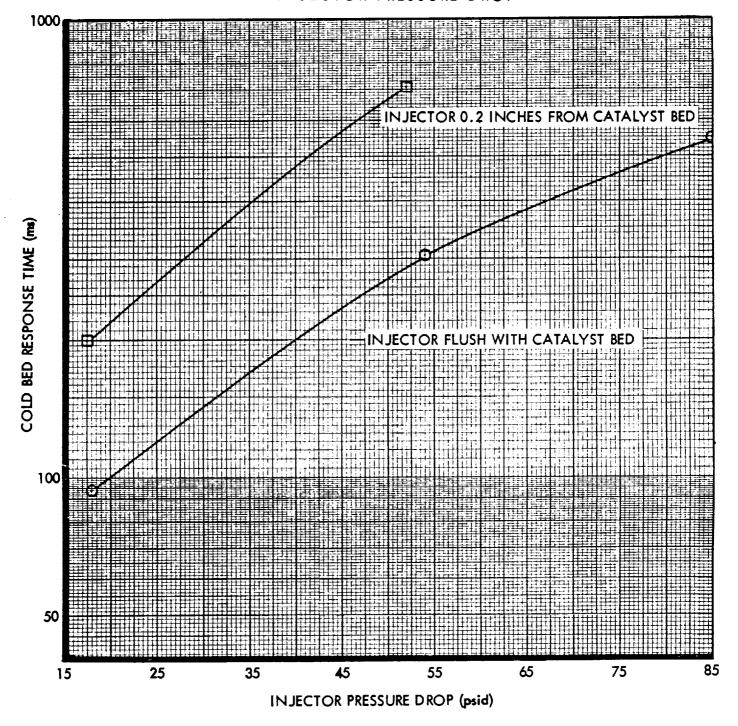
CHAMBER PRESSURE ROUGHNESS (% Peak-to-Peak)

+1

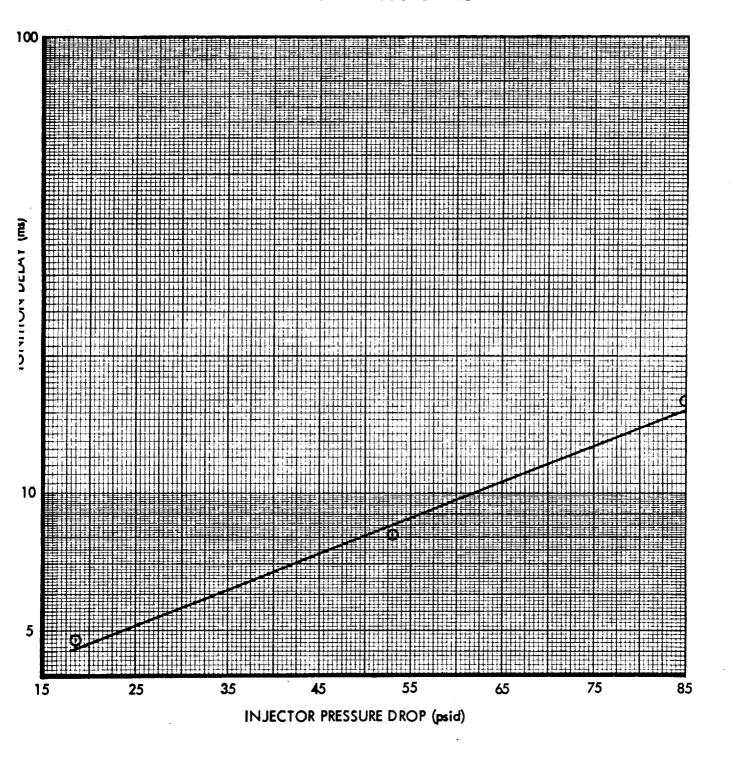
7,

9.

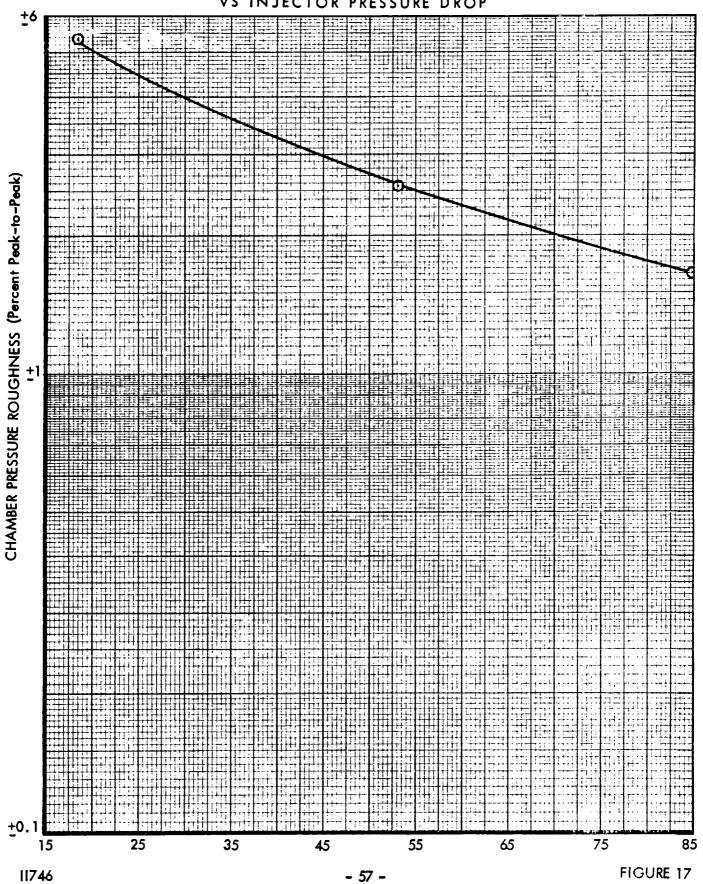
0.5 Ibf ENGINE
SHOWERHEAD INJECTOR
AVERAGE COLD BED RESPONSE TIME
VS
INJECTOR PRESSURE DROP



0.5 Ibf ENGINE
SHOWERHEAD INJECTOR
AVERAGE IGNITION DELAY
VS
INJECTOR PRESSURE DROP



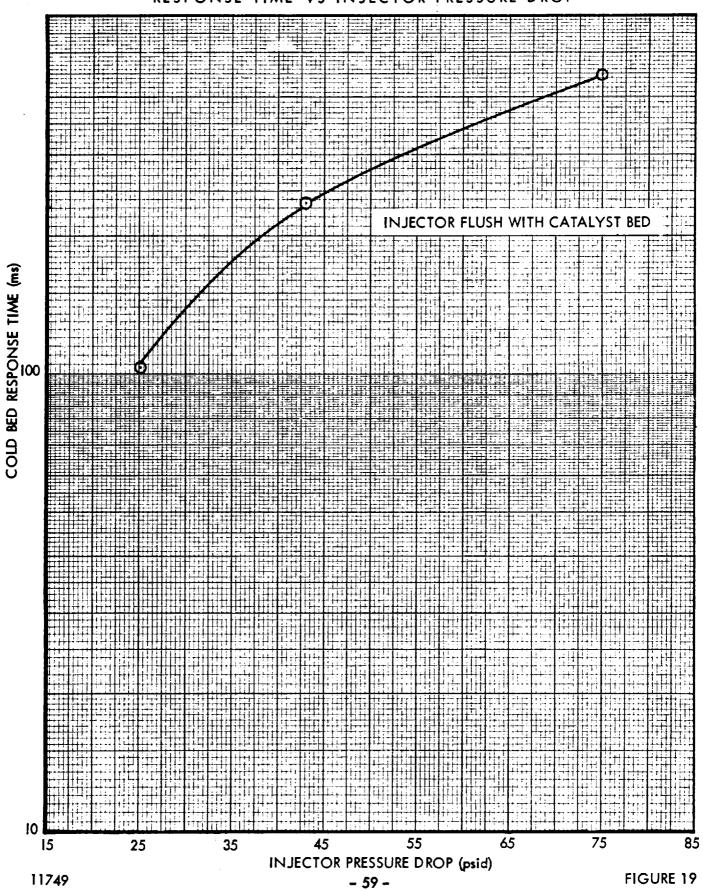
0.5 Ibf ENGINE SHOWERHEAD INJECTOR AVERAGE CHAMBER PRESSURE ROUGHNESS VS INJECTOR PRESSURE DROP



7-8+ 9. CHAMBER PRESSURE DECAY TIME (ms) 250 20 0 INJECTOR PRESSURE DROP (psi) RIGIMESH INJECTOR SCATTER DIAGRAM G IGNITION DELAY INJECTOR VARIABLE RESPONSE TIME ♦ DECAY TIME ○ ROUGHNESS <u>o</u> 200 8 800 COFD BED KESLONZE LIWE (ms) 0 ည **4** 30 2 2 IGNITION DELAY (nis)

CHAMBER PRESSURE ROUGHNESS (% Peak-to-Peak)

0.5 Ibf ENGINE RIGIMESH INJECTOR AVERAGE COLD BED RESPONSE TIME VS INJECTOR PRESSURE DROP



0.5 LBF ENGINE - TEST DATA SUMMARY - KIGIMESH IN JECTOR TABLE V

Chamber Fressure Koughness	% Pea -to-peak	02°61 ∓	20.00	3.34	+ 2.72	± 2,74	2.74	2.82	2 2.87	+ 27,10
		(3)	2	1.174	<u>-</u> . 35	1.161	9.7.	25	٠. تع	(S
Specific Thrust Impulse Coefficien	tof sec. 'lb (4)	(3)	<u>@</u>	153.2	151.1	159.1	152.4	54.3	2.3	(3)
Characteristic Velocity	ff, sec	6	O	4196	4149	4100	4135	71%	4190	(2)
Strady-State Catalyst Bed Temperature	.	1381	1381	3	14 15		1437	1400	145.	1531
Ster Ca Flow Rate Te	lbm, sec	(2)	(3)	302731	0.032714	0.302706	0.302913	0.302576	U. 002628	(2)
_	<u> </u>	(3	2	0.426	.408	0.405	(432	0.413	0.41	(2)
Chamber	psid	152.3	151.1	161.4	155.6	150.7	<u>8</u> .3	153.5	153.2	8
Injection Preserve		0.181	C.181	198.1	194.7	195.1	242.8	233,4	4	7.427
Decay Time	E	732	247	225	203	215	205	57	787	<u>.</u>
Response Time	Ē.	Š	112	235	2,iA	; E	, A	1 5	· [4]	3
lg nition Delay	Ė	1.	•0	, O.		2 2	! 2	: =	: 5	2 😝
Initial Catalyst Bed Temperature	'n	25	;	;	; ;	\$ 7	5 %	3 5	ì	67
F.rel Temperatura	۴	ý	1 5	} ₹	5 8	.	34	2 1	g ;	2 33
Test Cude	ε	Š	2 5	2 4	? :	1	? ?	P (? ;	75-2
Test No.		5	80-11-1-1	200	00-15-17	18-18-171	29-16-121	0'-15-1/1	//-18-1.1	171-31-78

(1) First number refers to naminal injector pressure drop. Second number refers to distance at injector from top of catalyst brid.

(2) Chamber pressure excursions top large to obtain steady-state data.
(3) Start and shortdown erratic.
(4) Nozzle Expansion Ratio is 3.5:1

(average value 6 ms) than at 45 or 75 psid pressure drop (average value 12 ms). The scatter diagram also shows a decrease in chamber pressure decay time as injector pressure drop is increased. Very high chamber pressure oscillations were obtained with the 15 psid injector (\pm 20% peak-to-peak) while smooth operation (\pm 2.7 to \pm 2.80%) was obtained at 45 psid and 75 psid.

Testing of the injector away from the catalyst bed produced very erratic operation and long response and tailoff times. Additionally, chamber pressure excursions of ± 27% peak-to-peak occurred. This erratic operation may well be the result of the poor spray pattern out of the injector. The spray pattern was not axial and impingement of propellant on the chamber walls probably occurred giving rise to the erratic operation.

Characteristic velocity for the tests averaged 4,179 feet per second, specific impulse averaged 152.7 lbf-sec/lbm, and the thrust coefficient averaged 1.174.

In comparing the rigimesh injector test results with the showerhead injector, the following conclusion can be made:

- a. Cold bed response times are very similar
- b. Variations in ignition delay with pressure drop are not as large with the rigimesh injector as with the showerhead injector.
- c. The showerhead injector runs smoother than the rigimesh injector at all injector pressure drops, although at 45 psid the results are very similar.
- d. Decay times are higher with a rigimesh injector design than the showerhead.

6.2.3 5 lbf Engine Showerhead Injector

Testing on the 5 lbf engine with the showerhead injector was in accordance with the test matrix shown in Figure 1. The first test on the 5 lbf engine used a catalyst bed composed of 10–12 mesh granular particles. During the test, cyclic oscillations occurred in the chamber pressure of 20 to 50 psia at a frequency of 13 to 18 cps. Several variables were tested which could possibly have led to the instability noted. These variables included:

- a. Nonstable orifice characteristics
- b. Injector manifolding which could lead to (a) above
- c. Feed system coupling
- d. Channeling of flow in the catalyst bed
- e. Hydrazine boiling in the injector manifold
- f. Nonstable flame front in the catalyst bed
- g. Bed loading
- h. Catalyst particle size and/or porosity.

Testing covering the above variables resulted in elimination of the first five items as the cause of the instability. The instability was found to be due to a nonstable flame front in the catalyst bed. The flame front was stabilized by use of fine mesh catalyst on top of the catalyst bed. The fine mesh catalyst has a higher specific surface area and apparently stabilized the flame front near the top of the catalyst bed. The testing conducted on determination of the cause of the instability is described in the ensuing paragraphs.

During water flow calibrations of the showerhead injectors, it was noted that fully established turbulent streams were not being achieved and that stream breakup and oscillatory flow was occurring. Also, at certain pressure drops, approximately \pm 5°, angular movement of the stream occurred. It was concluded that a possible "hydraulic flip" phenomena was taking place in the orifices. This phenomena was alleviated by increasing the orifice length to diameter ratio from 2.5 to 8.5, contouring the orifice entrance and decreasing the velocity in the line feeding the manifold from 15 to 4 feet per second. All three of the aforementioned changes were accomplished individually and changes were noted in stream properties with each change in the injector or manifold configuration. However, none of the changes had any significant effect on the operating characteristics of the engine.

Changing the number of orifices from 1 to 9, and therefore propellant mass distribution in the bed, did not affect the operation of the engine. Changing the injector pressure drop did not appear to result in any changes in engine

operation except for one test with a 75 psid injector which did run smoothly. However, this test could not be subsequently duplicated.

Three additional thermocouples were added in the catalyst bed to define the location of the flame front. For the majority of the tests, their locations were as follows:

 T_{R1} - 0.5 inches from top of bed

T_{R2} - 0.88 inches from top of bed

T_{R3} - 1.35 inches from top of bed

 T_{R4} - At the outlet of the bed.

On almost all tests instrumented in this fashion, the temperature reached steady state values within two to three seconds and was very stable with the upper bed temperature reading the highest value. For most of the tests, the thermocouples were located radially in the center of the bed. When the thermocouples were placed near the chamber wall (approximately 0.1 inches from the wall), the temperature measurements were not markedly different from the middle of the bed location, and based on this data, channeling of the flow down the chamber wall was eliminated as a possible cause of the instability.

Analysis and testing of other variables including feed system variations, reduction of propellant manifold volume, changes in manifold velocity, and changes in catalyst size from 10-12 mesh to 12-16 mesh did not produce significant changes in engine operation.

When 0.3 inches of 20-25 mesh catalyst was placed at the top of the catalyst bed, with the remainder of the bed 12-16 mesh catalyst, stable engine operation was obtained. The conclusion was that there was a flame front instability which was not observable from the thermocouple measurements. One would suspect that determination of a flame front instability from thermocouple measurements would be extremely hard to observe. The fine mesh catalyst apparently supplies sufficient additional catalyst external surface area to stabilize the flame front on ignition. The 0.3 inches of 20-25 mesh catalyst with the remainder of the catalyst bed composed of 12-16 mesh particles, was the bed configuration utilized for all injector optimization testing.

Subsequent to the instability testing, data was received from Shell Development Company which raised a question concerning the cause of the instability. Catalyst for the program was procured in mesh sizes ranging from 6 to 40. The catalyst in the 10 to 40 mesh size was manufactured at one time in a single lot. The average metal content of the lot was 32.8 percent which was within the specification limits of 32 to 34 percent. However, when the 10 to 40 mesh catalyst was screened into mesh sizes of 10 to 20, 20 to 30, and 30 to 40, the following metal contents were obtained by analysis of the catalyst:

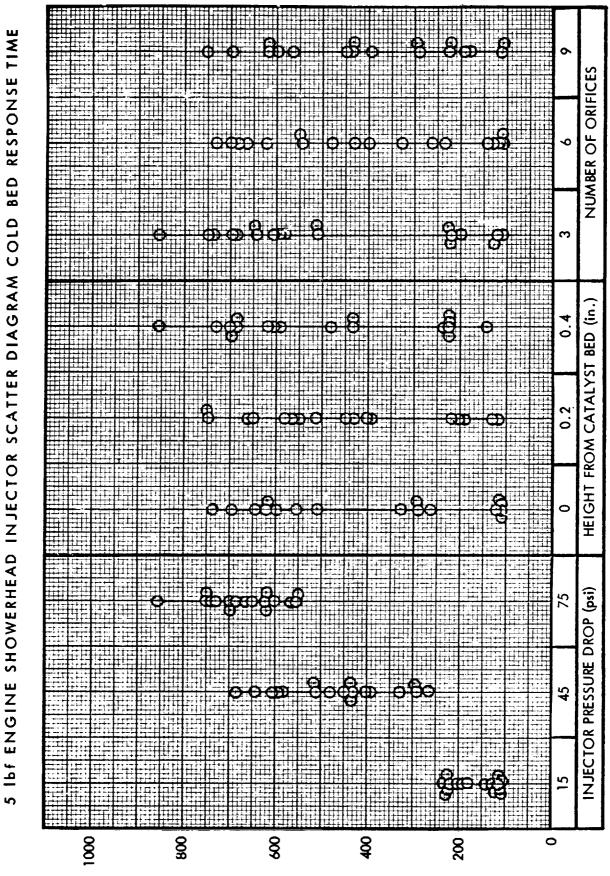
10-20 mesh	25.6%
20-30 mesh	33.6%
30-40 mesh	42.0%

Plotting the above data and extrapolating to 10 to 12 and 12 to 16 mesh catalyst, which was used in the instability tests, gives metal contents of 22 and 25 percent respectively. It was thought that perhaps the reduced metal content led to a reduction in catalyst activity and was the cause of the instability. Subsequent testing on the 50 lbf engine with other catalyst proved this hypothesis to be wrong, since the same type of instability occurred. It is obvious that manufacture of catalyst over a wide range of mesh sizes should not be accomplished in a single lot of catalyst since the fine mesh catalyst appears to absorb the active metals faster than the coarser mesh catalyst.

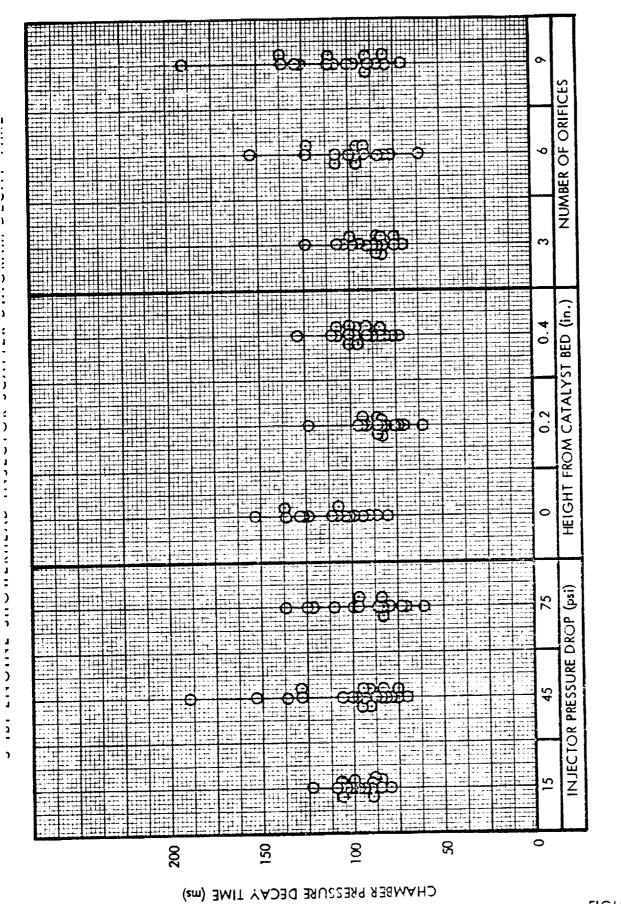
The data obtained from the showerhead injector testing is summarized in Table VI. Scatter diagrams for the reactor variables of ignition delay, cold bed response time, chamber pressure roughness, and chamber pressure decay times are plotted in Figures 20 through 23 as a function of the injector varibles. A factorial analysis of variance was performed on the data presented in each of the scatter diagrams. This allowed determination of which injector variable(s) has an effect on the reactor variable in question and also determination of interactions which exist between the injector variables. The results of these analyses are discussed in the ensuing paragraphs.

The analysis of variance conducted for the cold bed response time resulted in the following significant effects:

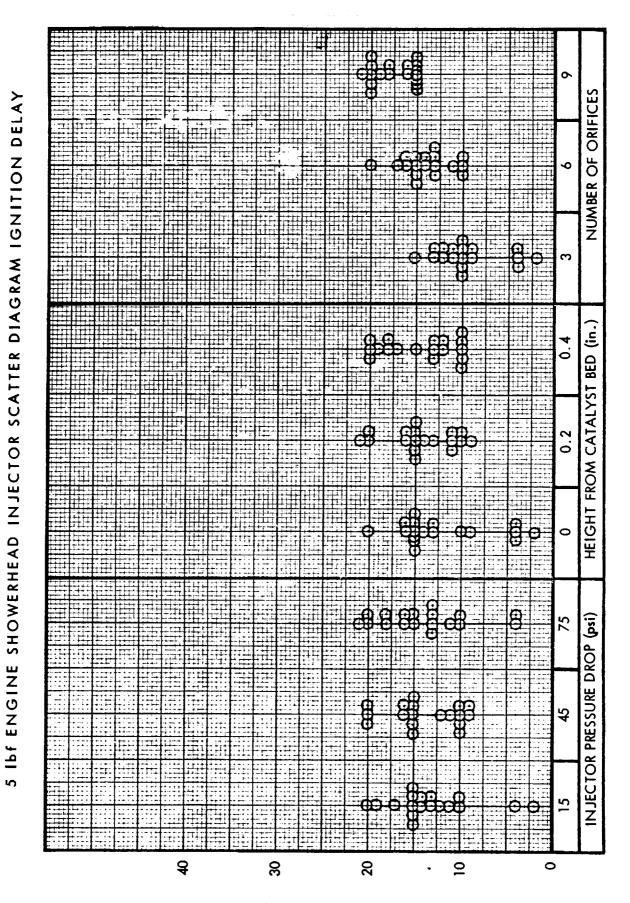
a. Cold bed response time is affected by injector pressure drop



COLD BED RESPONSE TIME (M (ms)



JECTOR VARIABLE



ICHITION DELAY (ms)

CHAMBER PRESSURE ROUGHMESS (Percent Peak-to-Peak)

IN JECTOR VARIABLE

TABLE VI 5 LBF ENGINE - TEST DATA SUMMARY - SHOWERHEAD INJECTOR

Chamber Pressure Roughness	% Peak -to-peak.	+ 2.61	+3.41	+3.40	+3.46	+ 1.62	29.T±	+2.43	+2.90	12.34	+ 2.49	± 2.05	+2.39	±2.57	+2.66	8 1	+2.73	97.1	+ 2.13	+ 6.28	±5.70	÷ 4. 10	±2.72	÷ 4.50	± 4. 10	± 3.32	+2.47	÷ 3.80	± 3.16	+3.08	+2.%	£ .⊥.	±2.12
Chember Thrust Pressure Coefficient Roughness	%	1.181	1.197	1.195	1.207	1.203	1.215	<u>.</u> .	1.209	1.209	1.202	1.202	1,215	1.225	1.209	1,216	1.204	1.236	1.185	1.211	1.216	1.205	1.207	1.218	1.210	1.202	1.218	1.209	1.203	1.226	1.22	1.217	1.213
_9	ft/sec lbf-sec/lbm (2)	151.9	153.7	156.9	157.9	155.8	155.8	i	154.5	155.1	153.9	<u></u>	156.0	156.7	154.4	156.3	158.8	158.2	154.9	154.6	155.7	158.1	156.9	158.2	157.8	154.1	155.0	154.7	152.7	156.5	156.2	157.8	1.9 <u>8</u> . I
•	ft/sec II	4140	4124	4225	4209	4158	4123		111	4127	4122	4124	4129	* : *	4104	4133	4544	4119	4191	4107	4121	4218	4181	4195	4198	4122	114	104	4083	4105	4116	4170	4139
5	¥≘	1376	1372	1351	1347	1368	1386	1372	1	1342	1385	1381	<u>\$</u>	1341	1340	1340	1321	1352	i	1419	1415	1402	1420	1429	1424	4 13	1394	13%	1398	1405	7	Ξ	1407
្ន	¥ E	1403	1392	1381	1377	1415	Ξ	1398	1347	1352	140	1407	1437	1361	1355	1359	1338	13.7	1	1 46	₹	₹	7	1494	1477	1437	ļ	į	Ì	ŀ		143	1433
_ 22	# E	1468	1468	1485	1460	<u> </u>	1516	₹	1355	1394	58	3	1524	1394	1381	1394	1394	140	!	<u> </u>	399	1881	1609	7991	1740	1479	1481	1468	1481	ŀ	*	503	-
_ - 5	¥	1580	909	₹ 8	1614	1574	1645	1578	1394	924	1623	1578	1735	15	1459	1437	344	1426	1416	1781	772	1772	18/1	1763	1740	1603	1529	1881	1594	1627	5091	1503	1516
Flow Rate	lbm/sec	0.02112	0.02060	0.02124	0.02091	0.02261	0.02226	:	0.02155	0.02206	0.02113	0.02164	0.02320	0.02308	0.02236	0.02234	0.02108	0.02310	0.02045	0.02277	0.02245	0.02121	0.02144	0.02238	0.02276	0.02225	0.02256	0.02149	0.02241	0.02289	0.02261	0.02251	0.02255
Three	ě	3.216	3.160	3.333	3.308	3.520	3.470	3.260	3.330	3,420	3.250	3.330	3.620	3.620	3.450	3.4%	3.343	3.660	3.160	3.520	3.4%	3.352	3.364	3.540	3.5%	3.428	3.496	3.316	3.422	3.581	3.531	3.551	3.520
Downstream Chamber Pressur	psió	143.5	139.4	147.3	<u>∓</u>	154.3	154.6	144.2	146.4	149.4	140.4	146.5	157.2	155.8	150.6	151.5	146.8	156.2	140.6	153.5	151.8	146.8	147.1	154.1	156.8	150.6	152.1	144.7	1.021	154.1	152.6	154.1	153.2
Upstraam Chamber Pressure	iğ.	160.4	155.4	158.5	159.3	1.69.7	6.791	159.4	161.8	164.4	150.5	162.2	169.4	171.2	165.6	7.591	161.0	172.3	i	173.3	172.2	8.591	166.4	168.3	1.2.1	166.5	170.9	160.8	164.8	170.3	168.5	0.691	168.4
Injection Pressure	. <u>ē</u>	177.1	12.0	206.3	206.3	246.9	244.7	178.9	183.9	205.4	201.9	223.9	247.1	194.2	1.081	203.7	194.3	241.2	210.4	187.1	185.9	208.3	206.9	236.3	241.2	185.4	189.7	0.661	206.8	243.2	241.5	186.3	186.1
Decay	Ė	8	102	128	83	8	<u>8</u>	107	501	53	86	123	8	9	<u>=</u>	136	<u>&</u>	137	125	8	8	75	3	3	2	76	123	*	6	19	%	8	88
Response Time	Ė	115	130	510	S 3 6	769	3 2	112	108	327	262	129	535	01.1	107	296	230	619	99	202	220	514	581	748	959	<u>8</u>	129	9	63	83	\$50	<u>8</u>	<u>86</u>
lgnit lan Delay	ė	•	2	0	٥	•	4	5	2	9	15	13	20	15	5	15	15	15	91	0	Ξ	٥	Ξ	2	01	*	15	5	15	=	9	15	15
Initial Catalyst Bed Temp.	۴	8	76	45	57	2	. 29	88	g	ત્ર	26	69	3	19	54	73	15	6 7	22	15	55	25	84	25	25	8	8	3	3	59	53	53	28
Fuel Temp.	*	79	59	38	64 53	8	8	57	35	67	3	8	58	4	25	55	\$	79	53	49	48	7	4	\$	1	જ	58	3	28	55	8	7	4
Test Code	6	1-19	1-18	81-2	81-2	6-18	?	7	7 =	5-18	81-5	81-6	9	19-7	81-7	9-7-6	8-14	6-19	6-19	61-10	81- 10	11-19	11-11	B1-12	81-12	81-13	61-13	81-14	81-14	81-15	81-15	81-16	81-16
Test No.		171-31-74	171-31-75	171-31-196	171-31-198	171-31-71	171-31-72	171-31-96	171-31-98	171-31-94	171-31-95	171-31-88	171-31-91	171-31-102	171-31-103	171-31-101	171-31-199	171-31-107	171-31-108	171-31-187	171-31-188	171-31-185	171-31-186	171-31-190	171-31-191	171-31-109	171-31-113	171-31-114	171-31-115	171-31-116	171-31-117	171-31-168	171-31-169

Chamber	Coefficient Roughness	% Peak 10-peak	+2.49	+2.48	+ 3.69	+3.47	F 5.78	+ 4.03	+2.50	12.35	+2.35	+ 2.94	+ 2.37	+2.26	+3.40	+2.70	+ 2.50	+2.70	+ 2.01	+2.01	+ 3.37	+ 2.65	+3.21	÷2.90
1	Coefficient		1.209	1.207	1.213	1.203	1.209	1.211	1.207	1.201	1.223	1.211	1.204	1,228	1.201	1.212	1.214	1.209	1.200	1.209	1.194	1.22.1	1.202	1,203
_	<u>\$</u>	lbf-rec,′lbm (2)	157.9	158.6	159.7	158.5	154.9	156.9	157.1	156.2	159.2	157.2	157.4	160.5	155.5	156.0	157.7	157.E	156.3	156.7	1.86.1	158.1	157.7	157.2
	•	ffrsec	4215	:22 5	4236	4240	4120	4168	4188	4185	4180	4176	4206	4206	4163	4139	4177	4199	4192	£91 7	4261	4167	4222	4202
1 -	3	¥:	1420	150	1407	1415	1415	1407	1402	1407	1424	1	1415	1415	1452	1393	1381	1407	1372	13R1	1381	1381	1372	1383
	3	ε۳	1448	14.8	1437	1437	1455	44 84	1442	<u>‡</u>	1459	1 40	1459	1446	1452	1415	1429	1418	1398	1407	1415	14.02	1398	1407
	7	*≘	<u>5</u>	1538	503	1516	1605	1573	1547	1560	1560	1568	1521	1561	1499	1516	1507	1516	1415	1459	1459	1424	1437	1459
, 	<u>.</u>	r:	1583	1583	1516	1547	<u>8</u>	1740	17.7	1735	1717	1762	1645	1713	1602	1685	1658	1670	1472	1490	1503	1459	1490	1516
	Flow Rate	lbm/sec	0.02174	0.02179	0.02247	0.02283	0.02241	0.02266	0.02182	0.02173	0.02266	0.02231	0.02143	0.02238	0.02156	0.02185	0.02324	0.02256	0.02144	0.02162	0.02151	0.02211	0.02237	0.02262
	Thrust	ě	3, 432	3.456	3.588	3.620	3.470	3.556	3.428	3.393	3.608	3.509	3.373	3.5%	3.352	3.408	3.064	3.560	3.352	3.388	3.400	3.496	3.523	3.556
Downstream Chamber	Pressure	g .g	150.4	151.2	156.2	158.9	151.5	155.0	150.0	149.2	155.8	152.9	147.9	154.5	147.3	148.4	159.3	156.7	149.3	149.2	149.3	151.2	155.0	156.0
Upstream Chamber	Pressure	. <u>?</u> 8.	165.6	0.791	174.1	176.3	163.7	167.9	163.4	162.1	168.7	166.4	162.3	165.2	163.2	163.5	174.7	172.1	160.7	161.5	161.7	166.4	167.9	168.8
Injection	Pressure	ž.	1%.1	5.761	241.7	244.3	178.3	182.7	208.1	206.3	239.7	235.1	180.5	28 .	201.7	202.7	246.7	242.3	179.3	179.3	1.83.1	198.7	234.9	257.1
Decay	Time	E	02	8	8	;	106	30	87	95	3	75	ş	<u>8</u>	107	25	83	22	8	8	5	128	011	64
Response	Time	Ė	3%	450	<u>3</u>	750	7:2	222	¢0°	85	98 2	855	235	142	490	589	730	700	225	27.	432	435	819	6 97
facilies	Pelay	Ë	8	ંગ	20	21	2	13	12	2	15	9	0	17	2	9	13	13	61	8	5 0	8	18	8 2
Initial Catalyst Bed	iemp.	۳	52	ឌ	46	28	%	55	şş	47	ß	48	\$	45	. \$	22	4	4	ß	59	29	23	42	99
چ چ	Temp.	y	£	2	4	43	4	4	47	49	45	33	7	40	45	46	4	39	53	15	53	53	4	25
-	Test Code	ච	71-19	11-12	81-18	91-18	91-19	91-19	81-20	91-20	12-18	81-21	g1-22	81-22	61-23	81-23	81-24	B1-24	81-25	B 1-25	B1-26	81-26	81-27	B1-27
	Test No.		171-31-172	171-31-173	171-31-174	171-31-175	171-31-210	171-51-511	171-31-212	171-31-213	171-31-208	171-31-209	171-31-205	171-31-207	171-31-200	171-31-201	171-31-202	171-31-203	171-31-218	171-31-219	171-31-216	171-31-217	171-31-214	171-31-215

T_{c1}, T_{c2}, T_{c3}, and T_{c4} are steady-state temperature measurements located at 0.5, 0.88, 1.35, and 1.75 inches from the top of the catalyst bed.
 Nozzle Expansion Ratio is 4.55:1
 Refer to Figure 1 for identification of test code.

- Cold bed response time is affected by the height from the catalyst bed
- c. Cold bed response time is affected by the number of orifices.

In Figure 24 cold bed response time data for all distances from the catalyst bed has been averaged at each pressure drop and is plotted versus injector pressure drop for the 3, 6, and 9 orifice injectors. An increase in cold bed response time with pressure drop is obvious from the curves.

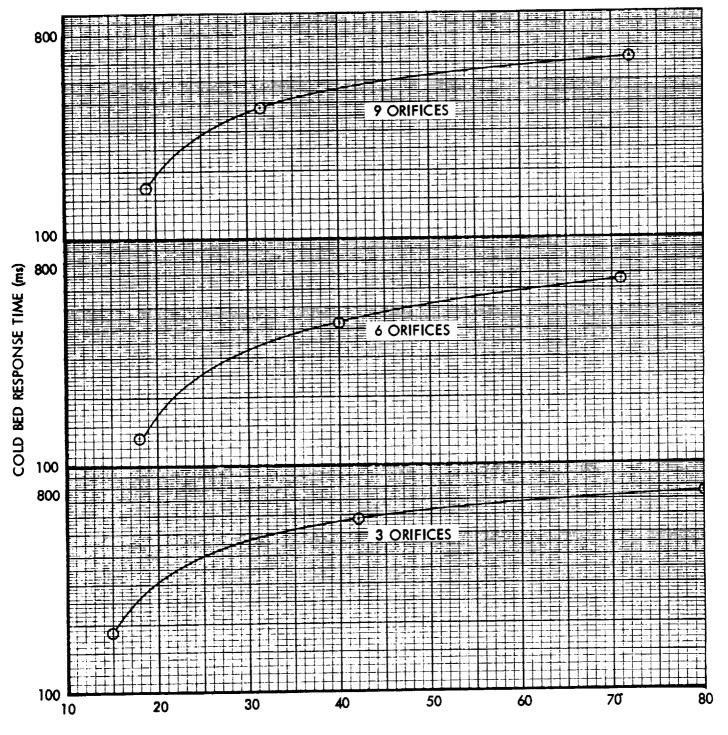
Figure 25 is a plot of average cold bed response time (average of data at all pressure drops) versus distance from the catalyst bed for the 3, 6, and 9 orifice injectors. It is seen that cold bed response times increase as the injector is moved away from the catalyst bed. This effect is very small for the 3 orifice injector but it is significant for the 6 and 9 orifice injectors.

Figure 26 is a cross plot of data in Figure 24 and depicts cold bed response time versus number of injector orifices for pressure drops of 20, 45, and 70 psid. It is seen that a minimum in cold bed response times exists with the 6 orifice injector at a pressure drop of 20 psid. At 45 and 70 psid pressure drop, the 6 and 9 orifice injectors have essentially the same response times which are both lower than the 3 orifice injector.

The analysis of variance conducted on the ignition delay data presented in the scatter diagram in Figure 22 resulted in the following observations:

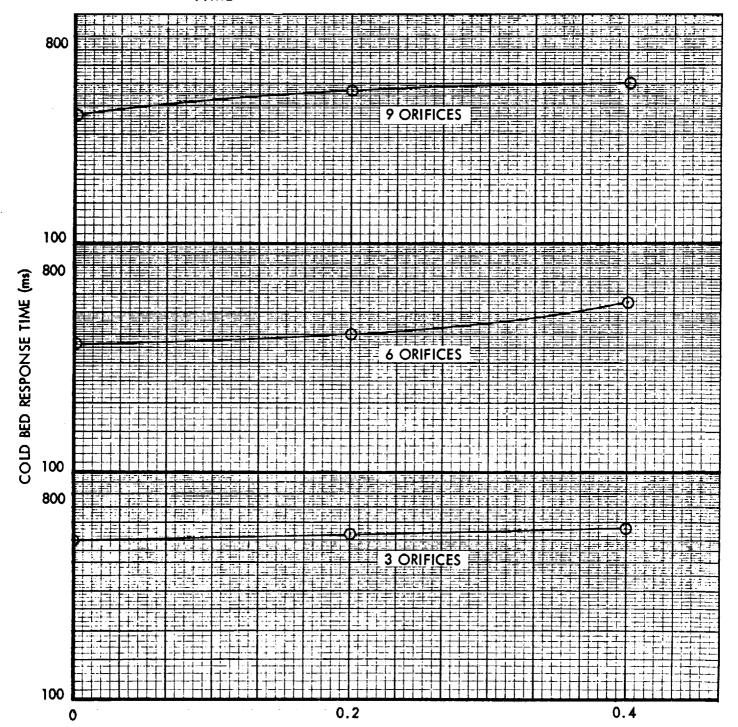
- a. Ignition delay is affected by the number of injector orifices.
- b. Ignition delay is not affected by injector pressure drop.
- c. Ignition delay is affected by the distance of the injector from the catalyst bed.
- d. An interaction exists between the injector pressure drop and the injector distance from the catalyst bed.
- e. An interaction exists between the number of orifices and distance from the catalyst bed.
- f. An interaction exists between the number of orifices, injector pressure drop, and injector distance from the catalyst bed.

5 16 ENGINE SHOWERHEAD INJECTOR AVERAGE COLD BED RESPONSE TIME VS INJECTOR PRESSURE DROP



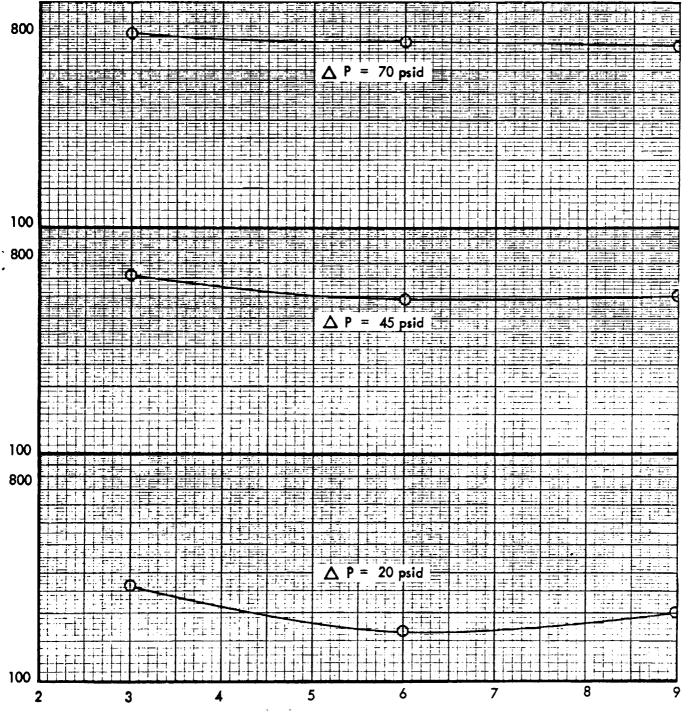
INJECTOR PRESSURE DROP (psid)

5 1bf ENGINE SHOWERHEAD INJECTOR AVERAGE COLD BED RESPONSE TIME VS DISTANCE FROM CATALYST BED



DISTANCE FROM CATALYST BED (inches)

5 16 ENGINE SHOWERHEAD INJECTOR AVERAGE COLD BED RESPONSE TIME VS NUMBER OF ORIFICES



NUMBER OF ORIFICES

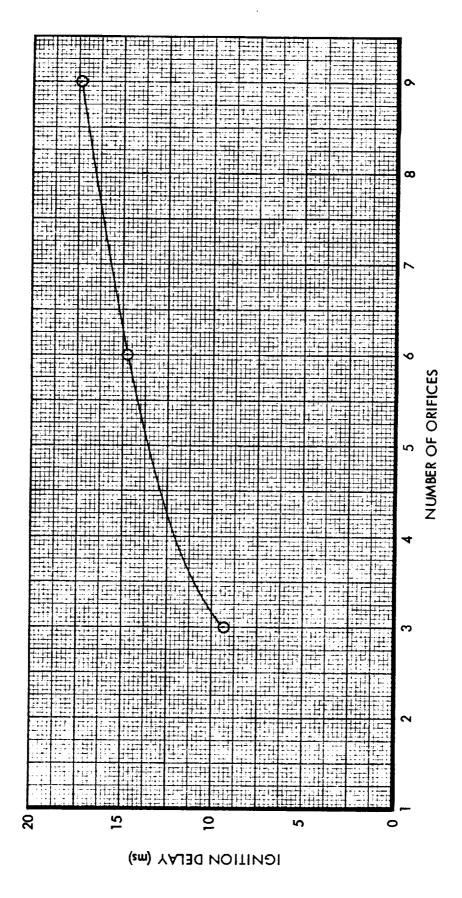
The interactions which exist between the injector variables make it difficult to come to definite conclusions regarding the effect of the variables on ignition delay. Figure 27 is a plot of average ignition delay versus the number of orifices. A definite increase in ignition delay is noted as the number of orifices is increased. The reason for this increase is not completely understood. With the 6 orifice injector, ignition delay decreases as the distance between the injector and the catalyst bed is increased. With the 3 and 9 orifice injectors ignition delay increases with distance from the catalyst bed. This information is presented in Figure 28, where ignition delay is plotted versus the distance of the injector from the catalyst bed for the 3, 6, and 9 orifice injectors.

The analysis of variance conducted on the chamber pressure decay time data presented in the scatter diagram of Figure 21 resulted in the following conclusions:

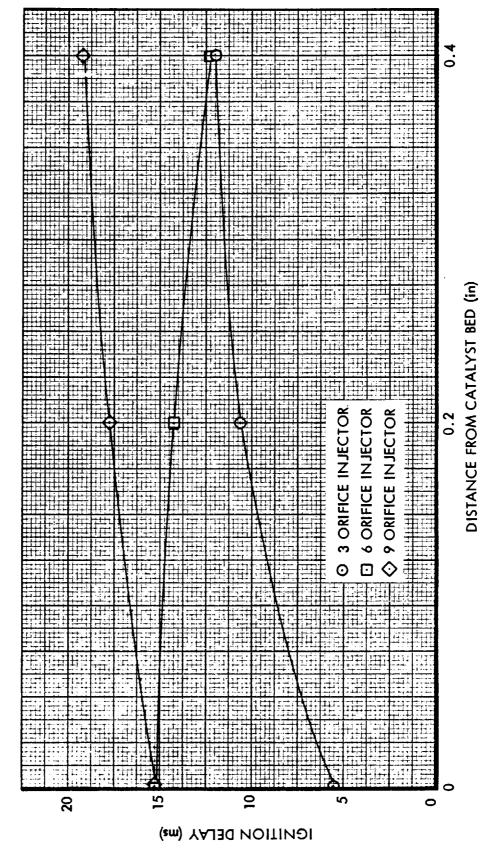
- a. Chamber pressure decay time is not affected by injector pressure drop.
- b. Chamber pressure decay time is significantly affected by the height from the catalyst bed.
- c. The number of injector orifices has an effect on the decay times.
- d. There is an interaction between the number of orifices and the distance from the catalyst bed.

In Figure 29 chamber pressure decay time is plotted versus the number of injector orifices for distances of the injector from the catalyst of 0, 0.2, and 0.4 inches. From this figure it is seen that the decay times increase with number of orifices with the injector flush and 0.4 inches from the catalyst bed. With the injector 0.2 inches from the bed the decay time is a maximum with the 6 orifice injector. The increase in decay time noted is probably due to the test configuration employed. As the number of orifices was increased, the propellant manifold diameter was increased to provide flow to the orifices. The manifold diameter was held only slightly larger than the orifice pattern diameter so that no areas of stagnant flow would exist in the manifold. Calculations indicate that the increase in holdup propellant volume as the number of

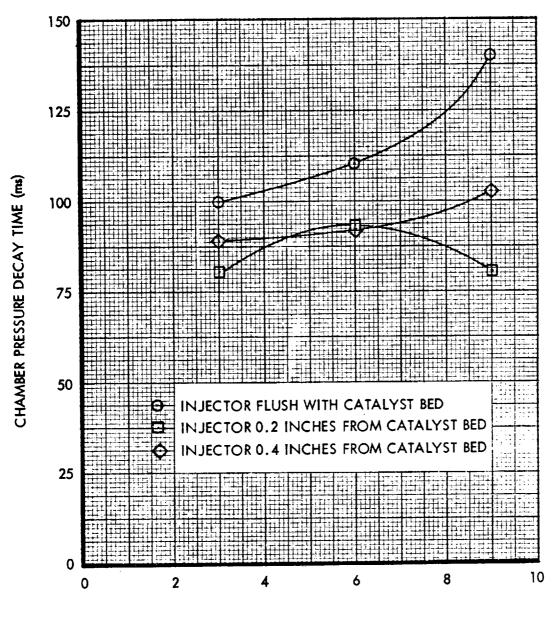
5 Ibf ENGINE SHOWERHEAD INJECTOR AVERAGE IGNITION DELAY VS NUMBER OF ORIFICES



5 Ibf ENGINE SHOWERHEAD INJECTOR AVERAGE IGNITION DELAY VS DISTANCE FROM CATALYST BED



5 16 ENGINE SHOWERHEAD INJECTOR AVERAGE CHAMBER PRESSURE DECAY TIME VS NUMBER OF ORIFICES



NUMBER OF ORIFICES

orifices is increased is probably sufficient to account for the increase in tailoff noted. Thus it would appear that if the holdup propellant volume had been held constant, no change in decay time with number of orifices would have occurred. The main effect on decay time is then the distance from the catalyst bed wherein decay times are lower with a 0.2 inch void between the injector and the catalyst bed than with the injector flush or 0.4 inches from the bed.

The analysis of variance conducted on the chamber pressure roughness data shown in Figure 23 indicates that all injector variables have a significant effect on the chamber pressure roughness and that interactions exist between all variables. This makes any general conclusions about chamber pressure roughness impossible. However, the following trends are noted in the data:

- a. With the injector flush with the catalyst bed, chamber pressure roughness decreases slightly with increased injector pressure drop for all orifice patterns.
- b. With the injector 0.2 inches from the catalyst bed, roughness decreases with increased pressure drop for the 3 orifice pattern, is essentially constant for the 6 orifice pattern, and increases with pressure drop for the 9 orifice pattern.
- c. With the injector 0.4 inches from the catalyst bed the same trends in (b) above appear.
- d. Increasing the number of orifices from 3 to 6 lowers the chamber pressure roughness. Virtually no difference exists between the 6 and 9 orifice injectors.

In a few of the tests, some pressure spikes of approximately 50 to 60% of steady state chamber pressure occurred. In general these spikes would occur when the catalyst bed was freshly packed. Slight additional packing of the bed, which occurs during operation appeared to eliminate the spikes. These results indicate catalyst bed porosity has a definite effect on engine operation.

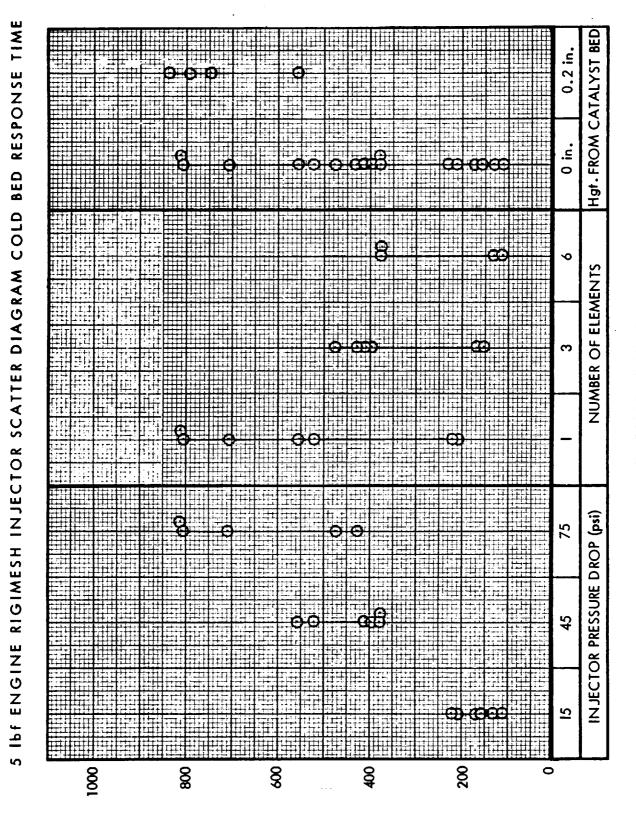
No variation in engine performance was noted when the injector pressure drop or number of orifices was varied. Slight increases in performance (0.5%) were noted when the injector was moved away from the bed, but it is not felt that this increase is significant. Characteristic velocity averaged 4,164 feet per second, specific impulse averaged 156.5 lbf-sec/lbm, and the thrust coefficient averaged 1.209 for the 54 tests tabulated in Table VI.

6.2.4 5 lbf Engine Rigimesh Injector

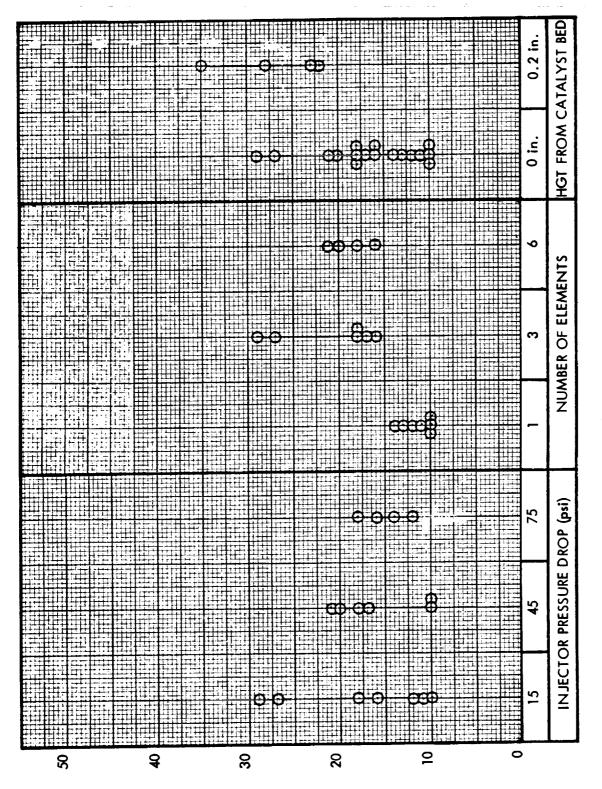
Testing of the rigimesh injector was conducted with 1, 3, and 6 element injectors each at 15, 45, and 75 psid pressure drop. Tests of each injector configuration were made with the injector flush with the catalyst bed and the 6 element injector was tested 0.2 inches away from the catalyst bed at 15 and 45 psid pressure drops. The test data obtained is summarized in Table VII. Scatter diagrams of the data for the reactor variables cold bed response time, ignition delay, chamber pressure decay time, and chamber pressure roughness are plotted in Figures 30 through 33.

From the scatter diagram in Figure 30, it is seen that cold bed response times increase with injector pressure drop. Figure 34 depicts cold bed response time plotted versus injector pressure drop for the 1, 3, and 6 element injectors. It is noted that the response times for the single element injector are significantly higher than those for the 3 and 6 element injectors. When the 6 element injector was moved 0.2 inches from the catalyst bed the start transient was very erratic and the response times increased by a factor of approximately 3. The cold bed response times with the rigimesh injector flush with the catalyst bed are similar to those with the showerhead injector.

The scatter diagram for ignition delay in Figure 31 indicates that ignition delay is affected by the number of orifices and injector distance from the catalyst bed. It is seen that the single element injector has ignition delay times all lower than the 3 and 6 element injectors. This same phenomena was noted with the showerhead injector and is not fully understood. Moving the injector away from the catalyst bed 0.2 inches produced marked increases in the ignition delay time.



COLD BED RESPONSE TIME (ms)



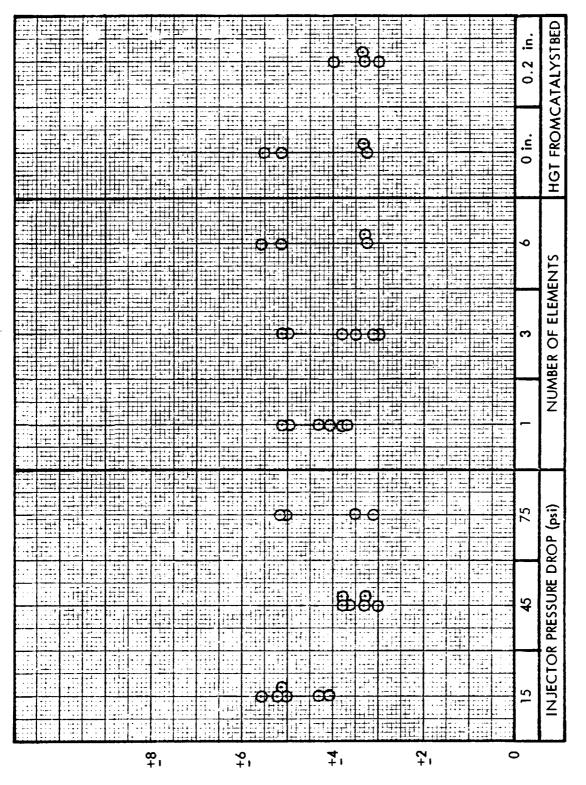
ICHILION DELAY (ms)

INJECTOR VARIABLE

11760

5 Ibf ENGINE RIGIMESH INJECTOR SCATTER DIAGRAM DECAY TIME

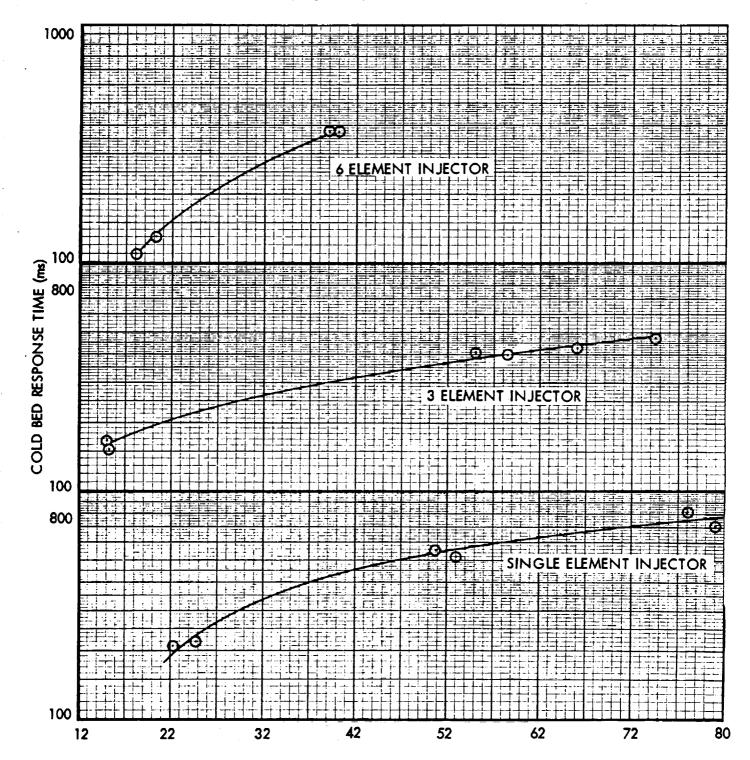
DECAY TIME (ms)



CHAMBER PRESSURE ROUGHMESS (Percent Peak-to-Peak)

INJECTOR VARIABLE

5 16 FENGINE RIGIMESH INJECTOR COLD BED RESPONSE TIME VS INJECTOR PRESSURE DROP



INJECTOR PRESSURE DROP (psid)

5 LBF ENGINE - TEST DATA SUMMARY - RIGIMESH INJECTOR TABLE VII

Chamber Pressure aughness	% Peak to peak	+4.30	+ 4.04	±3.71	+3.79	₹ 5.01	± 5.05	± 5.07	±5.01	±5.12	÷3.80	÷3.00	÷3.50	±3.71	+ 5.59	±5.17	+3.27	+3.31	+3.8	± 3.35	+3.00	+3.30
Chamber Thrust Pressure Coefficient Roughness	6	1.1%	1.213	1,210	1.204	1.218	1.210	1.219	1.208	1.208	1.216	1.210	1.223	18	1.180	.18	1.203	1.211	1.1%	1.175	1.206	1.206
_ _	fı/sac İbf~sec/İb.n	156.4	158.4	155.9	156.0	159.2	128.1	159.3	157.6	155.9	157.3	156.6	160.4	153.5	152.7	154.6	156.9	158.7	158.5	157.4	9.091	161.0
•0	fi/sec II	4207	4201	4145	4167	4207	4202	4504	4198	4153	4162	4163	4220	4170	4164	4166	4197	4218	4263	4309	4286	4297
72	# @	1372	1372	1420	1433	1340	1351	1334	1320	1338	1402	1390	1402	1402	1359	1359	1334	1338	12%	1297	1329	1316
1.3	₽ <u>8</u>	1398	1394	1463	1490	1359	1368	1359	1334	1364	1424	1415	1424	1424	1385	1381	1347	1359	1329	1359	1329	1381
1.2	¥ <u>8</u>	1472	1503	<u>5</u>	1694	1407	1424	1407	1359	1437	1525	1516	1536	1543	₹ 9	1437	1394	1394	1346	1340	1381	1351
7-	¥ &	1605	1623	1735	1694	Ξ	1503	1494	1364	1437	0691	1667	1735	1749	1503	1459	1450	1446	1394	1338	1429	1394
Flaw Rate	lbm/sec	0.02104	0.02245	0.02258	0.02198	0.02168	0.02113	0.02102	0.02170	0.02150	0.02278	0.02191	0.02316	0.02138	0.01962	0.02122	0.02218	0.02180	0.02050	0.01899	0.021341	0.021443
Thrust	βę	3.291	3.556	3.519	3,428	3.452	3,340	3.347	3.420	3.352	3.584	3.431	3.715	3.282	2.996	3.280	3.480	3.460	3.204	2.988	3.420	3.453
Downstream Chamber Pressure	.g.	145.3	154.8	153.6	150.3	149.7	145.7	145.0	149.5	146.5	155.6	149.7	160.4	146.3	134.1	145.1	152.3	150.9	- 4	154.3	150.1	151.2
Upstream Chamber Pressure	g. io	155.3	6.791	170.9	164.8	167.0	162.2	163.3	9.191	162.7	169.4	162.6	173.0	162.1	150.5	161.6	162.6	1.291	157.4	149.7	165.4	4.591
Injection Pressure	g ë	178.8	192.5	216.1	209.1	245.9	244.1	242.5	179.7	182.5	232.5	223.7	242.9	230.3	174.1	181.3	20.13	200.7	185.5	185.9	203.1	202.5
Decay Time	Ę	170	160	117	9	118	123	127	250	92	128	<u>8</u>	210	217	250	250	218	<u>8</u>	810	1150		700
Response Time	É	210	220	520	554	707	810	808	521	167	398	403	472	427	110	130	375	375	555	7,80	832	745
lgnition Delay	Ĕ	=	9	2	2	12	7	5	29	27	82	17	81	92	9	18	21	23	28	35	23	22
Initial Catalyst Bed Temp.	ů.	7	47	49	\$	45	47	42	50	55	8	9	S	S	8	55	8	57	8	55	5	59
Temp.	8 .	\$	9	4	4	42	45	45	1	45	53	47	4	4	5.	47	8	45	\$	4	4	48
Test Code	ε	15-0-1	15-0-1	45-0-1	45-0-1	75-0-1	75-0-1	75-0-1	15-0-3	15-0-3	45-0-3	45-0-3	75-0-3	75-0-3	15-0-61	15-0-6	45-0-6	45-0-6	152-6			452-6
Test No		171-31-166	171-31-167	171-31-159	171-31-160	171-31-176	171-31-177	171-31-178	171-31-170	171-31-171	171-31-155	171-31-156	171-31-157	171-31-158	171-31-161	171-31-162	171-31-164	171-31-165	171-31-162	171-31-183	171-31-180	171-31-181

(1) First number refers to nominal injector pressure drop. Second number refers to distance of injector from catalyst bod. The third number refers to the number of injector elements. (2) T_{c1} , T_{c2} , T_{c3} , and T_{c4} are steady-state temperature measurements located 0.5, 0.88, 1.35, and 1.75 inches from the top of the catalyst bed. (3) Nazzle Expansion Ratio is 4.55:1

The scatter diagram for chamber pressure decay time in Figure 32 indicates an increase in decay time with number of rigimesh elements. As was explained with the showerhead injector this is thought to be due to increased manifold propellant holdup as the number of elements increased. When the injector was moved 0.2 inches from the catalyst bed, the decay times increased by a factor of 3 to 5 as is seen from the data in Table VII.

From the scatter diagram in Figure 33 it is seen that chamber pressure roughness decreases as pressure drop is increased. In general, the rigimesh injector gave higher chamber pressure roughness at all conditions than did the showerhead injector. The engine ran fairly smooth with the injector 0.2 inches from the catalyst bed, once the start transient was over. During the start transient rough and erratic operation was obtained.

No change in engine performance was noted during the tests when the injector parameters were varied. Characteristic velocity averaged 4,183 feet per second for the 18 tests. Specific impulse averaged 156.8 lbf-sec/lbm and the thrust coefficient averaged 1.206. These performance numbers are almost identical to those obtained with the showerhead injector.

6.2.5 50 lbf Engine Showerhead Injector

The first test on the 50 lbf engine was conducted with the shower-head injector utilizing a catalyst bed composed entirely of $1/8 \times 1/8$ inch cylindrical pellets. Chamber pressure oscillations of \pm 40 psia peak-to-peak at a frequency of 10 cps occurred throughout the test. The instability was similar to that noted on initial tests with the 5 lbf engine. A series of tests was conducted with various sizes and bed lengths of granular catalyst at the top of the catalyst bed. This testing is summarized in Table VIII. Stable start transient and steady state operation were achieved when 0.2 inches of 25-35 mesh catalyst was used on the top of the catalyst bed. The remainder of the catalyst bed (2.48 inches) was composed of $1/8 \times 1/8$ inch cylindrical pellets.

Tests conducted with the showerhead injector consisted of tests with 20, 40, and 60 orifice injectors at pressure drops of 15, 45, and 75 psid with each orifice pattern. Each pressure drop and each orifice pattern

TABLE VIII SUMMARY OF 50 LBF ENGINE CATALYST PARTICLE SIZE STUDIES

Test No.	INJECTOR TYPE	CATALYST BED CONFIGURATION	TEST RESULTS
171-31-118	20 Hole Showerhead 45 psid pressure drop	Entire bed composed of $1/8^{\alpha} \times 1/8^{\alpha}$ cylindrical pellets.	Chamber pressure ascillations of \pm 40 psia occurred throughout test of 5 seconds duration. Frequency of escillations was 10 cps.
171-31-119	20 Hole Showerhead 45 psid pressure drop	0.3 inches of 16-20 mesh catalyst on top of bed. Remainder of bed $1/8^{\circ} \times 1/8^{\circ}$ cylindrical pellets.	Chamber pressure oscillations of $\frac{1}{2}$ 5 psia occurred one second after start. Frequency of oscillations was 20 cps. Oscillations would damp out and then reappear. Test duration was 5 seconds.
171-31-120	20 Hale Shawerhead 45 psid pressure drop	0.36 inches of 12-16 mesh catalyst on top of bed. Remainder of bed $1/8" \times 1/8"$ cylindrical pellers.	0.36 inches of 12-16 mesh catalyst on top of bed. Chamber pressure oscillations of ± 18 paid occurred 0.6 seconds after start and remained throughout Remainder of bed 1/8" x 1/8" cylindrical pel the test of 21 seconds duration. Frequency of oscillations was 18 cps.
171-31-121	20 Hole Showerhead 45 psid pressure drop	0.36 inches of 16-20 mesh catalyst on top of bed. Remainder of bed $1/8^{\prime\prime}\times1/8^{\prime\prime}$ cylindrical pellets.	0.36 inches of 16-20 mesh catalyst on top of bed. Chamber pressure oscillations of ±5-6 psid occur 0.8 seconds after start. Oscillations tend to damp Remainder of bed 1/8" x 1/8" cylindrical pel- out and stable operation is achieved at end of 30 second test. Frequency of oscillations is 23.5 aps. lets.
171-31-122	20 Hole Showerhead 45 psid pressure drop	0.4 inches of 16-20 mesh catalyst on top of bed. Remainder of bed $1/8^{\rm H} \times 1/8^{\rm H}$ cylindrical pellets.	Chamber pressure oscillations varying from ± 4 to ± 8 psid occurred 1.5 seconds after start and remained for the total test of 30 seconds duration. Frequency of oscillations was 25 cps.
171-31-123	20 Hole Showerhead 45 psid pressure drop	0.2 inches of 25-35 mesh catalyst on top of bed. Remainder of bed $1/8^{\circ} \times 1/8^{\circ}$ cylindrical pellets.	Chamber pressure oscillations of ±4 psia at a frequency of 20 cps occurred for first 5 seconds of test. The oscillations then damped out to ±3 psia of random oscillations for remainder of test of 23 seconds duration.
171-31-124	20 Hole Showerhead 45 psid pressure drop	Same as Test No. 171-31-123, Bed not un- packed from previous test.	Chamber pressure oscillations of ±4 to ±8 psia occurred for first 3 seconds of test at frequency of 20 cps. The ascillations then damped out to ±3 to 4 psia of random ascillations for remainder of test of 21 seconds duration.
171-31-125	20 Hole Showerhead 45 psid pressure drop	Same as Test No. 171-31-123. Bed not un- packed from previous test.	Stable operation throughout test of 5 seconds duration. Random ascillations of $\frac{1}{2}$ 3 psid.

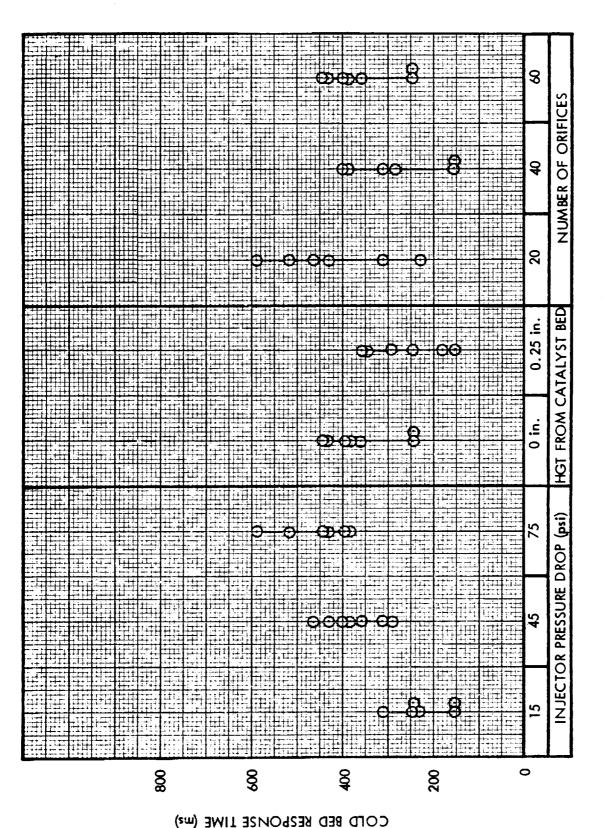
was tested with the injector flush with the top of the catalyst bed. The 60 hole pattern injector was tested at 15, 45, and 75 psid with the injector 0.25 inches from the top of the catalyst bed. The test data obtained from this testing is summarized in Table IX.

Scatter diagrams for the reactor variables of ignition delay, response time, chamber pressure roughness, and chamber pressure decay time are plotted in Figures 35 through 38 as a function of the injector variables.

Examination of the scatter diagram in Figure 35 indicates an increase in cold bed response time as the injector pressure drop is increased. Cold bed response time is plotted versus injector pressure drop in Figure 39. The scatter diagram also indicates that the response time with the 40 orifice injector is lower than that with the 20 or 60 orifice injectors. Statistical analysis was applied to this data to determine whether the differences were significant. This analysis concluded that with a confidence level of 90% the differences were significant. A confidence level of 95% gave a negative result of significance, which probably is due to the small number of the sample. Figure 40 is a cross plot of the data in Figure 39 and depicts average cold bed response time versus the number of orifices. It is seen that a minimum exists with the 40 orifice injector at each pressure drop studied. The data in the scatter diagram indicates a possible decrease in response time when the injector is moved 0.25 inches from the catalyst bed. Statistical analysis of this data indicated no significant difference at the 90% confidence level.

No significant difference was noted in ignition delay, chamber pressure roughness, or chamber pressure decay time as the injector parameters were varied. Chamber pressure roughness decreased slightly with increased pressure drop and when the injector was moved 0.2 inches from the catalyst bed, but the differences are not significant. This is seen in Figures 41 and 42 where chamber pressure roughness is plotted as a function of injector pressure drop.

There was no observable change in engine performance as the injector parameters were varied. The average characteristic velocity for the 27 tests tabulated in Table IX is 4,237 feet per second. Specific impulse averaged 158.1 lbf-sec/lbm and the thrust coefficient averaged 1.201.



NJECTOR VARIABLE

CHAMBER PRESSURE ROUGHNESS (Percent Peak-to-Peak)

							92	GĐ	(0 in. 0.25 in.
							5 €		6				22
المشاشة		+++		1						;;;;; ;;;;;			15 45

INJECTOR VARIABLE

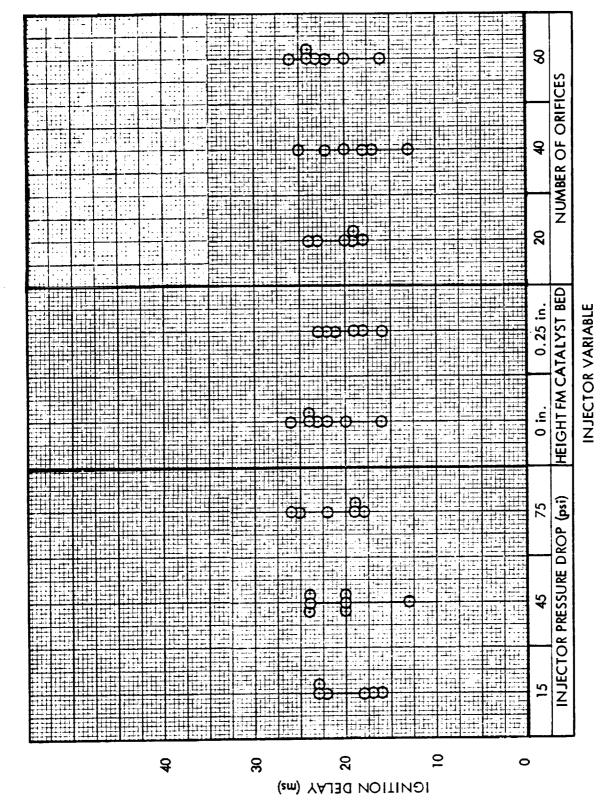
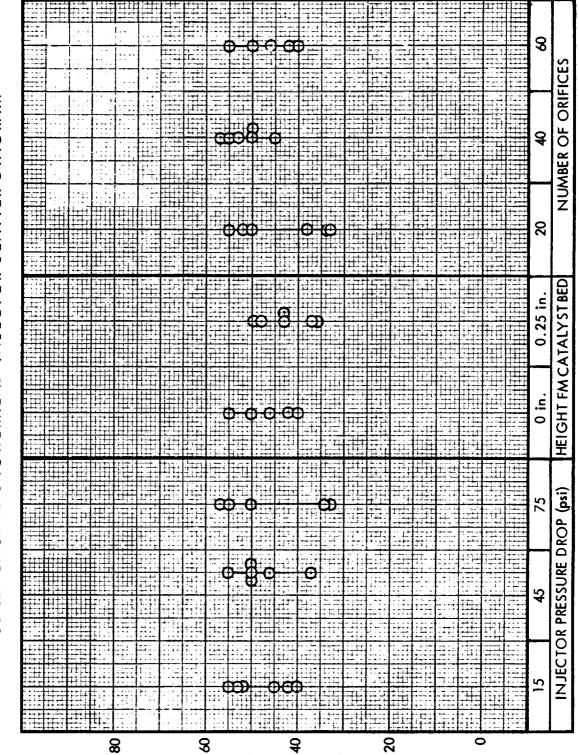


FIGURE 37

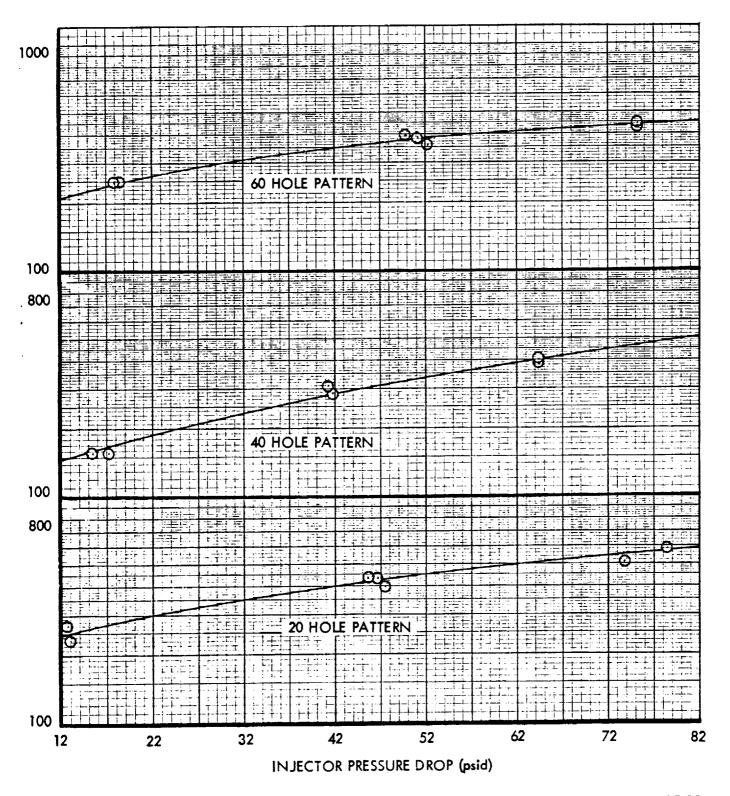
CHAMBER PRESSURE DECAY TIME (ms)





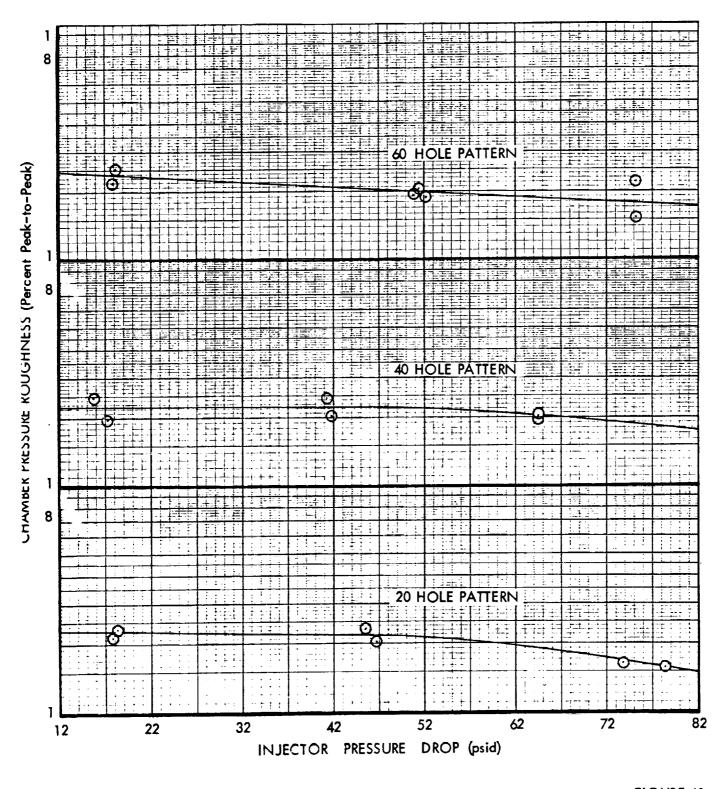
INJECTOR VARIABLE

50 Ibf ENGINE SHOWERHEAD INJECTOR COLD BED RESPONSE DATA VS INJECTOR PRESSURE DROP



15 psid⊞ 45 psid 50 16 ENGINE SHOWERHEAD INJECTOR COLD BED RESPONSE TIME VS INJECTOR PRESSURE DROP NUMBER OF ORIFICES COID BED RESPONSE TIME (Milliseconds)

50 1bf ENGINE SHOWERHEAD INJECTOR CHAMBER PRESSURE ROUGHNESS VS INJECTOR PRESSURE DROP



50 Ibf ENGINE 60 HOLE SHOWERHEAD INJECTOR CHAMBER PRESSURE ROUGHNESS VS INJECTOR PRESSURE DROP

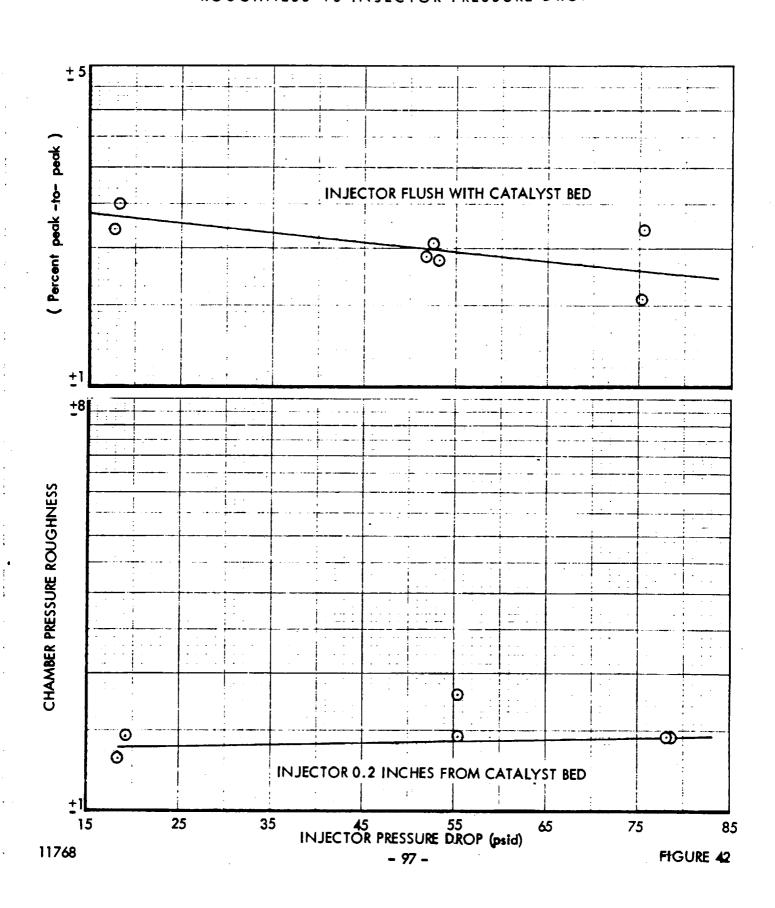


TABLE IX SO LBF ENGINE - TEST DATA SUMMARY - SHOWERHEAD INJECTOR

Test Code	8	15-0-20	15-0-20	45-0-20	45-0-20	45-0-20	75-0-20	75-0-20	15-0-40	15-0-40	45-0-40	45-0-40	75-0-40	75-0-40	15-0-60	15-0-60	45-0-60	45-0-60	45-0-60	75-0-60	75-0-60	1525-60	1525-60	4525-60	4525-60	07-35	09-07-07	7525-60	R07:-€/
Chamber Pressure Roughness	% Peak to -peak	± 1.05	± 2.13	± 2.03	+2.36	1.22	÷ 1.56	1.62	± 2.18	96.1±	±2.45	±2.01	± 2.03	± 2.03	± 2.19	± 2.52	£ 1.93	+ 1.89	2.05	1.52	±2.19	1.43	1.30	£.	-1.47	<u>}</u>	9 ; - 1	+ 2.29	1.45
ى سى	å* (E)	1.200	1.201	1.200	1.200	1.194	1 215	1.210	1.214	1.209	1.197	1.195	1.191	1.196	1.195	1.196	1.204	1.204	1.194	1,198	1.200	1.200	1.206	1,203	1 211	1.4.	ર ર	1.202	1.204
Specific	lbf-sec.Tkm (1)	154.32	156.90	159.51	158.30	157.61	159.86	159.07	160.40	158.46	157.60	158.16	157.35	158.67	156.81	156.37	159.09	158.21	156.03	157,85	157.09	157.89	159.07	158.35	73 634	\$ 50	158.42	157.71	159.24
ŧ	\$	4243	4203	4278	4242	4247	4234	4228	4251	4226	4237	4257	4255	4268	4222	4205	42.2	42.26	4222	4240	4210	4205	4242	42.07	177	1774	4243	4221	4253
Flow Rate	lbm, sec	0.22107	0.22479	0.21365	0.21106	0.21591	0.23395	0.22569	0,21122	0.22331	0.21529	0.21687	0.21580	0.21557	0.21938	0.22176	0.21202	0.21730	0.21471	0.22063	0.22089	0.22927	0.22348	0 2245	2,24,50	0.274	0.22472	0,27383	0.22608
Thrust	1 9	35.00	35.27	34.08	33.41	3,40	37.40	35.90	33.88	35.47	33.93	34.30	33.96	34.20	34.40	34.68	33,73	34.38	33.63	34.83	34.70	36.20	35.35	35 55		35.8	35.60	35.30	36.00
Downstream Chamber Pressure	ei g	151.6	152.7	147.7	141	148.2	160.1	154.2	145.1	152.3	147.4	149.2	148.4	148.7	149.7	150.7	145.7	7 2	5.41	151.2	150.3	154.0	5.55) (SC)	153.1	1.451	152.7	155.4
Upstream Chamber Pressure	Ğ	175.7	177.6	167.5	0 291	12.	185.9	180.1	170.4	177.3	172.4	172.8	171.6	172.0	177.1	180.4	174.3	174.2		177.8	177 2	174.7	120.4	9.4.	1.6.1	174.7	175.9	177.8	175.9
Tailoff Time	Ė	62	99	\$ 5	3 5	;	4	. 	છ	\$3	3	8	: 3	29	25	;	; ;	75	3 4	3 8	3 1	3	'n	3 1	K	53	\$	230	47
Response Time	Ę	312	230	F 55	7	3	6	516	155	551	311	287	3%	388	247	247	8	0 20	100	2, 27	•	‡ 3	ָרָבָּ בַּי	k /)	242	248	355	427	¥
gnition Delay	Ė	<u> </u>	: ;	3 2	.	3	! 2	<u> </u>	. 1	. 22	1 2	2	3 ₹	9	2 2	i 4	2 ?	2 2	* 6	3 2	2 2	77	≥ :	<u>•</u>	23	18	23	20	21
Initial Catalyst Temperatura	,	ŗ	? ;	3 ,8	ò	; ;)	8 -6	3 %	3 ≨	3 %	2 3	\$ S	; 3	\$ \$	3	\$ 5	ò	ž (3 8	2 :	\$	2 1	36 .	22	23	73	64	. 2
Fuel Temperature	ų.	y ,	? :	\$;	<u>,</u>	.3 :	<u>.</u>	Ç `)	٦.5	: \$	3 :	י ל) ³	ė 4	ę i	ş ;	<u>.</u>	3 :	:A :	2 :	7	15	97	64	જ	ē	; 5	នេ
Injector Fuel Pressure Drop Temperature	8	:	. · ·	- 1	46./	45.7	1.74	? ? ?	13.7		. :	; ;	7. 7	3 3	: E	^ ·	70		52.1	5).1	75.3	5.0°	٠.9I	18.5	55.6	55.6	4	4	6, 80
Z Z			C*1-1:-1:4	171-31-146	171-31-120	171-31-127	171-31-128	171-31-142	1/1-31-143	251-15-171	101 10 121	C1 - 1 C - 1 / 1	751-15-171	621-18-171	061-16-171	171-31-140	171-31-141	171-31-133	171-31-136	171-31-137	171-31-138	121-31-136	171-31-152	171-31-153	171-31-147	171-31-148	171140	121 21-150	171-31-151

Nozzle Expansion Ratio 4.03:1
 Pirst number refers to nominal injector pressure drop. Second number refers to injector distance from catalyst bed. Third number refers to number of critices.

Examination of the test data in Table IX indicates that test number 171-31-150 has appreciably longer rise and tailoff times than do tests 171-31-149 and 171-31-151 even though all three tests were with the same injector. For test 171-31-150, a 10 x 10 mesh screen of 0.025 inches wire diameter was placed on top of the 60 mesh screen used as the upper bed support. The addition of the 10 mesh screen apparently supplied volume where hydrazine could collect and resulted in the longer observed rise and tailoff times.

6.2.6 50 lbf Engine - Rigimesh Injector

Testing of the rigimesh injector was conducted with injectors having 7, 13, and 19 elements at 15, 45, and 75 psid nominal pressure drop with each injector. Tests of each injector configuration were made with the injector flush with the catalyst bed. The 13 element injector was also tested at 0.25 inches from the catalyst bed at pressure drops of 15 and 75 psid. The test data obtained is summarized in Table X. Scatter diagrams of the data for cold bed response time, ignition delay, chamber pressure decay time, and chamber pressure roughness are plotted in Figures 43 through 46.

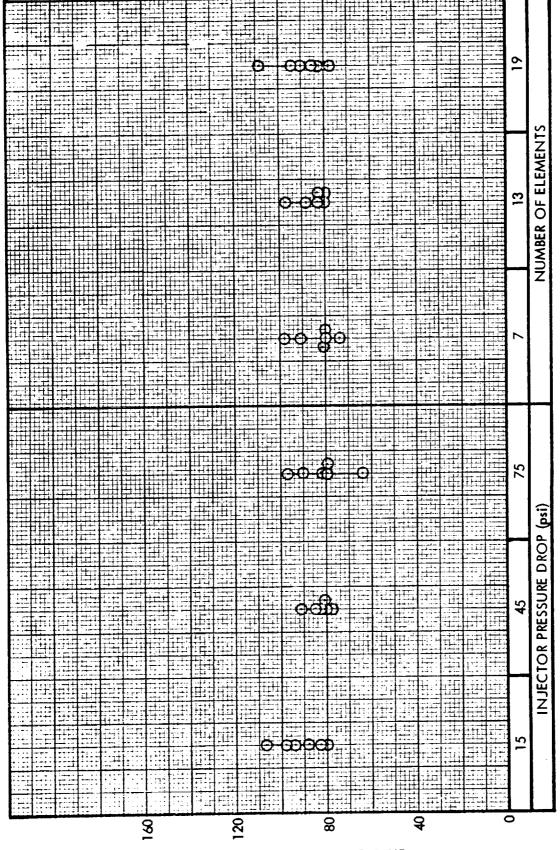
Figure 47 presents a plot of average cold bed response time versus injector pressure drop. An increase in response time with injector pressure drop is noted. The response times with the rigimesh injector are similar to or slightly better than those with the showerhead injector. The response times with the rigimesh injector do not appear to be as dependent on the pressure drop as those for the showerhead injector or the rigimesh injector at the 0.5 and 5 lbf thrust levels. The response times for all three hole patterns are similar at the low pressure drops with the 19 element injector being superior as the pressure drop is increased.

The scatter diagram in Figure 44 indicates no change in ignition delay with pressure drop. An increase in ignition delay does occur, however, as the number of injector elements is increased. Average values are 19.2, 24.3, and 27.2 milliseconds with injector elements of 7, 13, and 19 respectively.

IN JECTOR VARIABLE

COLD BED RESPONSE TIME (ms)

IGNITION DELAY (ms)



CHAMBER PRESSURE DECAY TIME (ms)

IN JECTOR VARIABLE

INJECTOR VARIABLE

50 Ibf ENGINE RIGIMESH INJECTOR SCATTER DIAGRAM CHAMBER PRESSURE ROUGHNESS

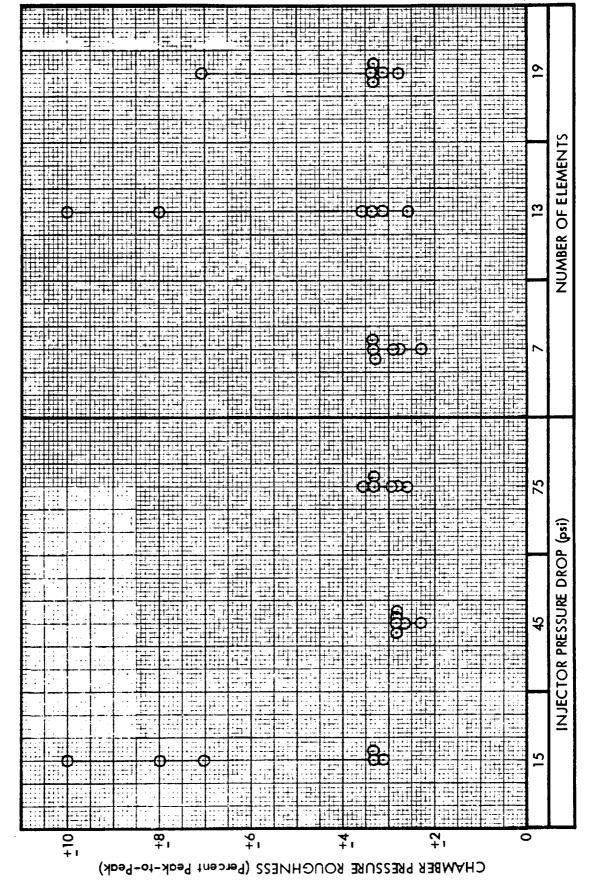
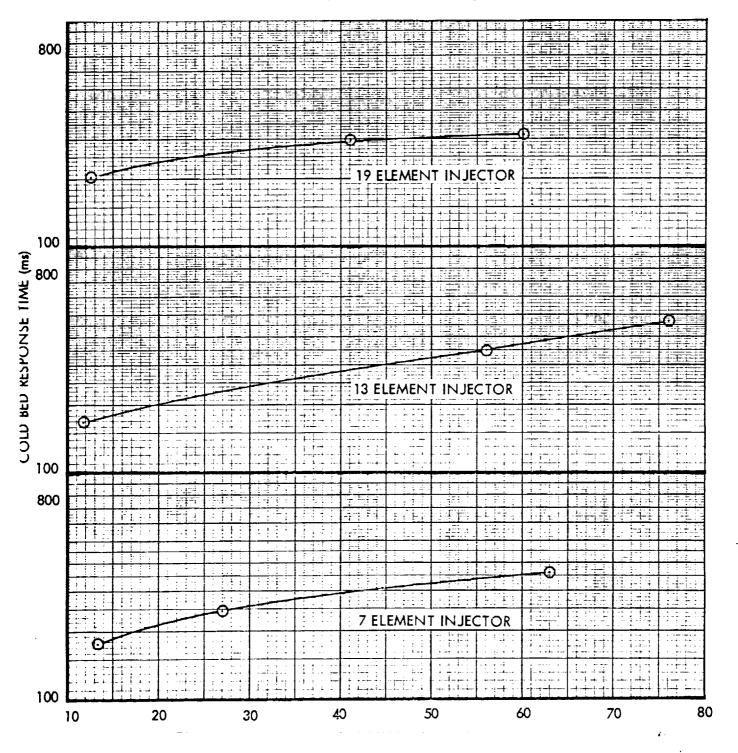


FIGURE 46

50 1bf ENGINE RIGIMESH INJECTOR AVERAGE COLD BED RESPONSE TIME VS INJECTOR PRESSURE DROP



INJECTOR PRESSURE DROP (psid)

50 LBF ENGINE - TEST DATA SUMMARY - RIGIMESH INJECTOR

Chamber Thrust Pressure Coefficient Roughness %Peak-to-peak (2)	+ 3.32	+ 3.35	+ 2.30	+ 2.84	+ 2.95	+ 3.30	+ 8.00	+ 9.94	+3.17	+ 3.37	+ 2.64	+ 3.58	+3.13	+7.04	+ 3,38	+ 3.33	+ 2.83	1 3.32	+7.34	+ 6.29
Thrust Coefficient 9	1.200	1.202	1,202	1.197	1.205	1.200	1.215	1.205	1,203	.19	1.209	 81.1	1.194	1.187	1.183	1.209	1.213	1.213	1.210	1.217
Specific Impulse (Z)	157.75	157.53	157.25	156.73	157.95	157.61	158.79	158.02	157.09	155.92	156.89	157.07	155.69	155.84	156.63	157.64	158.79	158.50	157.16	160.51
Characteristic Velocity fl/sec	4228	4217	4213	4213	4215	4227	4205	4219	4201	4183	4176	4246	4196	4224	7237	4195	4216	4205	4178	4242
Flow Rate Ibm/sec	0.2201	0.2192	0.2234	0.2197	0.2203	0.2218	0.2209	0.2213	0.2209	0.2197	0.2242	0.2036	0.2118	0,2079	0.2168	9127.0	0.2333	0.2325	0.2232	0.2318
Throst Ibf	34.726	34,532	35.124	34.433	34.832	34.950	35.074	34.975	34.706	34.250	35.172	31.980	32.970	32.400	33.960	34.925	37.050	36.850	35.074	37.206
Injection Preserve psia	200.4	201.6	1.122	219.0	248.4	2,53,2	204.0	204.6	247.2	251.7	291.6	172.4	203.1	204.6	228.9	233.7	264.6	264.3	202.5	294.6
Downstre 3.11 Chaint or Pressure paio	150.4	149.4	152.1	149.6	150.1	151.5	1.021	150.9	150.0	148.5	151.3	139.7	143.6	141.9	148.0	150.2	158.8	158.0	149.9	158.9
Upstream Chamber Pressure paid	176.2	173.3	177.8	174.7	174.8	176.4	176.7	178.7	177.8	:	177.6	163.2	176.2	179.5	173.4	178.0	190.5	189.7	176.7	183.7
Decay Time	8	8	5	18	7	8	8	28	8	8	88	44	3	107	33	78	8	8	3	8
Response Time ms.	35	\$	255	230	385	330	<u>.</u>	3	ឌ	356	4	35	3	240	240	294	242	315	<u>8</u>	\$
lynition Celay ms.	23	70	1	_	8	8 2	77	23	22	75	22	28	8	56	&	52	28	22	35	1
Initial Cotalyst Bed Temperature	79	3	۲	29	ዩ		3	ŝ	89	×	8	3	59	8	59	8	S	67	3	œ
Fuel Tempurature °F	S	84	\$	SZ.	\$	S	ጜ	41	7	\$	7	6	S	5	3	₫	4	47	\$	47
Code Te	15-0-7	15-0-7	₹ 2-0-7	45-0-7	75-0-7	75-0-7	15-0-13	15-0-13	45-0-13	45-0-13	75-0-13	75-0-13	15-0-19	15-19	45-0-19	45-0-19	75-0-19	75-0-19	1525-13	7525-13
781 No.	127-31-221	171-31-227	171-31-223	171-31-224	171-31-225	171-31-226	171-31-230	12-15-121	171-31-234	171-31-235	171-31-233	171-31-232	171-31-242	171-31-243	171-31-238	171-31-239	171-31-240	171-31-241	171-31-236	171-31-237

(1) First number refers to nominal injector pressure drap. Second number refers to distance of injector from catalyst bed. Third number refers to the number of elements.
(Z) Nozzle Expansion Ratio is 4.03:1

Chamber pressure decay time does not appear affected by either the number of orifices or the injector pressure drop.

At all conditions the engine does not run as smoothly with the rigimesh injector as with the showerhead injector. This appears to be the major difference between the injectors.

When the injector was moved 0.25 inches from the catalyst bed erratic start transients were obtained and the chamber pressure oscillations were higher than with the injector flush with the catalyst bed.

Characteristic velocity averaged 4,211 feet per second for the tests reported in Table X. Specific impulse averaged 157.5 lbf-sec/lbm and the thrust coefficient averaged 1.203.

6.3 Summary of Injector Optimization Testing

The injector testing reveals certain consistencies in the data obtained at all three thrust levels. These trends and recommendations for injector design criteria are described in the ensuing paragraphs.

It was found that cold bed response time increased as the injector pressure drop was increased at all three thrust levels. This result appears to be caused by the higher surge flow rates which exist at engine start for the low pressure drop injectors. Since chamber pressure was held constant for all of the tests, as the injector pressure drop is lowered, the flow resistance decreases resulting in higher transient flow rates. It appears that in all cases the catalyst is capable of decomposing the propellant faster than it is being supplied. The data obtained suggests that faster response times can be obtained by increasing bed loading. It is noteworthy that the trend in cold bed response was obtained at each thrust level although the nominal design bed loading increased with thrust level. The effects of bed loading on response time will be more fully investigated during later phases of the program.

The data obtained with the 5 and 50 lbf engines with the showerhead injector suggests that an optimum number of orifices exists which minimizes cold bed response time. It is noted that minimum response times were obtained with the 5 and 50 lbf engines with 6 and 40 orifice injectors respectively. These numbers of orifices correspond to 5.3 and 5.6 orifices per square inch of catalyst bed cross sectional area

respectively. It would thus appear that the true minimum occurs with approximately 6 orifices per square inch of catalyst bed area.

It was found that with the injector flush with the catalyst bed, smooth start-transient and steady state operation could be obtained with low pressure drop injectors. These results indicate that atomization of the propellant is not a necessary design criteria as was the case for the nonspontaneous catalyst (Reference 3).

At the 5 and 50 lbf thrust levels it was found that large chamber pressure oscillations existed when large size catalyst pellets were used throughout the catalyst bed. These oscillations could be virtually eliminated through the use of a layer of finer mesh catalyst at the top of the catalyst bed. The size and depth of catalyst required appears to be related to the bed loading and is not yet fully defined. These effects will be studied in more detail in later phases of the program. A penalty is incurred, however, through the use of the fine mesh catalyst and the resultant increase in catalyst bed pressure drop; however, at no time in the testing did the pressure drop become large enough to cause damage to the catalyst. It is noteworthy that during testing on the 50 lbf engine, pressure drops across the catalyst bed as high as 35 psid were realized with no evidence of catalyst breakup or damage. It thus appears that the spontaneous catalyst has a strength which is significantly higher than the nonspontaneous catalyst, designated by JPL as H-A-3, which was limited to pressure drops of 20 psid.

It was found that smooth operation could be obtained with the injector away from the catalyst bed. There appears to be no advantage, however, to having the injector away from the catalyst bed. Ignition delay and chamber pressure response times were higher and the engines tended to run rougher at the 0.5 and 5 lbf thrust levels when the injector was away from the catalyst bed. At the 50 lbf thrust level very similar results were obtained with the injector located either flush or 0.25 inches from the catalyst bed.

The rigimesh injector is a workable injector concept and gives results similar to the showerhead injector with the following exceptions:

- a. Chamber pressure oscillations are higher
- b. Chamber pressure decay times are higher

c. The rigimesh injector gives poor operation when it is not flush with the catalyst bed. This is probably caused by nonaxial flow from the injector and the impingement of this flow on the chamber walls.

One of the main advantages of the rigimesh injector is that it offers better resistance to being plugged by catalyst fines which might be generated from a vibration environment than does the showerhead injector (Reference 4). This is especially true if small orifices must be employed in the showerhead injector design. One of the disadvantages of the rigimesh injector is the inability to reproducibly size the injector for a given pressure drop. Prior to detail design of the rigimesh injector, flow tests were conducted with a number of sizes of rigimesh to obtain flow rate per unit cross sectional area. It was found that this data was not consistent with that obtained when the injectors were manufactured. There are probably two problems which lend to this lack of consistency. Rigimesh is made of sintered woven wire sheet. Various pore openings are obtained by utilizing either various numbers of layers of the sheet, of using different wire diameters, or by pressing the layers to varying thicknesses. Variation in wire diameter for the same thickness of rigimesh can produce marked changes in the flow rate per unit cross sectional area. Up to 50% variations have been quoted by the vendor. The rigimesh was machined by clamping the material between two flat plates. Application of excessive pressure from the clamping can result in decreasing the thickness of the rigimesh and thus reductions in the pore size. If this material is to be used it must be ordered to produce a given flow rate per unit cross sectional area and then pressed until the desired value is obtained.

It is felt that the showerhead injector represents a superior injector concept over the rigimesh injector for most applications. In most cases orifice diameters can be kept relatively large through the use of low pressure drop injectors. Additionally, reactor operation is not critically dependent on the number of orifices so that the number of orifices can be reduced over the indicated optimum without significant degradation in reactor operation. Orifice sizes as small as 0.010 inches have been used on the program with no problems of orifice plugging during engine tests. It should be noted, however, no vibration tests were conducted to determine whether or not orifice plugging would occur from catalyst fines generated by launch vehicle type vibration levels.

The following design criteria is recommended for the showerhead injector:

- a. Use approximately six orifices per square inch of catalyst bed cross sectional area. If required, this can be reduced by a factor of at least two without serious degradation in engine operation.
- b. Utilize low pressure drop injectors. The pressure drop can be held to 10 to 15% of the steady state chamber pressure.
- c. Mount the injector flush with the top of the catalyst bed.
- d. Propellant can be fed into the injector manifold through a single supply tube. Propellant velocities in the supply tube as high as 50 to 75% of the injector stream velocities were utilized in the study with no adverse effect on propellant distribution and/or reactor operation.
- e. Velocities in the propellant distribution manifold as high as 20 to 30% of the injector stream velocities were utilized in the study without having maldistribution of flow to the injector orifices.
- f. No evidence was found to indicate high L/D orifices and turbulent stream characteristics are necessary design criteria. It appears that orifice lengths are dictated by the required injector plate thickness needed to meet structural requirements.

·		
,		

7.0 CATALYST BED DESIGN PARAMETER STUDIES

Parametric tests were conducted to determine the effects of chamber pressure bed loading, catalyst particle size and bed length on reactor operation. Data to be obtained during these tests included:

- a. Ignition Delay Time
- b. Cold Bed Response Time
- c. Ammonia Dissociation
- d. Catalyst Bed Pressure Drop
- e. Characteristic Velocity and Sea Level Specific Impulse
- f. Chamber Pressure Roughness.

Identical tests were conducted at nominal thrust levels of 0.5, 5, and 50 lbf. The test data accumulated served as a basis for development of design and scaling criteria defining reactor performance and operation.

7.1 Test Conditions Studied

The range of study was to cover chamber pressure from 50 to 1,000 psia, bed loading over at least a 3:1 range, and catalyst bed lengths over at least a 3:1 range. The test matrixes in Figures 48, 49, and 50 list the conditions tested with the 0.5, 5, and 50 lbf engines. Chamber pressure was varied from 50 to 1,000 psia with intermediate values of 105, 225, and 475 psia. Bed loading was varied in increments of 0.01, 0.021, and 0.045 lbm/in²-sec. Catalyst bed lengths for the 5 lbf engine were 0.5, 1.0, 1.5, and 2.0 inches; for the 50 lbf engine were 1.0, 2.0, and 3.0 inches; and for the 0.5 lbf engine were 0.5, 1.25, and 2.0 inches.

Tests were conducted at each point in the matrixes shown except where the estimated catalyst bed pressure drop exceeded 70 psid or where previous tests at a longer bed length had resulted in unsatisfactory operation. Instrumentation utilized for the tests is tabulated in Table XI.

7.2 Test Results

7.2.1 5 lbf Engine

Prior to initiating the bed loading chamber pressure, and bed length tests, a series of tests was conducted to determine the required fine mesh

0.5 Ibf ENGINE TEST MATRIX FOR BED LOADING, CHAMBER PRESSURE, AND BED LENGTH STUDIES

	1000	A3-12	A3-26	A3-37
	472.6	A3-10 A3-11	A3-25	A3-36
0.0447	223.5 472.6 1000	A3-10	A3-24 A3-25	
	50 105.7		A3-23	
	50		-	
	0001	A3-9	A3-22	A3-35
	472.6 1000	A3-8	A3-21 A3-22	A3-34
0.02115	105.7 223.5	A3-7	A3-20	A3-32
	105.7	A3-6 A3-7	A3-17 A3-18 A3-19 A3-20	A3-32
	50		A3-18	
	1000	A3-5	A3-17	A3-31
	472.6	A3-4	A3-16	A3-30
0.01	223.5	A3-3	A3-15	43-29
	105.7	A3-2	A3-14	A3-28
	50	0.5 A3-1	25 A3-13	2.0 A3-27
ding -sec	. s e	0.5	1.25	2.0
Bed Loading Ibm/in2-sec	Chamber Pressure (psia)	(ni) dt	gned Leng	Λισιο

5 Ibr ENGINE TEST MATRIX FOR BED LOADING, CHAMBER PRESSURE, AND BED LENGTH STUDIES

-																
	Bed Logding (Ibm/in²-sec)			0.01					0.02115					0.3447		
	Chamber Pressure (psia)	50	105.7	223.5	977.79	1000	S	7:501	223.5	472.6	1000	20	105.7	223.5	472.6	1000
	0.5	1-63	83-2	13 -3	5 2 4				83-5	\$ 23	B3-7				8 2	83-9
H (INCHES)	1.0	01-03	83-11	83-12	13-13	E3-14	83-15	83-16	17-63	63-18	B3-19			02-03	10-21	83-22
PED FENCE	1.5	13-13	B3-24	83-25	63 -26	83- 77	82-28	B3-29	B3-30	16-53	83-32			13-33	34.03	82-33
	2.0	9E-E¶	15-50 15-37	£3-38	62-29	83-40	2	B3-42	5 1 - 52	4 8	83-45			13-46	13-47	83-48

50 Ibf ENGINE TEST MATRIX FOR BED LOADING, CHAMBER PRESSURE, AND BED LENGTH STUDIES

	0001	C3-9 C3-10	C3-23 C3-24	G-37 G-38
2790.	224 473	S 8 8	C3-22 C3	<u>ខ</u> % ទ
	- 8		C3-21	S-63
	95			
	0001	G-7	G-28	<u>8</u>
	473	9-E	g-18	G-33
.02115	224	2-5	C3-18	C3-32
	8		C3-17	G3-31
	20		C3-15* C3-16	- C3-30
	1000	3-4		ca-29•
	473		C3-14•	C3-28*
ю.	224	3-7	C3-13	α - :0
	105	- 5	G-11 G-12	g-%
	. 98 ·		6	C3-25
Bed Loading (lb/in²-sec)	Chamber Pressure (psia)	1.0	2.0	3.0
		HE2)	иі) нтәизі	G38

"These tests were not conducted because of damage to test hardware.

TABLE XI

INSTRUMENTATION LIST FOR REACTOR DESIGN PARAMETER STUDIES

Digital × × × × TYPE RECORDER Oscillograph × × × × × × Strip Chart × × × × × SYMBOL .3..3 Downstream Chamber Pressure Upstream Chamber Pressure Gas Sample Bottle Pressure Injector Head Temperature Injector Head Temperature Catalyst Bed Temperature Catalyst Bed Temperature **PARAMETER** Gas Outlet Temperature Propellant Flowrate Propellant Flowrate Injection Pressure Fuel Temperature Valve Position Thrust

cata.yst on the top of the catalyst bed. Earlier tests (See Paragraph 6.2.3) had indicated this was required to assure smooth steady state operation. These tests were conducted with the 1.5 inch chamber at a bed loading of 0.045 lb/in²-sec and a chamber pressure of 225 psia. The results of this testing are summarized in Table XII. The catalyst bed configuration arrived at was 0.3 inches of 25-30 mesh catalyst on the top of the bed, with the remainder of the bed 14-16 mesh granular catalyst.

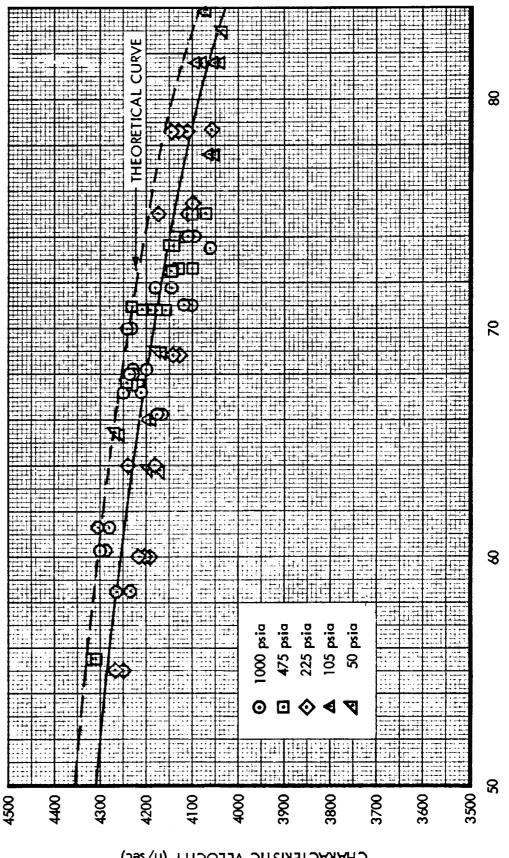
Data obtained from testing on the 5 lbf engine is summarized in Table XIII. The characteristic velocity data has been corrected for chamber radiation heat losses and propellant temperature effects and is plotted against fractional ammonia dissociation in Figure 51. Radiation heat loss corrections were made assuming radiation to free space with a chamber emissivity of 0.9. All test data was normalized to a propellant temperature of 70°F (Reference 5). When these corrections are made to the data, the mean curve falls within approximately 98.5% of the theoretical curve.

Sea level thrust coefficient data for expansion ratios of 1.0 and 2.2 is plotted versus chamber pressure in Figure 52. The theoretical curve has been corrected for divergence losses assuming a 15° conical nozzle. From the curve it is noted that the data at an expansion ratio of 1.0 falls on the theoretical curve while the data at an expansion ratio of 2.2 averages approximately 99% of the theoretical value.

7.2.2 50 lbf Engine

Prior to initiation of the bed loading, chamber pressure, and bed length studies, tests were conducted with 20-25 and 25-30 mesh granules on the top of the catalyst bed to determine the required fine mesh catalyst size for smooth decomposition. Previous testing (see Paragraph 6.2.5) had shown that larger size granules resulted in unsatisfactory operation. These tests were conducted with the 3.0 inch length chamber at a bed loading of 0.045 lb/in²-sec and a chamber pressure of 225 psia. Chamber pressure oscillations of ± 3 to 9% occurred during testing with 20-25 mesh granules on the top of the catalyst bed. Testing with 25-30 mesh granules resulted in maximum chamber pressure oscillations of ± 2%. A catalyst bed configuration was finalized which consisted of

AMMONIA DISSOCIATION FOR 5 16F ENGINE CORRECTED CHARACTERISTIC VELOCITY



CHARACTERISTIC VELOCITY (ft/sec)

AMMONIA DISSOCIATION (Mole Percent)

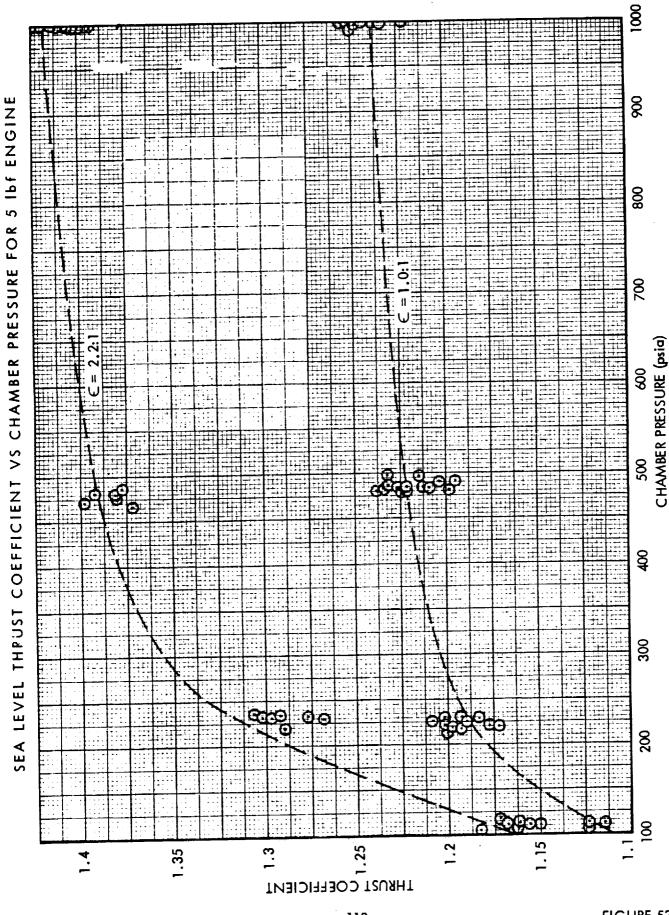


TABLE VII

SUMMARY OF 5 ISFENGINE CATALYST PARTICLE SIZE STUDIES

TEST RESULTS	Bed Chamber pressure oscillations of ± 36 psia occurred throughout test of 5 seconds duration. Frequency of oscillations was 8.3 cps. Ignition delay was 20 ms.	Test was very smooth (± 1.5% chamber pressure oscillations) up to 9 seconds. Random oscillations of ± 16% chamber pressure variation for remainder of 30 second test. Ignition delay was 4 ms. Chamber pressure decay time was 340 ms.	Test was smooth in operation up to 20.6 seconds and then very rough for remainder of test of 30 seconds duration. Chamber pressure decay time was 460 ms.	Test was smooth in operation up to 22 seconds and then very rough for remainder of test of 30 ms.	Test was smooth in operation up to 17.8 seconds. Random oscillations which tend to damp out 8 and return occur throughout remainder of 30 second test. Chamber pressure decay time was 425 ms.	Smooth operation up to 11 seconds. Pressure spikes and random roughness occur periodically up to Z , 6 seconds at which time engine starts to run smooth again. Chamber pressure decay time was 105 ms.	Smooth operation to 12 seconds at which time chamber pressure spikes and random oscillations occur until end of test. Chamber pressure decay time was 217 ms.	Test was smooth except for 5 pressure spikes of approximately 50 prid overshoot which occur between 13 and 25 seconds into 30 second test. Chamber pressure decay time was 90 ms.	Test was smooth except for two small pressure spikes at 25 and $oldsymbol{\mathcal{D}}$ seconds. Chamber pressure
CATALYST BED CONFIGURATION	Entire bed composed of $1/8 \times 1/16$ " pellets. Bed length 1.5 inches.	0.3 inches of 16-20 mest catalyst on top of catalyst bed. Remaining 1.2 inches of bed 1/8 x 1/16" pellers.	0.3 inches of 20-25 mesh catalyst on top of catalyst bad. Remaining 1.2 inches of bed 1/8 × 1/16" pellets.	0,3 inches of 20-25 mesh catalyst on top of catalyst bad. Remaining 1,2 inches of bed 1/8 × 1/16" pellets.	0.5 inches of 20-25 mest catalyst on top of catalyst bad. Remaining 1.2 inches of bed 1/8 x 1/16" pellers.	0.5 inches of 25-30 mest catalyst on top of catalyst bad. Remaining 1.2 inches of bed 1/8 x 1/16" pellets.	0.3 inches of 20-30 mest catalyst on top of catalyst bed. Remaining 1.2 inches of bed 1/8 x 1/16" pellets.	0.3 inches of 25-30 mesh catalyst on top of catalyst bed. Remaining 1.2 inches of bed 14-16 mesh catalyst.	Same as 251.
TEST NO.	244	245	246	247	248	249	250	251	252

	(5) Thrust Coefficient	308	1.4	1.243	1.243	1.408	1.20	1.396	1.424	1.233	1.222	1.407	1.20	[3-	1.250	1.250	1.25	1.25	1.40	.393	2	1.24	1.250	1.397	1.22	1.23	1.22	1.37	1.28	1.393	1,215	1.233
	(6) Ammonia Dissociation mole %	İ	71.k	}	58.5	11	60.3	1	71.0	-	68.3	1	6.19	73.7	-	66.2	!	0.89	-	74.0	:	9.89	!	70.0	ļ	70.8	-	62.8	-	55.3	ļ	74.0
	(6) Catalyst Bed Ammonia Pressure Drop Dissociation ok psid mole %	c		0	0	60 ,	۰.	7	•	•	-	ĸ	7	2	4	2	23	12	m	7	2	9	18	8	0	0	36.2	3.2	51		0	0
	Chamber Pressure Roughness P % peak to peak	4	+ 0.5	+ 3.6	8. - f	+ 5.9	+ 4 .8	+0.6	+0,3	+ 1.8	± 0.8	± 3.2	+3.2	÷ 0.6	8.0.+ -	÷0.5	<u>-</u> .	± 1.2	÷ 0.5	¥ 0.8	+ 0.9	9.0 ±	+0.9	+ 2.4	+1.7	+1.5	+ 10.5	+ 5.4	÷ 6.0	+3.1	+ 0.6	<u>-</u>
GTH TESTS	(5) Specific Impulse Ibf-sec/Ibm	124.1	178.0	162.8	162.8	186.2	164.4	172.2	175.0	159.8	157.7	186.2	165.0	169.2	159,5	159.8	163.4	162.7	171.2	170.0	159.5	159.8	163.3	182.1	156.2	157.5	150.7	175.8	163.1	184.7	153,9	156.0
IABLE XIII 205 DIAMETER REACTOR BED LOADING, CHAMBER PRESSURE, AND BED LENGTH TESTS	Characteristic Velocity ft/sec	707	4050	4222	4207	4264	4246	3964	3956	4173	4160	4259	4252	3892	4114	4119	4197	4188	3926	3935	414	4149	4204	4198	4084	4142	3978	4105	4280	4273	4076	4070
PRESSURE,	(4) Decay Time	122	82	113	135	æ	92	528	237	102	8	ጵ	8	258	8	136	62	8	302	333	165	2	æ	117	3	6/1	27.5	112	7.5	8	175	175
KIR VG, CHAMBEI	Response Time	7	. ₹	43	8	\$	87	267	8	901	108	8	79	200	133	. 120	8	76	253	325	168	<u>3</u>	103	7	193	216	145	128	0,	79	292	297
BED LOADING	(2) Ignition Delay	\$: =	=	۰	=	12	82	12	2	13	=	۰	12	2	2	Ξ	=	2	11	=	=	2	۰	2	13	2	٥	۰	13	13	22
TER REACTOR	Exit Gas Temperature	1430	1464	1525	1529		<u> </u>	1398	1420	1472	1472	1542	1543	1269	1398	1415	1468	1481	1329	1329	1428	1424	1485	1472	1437	1437	1536	1513	1614	1587	1338	1329
1.205 DIAME	(1) Flow Rate Ibm/sec	0.01158	0.01161	0.02280	0.02304	0.04870	0.04883	0.01167	0.01183	0.02346	0.02356	0.04856	0.04819	0.01206	0.02385	0.02351	0.04730	0.04784	0.01192	0.01183	0.02348	0.02360	0.04814	0.04880	0,01140	0.01111	0.02488	0.02414	0.05064	0.04993	0.01179	0.01174
SUMMARY OF 1.	Throst 16 f	6	2.067	3.712	3.752	<i>4</i> .07	8.03	2.01	2.07	3.748	3.716	9.040	7.950	2.000	3,7%	3,756	7.728	7.784	2,040	2.010	3,744	3.772	7.860	8.900	1,780	1,760	3.750	4.245	8.260	9.220	1,815	1.831
S	Downstream Chamber Pressure psia	1101	1016	\$	5001	1015	1009	900	101	101	1012	101	266	1014	1013	1000	996	975	101	900	9001	6001	986	1003	485	476	482	48	181	475	496	464
	Initial Catalyst Temperature	Ş	3 25	\$	15	\$	4	92	9	1	54	47	62	51	\$	\$	56	64	52	51	4	4	62	53	52	47	84	54	6	45	46	1
	Page di		9 0	0.5	0.5	0.5	0.5	1.0	1.0	0.1	0.	0.1	0.1	1.5	1.5	1.5	1,5	1.5	2.0	2.0	2.0	2.0	2.0	2.0	6.0	0.5	0.5	0.2	0.5	0.5	0,1	1.0
	Z Z Z	9	345	2,4	781	906	306	314	316	273	8/7	300	302	325	992	3 98	287	285	319	321	283	284	567	5 88	332	334	27.7	342	31	313	307	308

	_	- 1		•																	٠.									-				
	(5) Thust Coefficient		1.195	1.203	1 .381	1.381	1.22.1	1.222	1.214	1.210	1.233	-	1.398	1.241	1.223	1, 198	1.233	1,238	1.372	1.234	1.183	1.305	1.292	<u>1</u> .183	1.183	8	1,203	1,305	1.297	1,193	1.198	1.177	1.173	1.201
	(6) Ammonia Dissociation	mole %	ļ	67.6	-	4.79	1	75.0	i	62.4	72.6	•	-	70.8	-	71.8	į	73.5		70.0		64.0	1	75.0	į	59.8	ļ	1	55.0		73.0	į	6.89	1
	عد ن	Bid	5.0	7.0	23.6	21,8	9.1	0.1	6.6	7.2	6.4	46.6	22.0	23.6	3,6	3.0	6.0	7.0	43.4	39.6	0.1	0.	3.8	3.8	36.4	10.2	0.11	31,0	28.8	5.2	5.2	16.1	0.71	47.4
	Chamber Pressure Roughness	bf-sec/lbm % peak to peak	± 2.5	+ 1.2	+ 3.8	+ 2.5	¥.0.4	+ 1.2	+ 2.3	± 2.1	+ 2.2	e, 6, 8	± 2.3	+ 6.3	+0.6	+ 1.3	+1.7	± 2.3	± 2.1	8,1 ÷	+ 2.8	± 2.0	± 1.7	± 1.7	+ 1.3	± 2.3	+ 1.8	+ 4.5	+ 10.5	+ 2.9	± 1.7	± 2.4	± 2.2	± 2.2
	(5) Specific Impulse	lbf-sec/lbm 9	156.3	156.7	182.0	182.7	151.3	151.8	152.4	153.5	156.1	1	179.5	162.5	150.1	149.2	156.7	157.2	178.2	162.3	153.0	97.791	162.0	149.5	152.0	152.6	154.4	171.6	6.691	143.3	145.0	147.7	147.7	157.1
	Characteristic Velocity	ft/sec	4212	4199	4240	4257	3992	4005	4042	4090	4075	4132	4180	4218	3953	4004	4064	4085	4185	4235	4130	4125	4038	4039	4129	4132	4139	4230	4216	3868	3897	4047	4056	4211
	(4) Decay Time	as.	110	9 0	8	8	200	215	ł	22	112	<u>8</u>	82	2	217	233	131	213	18	11	110	121	8	<u>6</u>	88	82	8	ន	22	136	122	8	18	9
TABLE XIII (Cont'd)	(3) Response Time	as.	143	191	163	185	303	375	052	260	179	370	246	262	329	266	197	398	338	440	\$	476	787	888	318	548	622	257	275	1469	319	173	319	757
TABLE XI	(2) Ignition Delay	ä.	۰	ļ	٥	12	±	6	2	12	15	٥	2	∞	92	∞	2	=	<u>:</u>	º	s,	8 0	13	±	4	5	7	2	۰	<u>8</u>	<u>&</u>	•	S	•
	Exit Gas Temperature	<u>.</u>	1424	1442	1494	1492	1278	1261	1372	1372	1385	1424	1494	1450	1286	1295	1407	1394	1442	141	1398	1415	1308	1312	1451	1407	1442	1512	1503	1244	1252	1351	1351	1424
	(1) Flow Rate	lbm/sec	0.02388	0.02387	0.05050	0.05046	0.01170	0,01160	0.02453	0.02341	0.02454	0.04774	0.05048	0,04905	0.01166	0.01147	0.02482	0.02421	0.05005	0.04899	0.01164	0,01140	0,01181	0.01148	0.02369	0.02384	0.02415	0.05166	0.05162	0.01152	0.01159	0.02388	0.02389	0.04640
	Thrust	٩	3.732	3.740	9.190	9.220	1,770	1.750	3.739	3,731	3.830	İ	9.060	7.970	1,750	1.710	3.890	3.805	8.920	7.950	1.780	1.910	1.914	1,716	3.600	3.636	3.729	9.860	8.770	059.	089	3.528	3.528	7.290
	Downstream Chamber Pressure	Di Si	489	88	478	476	181	479	482	484	8 84	439	469	4 73	<i>(1)</i>	476	464	- 88	3	474	232.7	234.1	233.1	225.5	226.5	224.9	228.3	232.2	231.5	216.7	219.7	220.7	221.3	215.7
	Initial Catalyst Temperature	9	\$	15	46	55	45	13	46	. 95	7	£	છ	62	51	55	28	\$	\$	28	56	53	‡	4	59	56	46	57	\$	3 5	\$	3	15	જ
	Bed Length	<u>.د</u>	0.1	0.1	1.0	1.0	1.5	1.5	1.5	1.5	1,5	1.5	1,5	1.5	2.0	2.0	2.0	2.0	2.0	2.0	0.5	0.5	0.	o. -	0.1	0,	0,	0.	0.	2,5	2,	7,1	5.1	5.
	Test No.		265	267	3 6	305	318	320	261	297	315	289	<u>~</u>	283	328	359	262	5 84	8	30	352	354	310	312	254	256	283	345	347	322	323	123	252	295

(5) Thrust Coefficient	1.27	1.268	1.290	1.209	1.205	1.188	1.194	1.163	1.160	1,161	1.183	1.118	1,116	1,170	1.123	1,123	1.15	1.150	1,156	1.022	1.005	0.968	0.953	1.76.0	0.912	0.912	0.940	0.961	200.0
(6) Ammonia Dissociation mole %	-	78.8	į	•	78.5		77.0	į	-	ļ	0.77	1	0.99	81.5	1	56.7	78.2	į	91.6	ŀ	63.7	;	0.69	83.0	į	65.3	ļ	1	85.2
(6) Catalyst Bed Ammania Pressure Drap Dissociation t psid mole %	8.4	8.9	28.4	28.0	53.4	57.8	73.8	1.8	5.7	2.9	3.3	6.91	17.2	5.6	22.3	21.4	24.6	10,5	9'.11	8.5	7.9	30.0	30.1	8,1	38.7	8.14	18.0	18.3	. 6'21
Chamber Pressure Roughness % peak to peak	8.1	6. - +1	± 2.3	+ 2.2	± 2.3	± 2.0	+ 2.2	4.4	±3.2	+ 2.4	+3.7	+ 4.6	+ 4.1	+3.6	+3.5	+ 4.7	+ 5.1	+ 3.6	+ 4.9	÷ 5.5	4.4.6	+ 5.0	+4.2	8.0+	+ 3.8	+ 14.0	+ 5.3	+ 4.3	+7.7
(5) Specific Impulse of-sec/lbm	156.2	157.1	162.4	153.5	152.4	154.2	156.8	147.8	14.1	14.7	141.6	144.5	144.1	146.2	140.9	140.2	138.7	141.8	142.9	127.7	125.6	127.2	126.5	120.2	120.4	119.2	118.6	121.6	1.18.1
Characteristic Velocity ft/sec II	3939	3988	4054	4090	4072	4185	4230	4095	4005	4013	3852	4163	4152	4024	4038	4022	3913	3971	3978	4028	4017	4236	4275	3990	4265	4207	4062	4074	4087
Decay Time	9	147	120	8	8	28	8	16	16	151	8	22	59	88	8	8	1	8	8	88	8	36	ಜ	59	83	9	62	128	135
(3) Response Time ms.	335	956	214	242	346	424	482	650	986	874	813	545	949	1450	1363	1586	985	3000	3000	1132	1224	816	158	1810	3180	200	2900	4200	3090
(2) (gnition Delay ms.	7	13	2	13	92	13	9	vn	13	15	•	S	2	13	80	9	٥	٥	7	-	S	က	5	4	9	6	0	0	5
Exit Gas Temperature ° F	1361	12/3	1359	1420	1359	1407	1407		1342	1321	1355	1394	1398	1261	1321	1321	1329	1261	1270	1364	1329	<u>=</u>	1377	1314	1312	1321	1235	1244	1252
(1) Flow Rate Ibm/sec	0.01178	0.01184	0.02446	0.02432	0.02406	0.04197	0.04637	0.01166	0.01213	0.01230	0.01215	0.02446	0.02393	0.01293	0.02407	0.02399	0.02422	0.01199	0.01190	0.01387	0.01266	0.02604	0.02529	0.01256	0.02504	0.02440	0.01164	0,01184	0.01169
Thrust	1.840	1.860	3.972	3,732	3.667	6.470	7.773	1,723	1.747	1,780	1.720	3.516	3.448	1.890	3,391	3,364	3.360	1,700	1,700	1.770	1.550	3,312	3,200	1,510	3,016	2,910	1,380	1.440	1.380
Downstream Chamber Pressure psia	226.7	129.1	217.9	227.1	223.7	193.9	216.5	108.4	109.5	111.3	105.5	11.8	109.7	117.3	107.3	106.5	97.70	107.4	106.7	59.4	54.1	54.8	53.7	53.4	51.5	.49.5	50.3	51,3	8.02
Initial Catalyst Temperature	6	55	55	28	28	65	83	49	67	ಜ	54	51	ዴ	55	67	58	15	95	દર	22	\$	t	55	19	64	26	53	8	\$
Bed Length in.	2.0	2.0	2.0	2.0	2.0	2.0	2.0	6.6	0.1	0.1	1.0	0.1	0.1	1,5	2,1	2,1	2.1	2.0	2.0	1.0	1.0	1.0	0.1	1.5	1.5	1.5	2.0	2.0	2.0
Test No.	330	331	286	288	290	324	326	356	336	337	341	269	270	366	253	255	317	351	353	343	344	280	282	365	257	259	355	357	359

Average of two flowmeters in series.
 Time from propellant entry into chamber to 1% of steady state chamber pressure.
 Time from propellant entry into chamber to 90% of steady state chamber pressure.
 Time from chamber pressure start decay to 10% of steady state chamber pressure.
 Sea level conditions at expansion ratio of 1.0:1 or 2.2:1.
 Average value obtained from ammonia to hydrogen and ammonia to nitragen male ratios.

0.2 inches of 25-30 mesh catalyst on the top of the bed with the remainder of the bed $1/8" \times 1/8"$ cylindrical pellets.

Data obtained from testing on the 50 lbf engine is summarized in Table XIV. Corrected characteristic velocity (see Paragraph 7.2.1) is plotted against ammonia dissociation in Figure 53. The mean curve falls within approximately 99% of the theoretical curve.

Sea level thrust coefficient data is plotted versus chamber pressure in Figure 54. The theoretical curve has been corrected for divergence losses assuming a 15° conical nozzle. The test data averages approximately 98.5% of the theoretical curve.

7.2.3 0.5 lbf Engine

Because of the small size of the 0.5 lbf engine, a layered bed technique was not utilized. Rather, the chamber was filled with a single size catalyst throughout. Testing was conducted with both 16-20 mesh and 20-25 mesh size catalyst in the engine. The 16-20 mesh catalyst resulted in excessive chamber pressure excursions while smooth operation was obtained with the 20-25 mesh catalyst. This size catalyst was subsequently used for all of the reactor design parameter studies.

Data obtained from testing on the 0.5 lbf engine is summarized in Table XV. Corrected characteristic velocity is plotted against measured ammonia dissociation in Figure 55. The mean curve falls within approximately 99% of the theoretical curve.

Sea level thrust coefficient data is plotted versus chamber pressure in Figure 56. The theoretical curve (for $\mathcal{F} = 1.28$) has been corrected for divergence losses assuming a 15° half angle conical nozzle. The test data averages approximately 99% of the theoretical value.

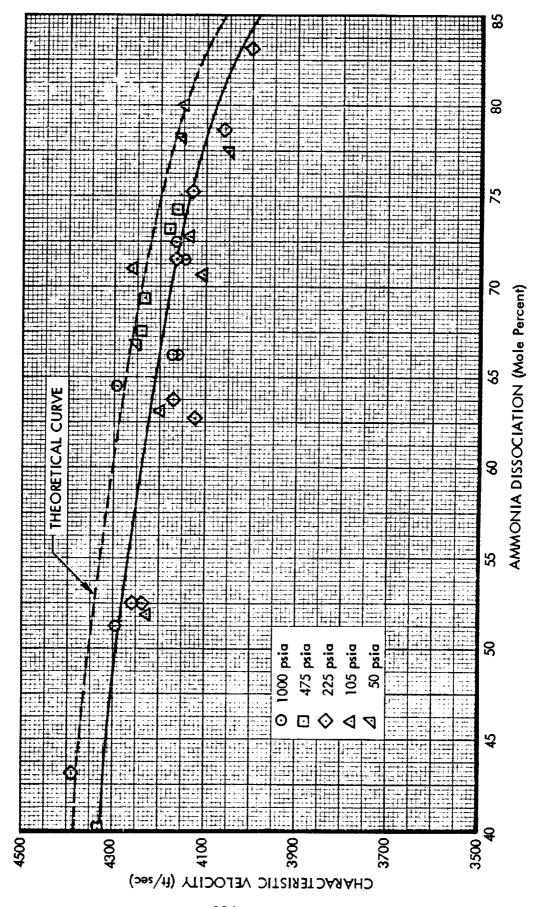
7.3 Summary of Test Data

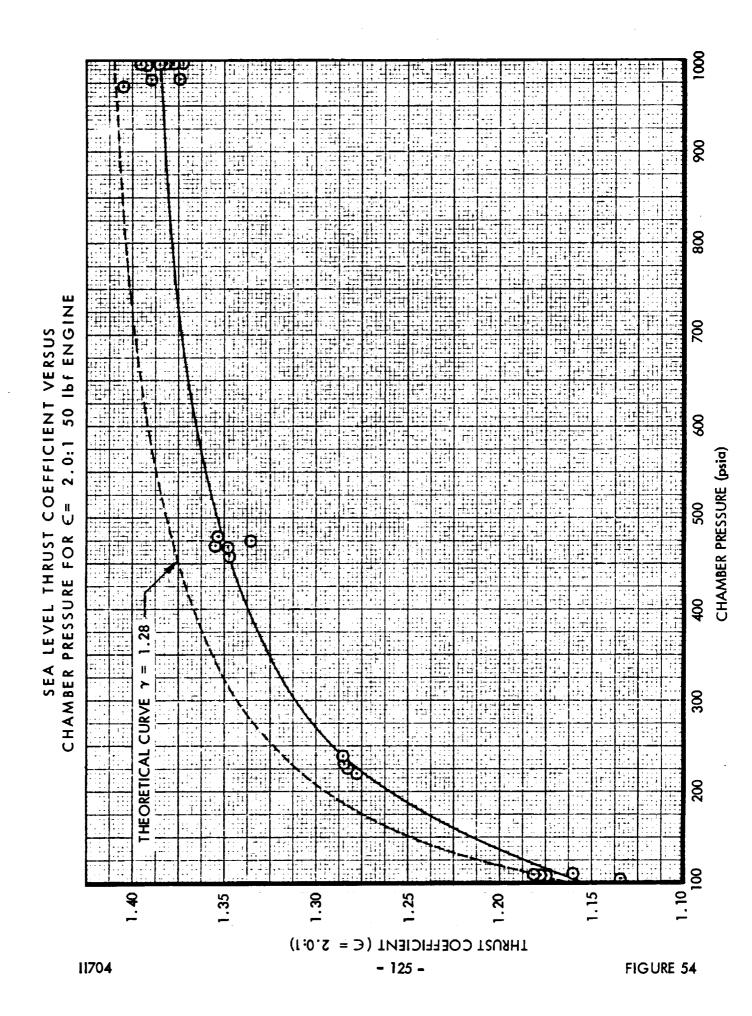
Detailed, analysis, correlation, and development of design and scaling criteria from the test data obtained is presented in Volume II of the final report. The following sections summarize the design and scaling criteria developed as a result of the test data obtained.

CORRECTED CHARACTERISTIC VELOCITY

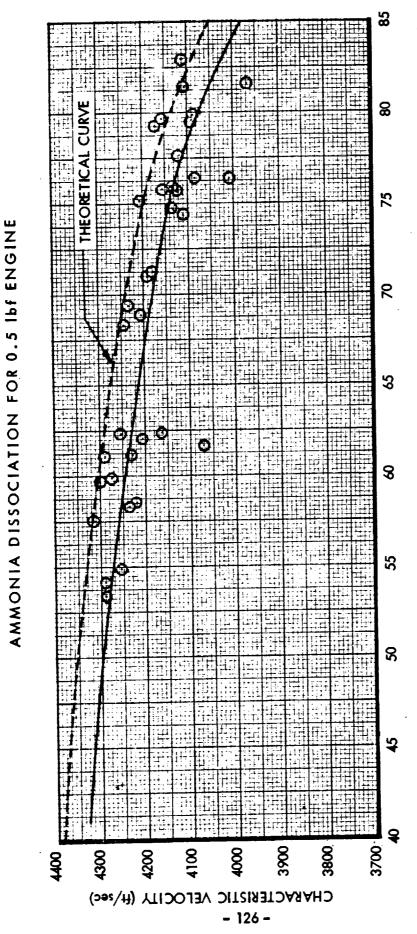
VS AMMONIA DISSOCIATION

FOR 50 1bf ENGINE





CORRECTED CHARACTERISTIC VELOCITY VS



AMMONIA DISSOCIATION (Mole Percent)

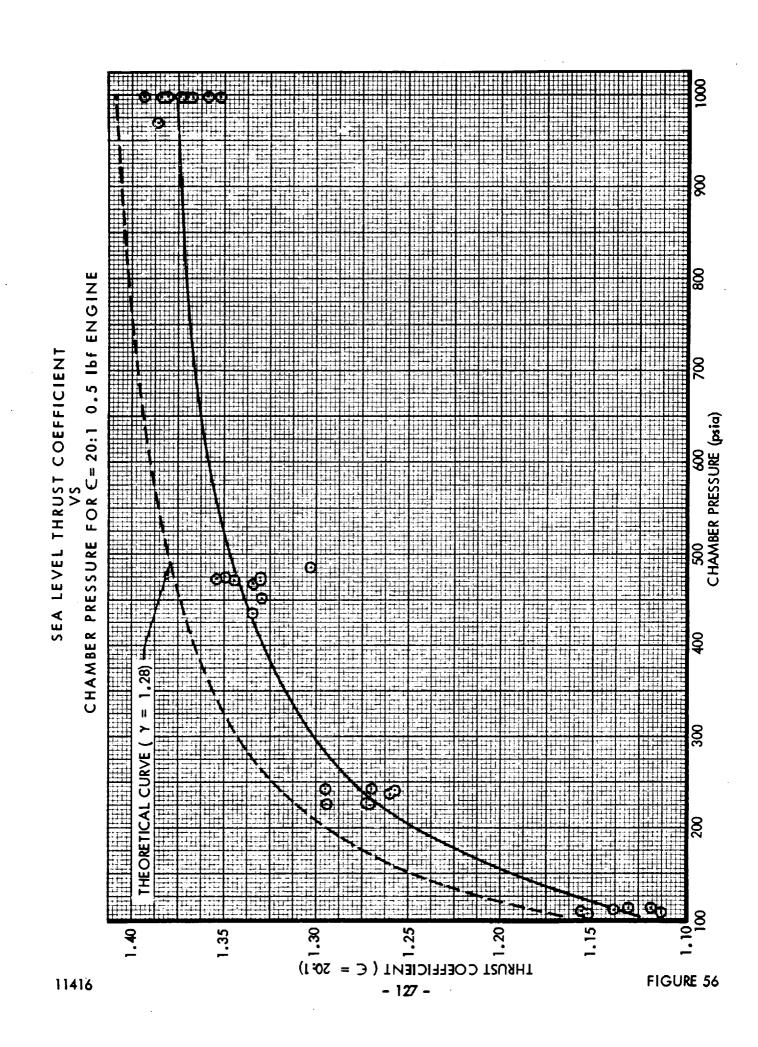


TABLE XIV

SUMMARY OF 3.010 DIAMETER REACTOR BED LOADING, CHAMBER PRESSURE, AND BED LENGTH TESTS

Complete Presente			loitio	Downstream		ε		8	ල	3	ī		Chamber	4		9
1,	No	Bed	Catalyst	Chamber	Thrust		Exit Gas Temperature	Ignition Delay	Response Time	Decay Time	Characteristic		Pressure Roughness	Calaiysi bed Pressure Drop	Ameronia Dissociation	Coefficient
1,0 6,9 1000 21,13 0,11702 1533 11 64 170 4140 179,4 21,53 10 664,4 1,0 5,1 1000 21,23 0,17001 1400 14 756 256 412 175,2 0,3 2 2 3 3 1,0 5,1 1000 21,23 0,12002 1713 9 9 9 412 175,2 0,3 2 2 3 3 1,0 5,4 969 5,5 0,3004 1565 1713 9 9 9 412 179,4 1,2 0 3 3 1,0 5,4 969 5,5 9,030 1,030 1,030 1,030 1,03 1,03 1,03 1,03 1,03 1,03 1,03 1,03 1,0 5,4 969 5,5 9 0,3004 1,03		P C	J.	psia	191	1bm/sec	u.	Ě	Ě	as.	ft/sec	lbf-sec/lbm	% peak to peak	psid	mole %	
2.0 6.6 1 1000 2120 1100 11010 11010 11010 11010 200 4101 11010 11010 200 4101 11010 11010 200 11010	8	6	0,4	0801	21.13	0.11762	1555	=	\$	170	4143	179.6	~	0	4.99	1.395
3.0 64 100 21,22 0,1700 145 11 176 296 4101 177.7 € 0.5 2 71,5 1,0 53,0 77 53,45 0,20734 183 6 172 64 411 11.7 € 0.6 7 64,35 1,0 54 78 54 78 412 17.2 € 0.6 7 64,35 1,0 54 58,45 0,2016 184 16 178 59 412 17.9 € 0.6 7 64,35 2,0 60 400 182 17 412 17.9 17.9 412 17.9 17.9 418 59 419 17.9 418 59 419 17.9 418	8 8		;	802	21.03	0.11918	1460	±	203	506	4121	176.5	+ 0.3	2	73.5	1.378
1, 0 5, 5 7, 7 5, 5, 5 0, 30, 51 7, 13 7 7 8 8 8 8 42, 64 181, 1 4, 12, 0 5 5 51, 3 1, 3	38	3.0	1 79	040	21.32	0.12000	1455	=	176	2%	4101	177.7	5.0 +	2	71.5	1.394
2,0 56 978 55.6 0.30734 160 16 162 44 421 181 4 0.9 7 64.5 2,0 6,4 6 16 16 16 16 17 64.5 7 64.5 1,0 6,4 6 6 16 16 17 417 17.9 4.0 7 64.5 1,0 6 6 6 6 6 16 18 9 417 17.9 1.0 7 64.5 1,0 6 6 6 6 6 6 6 11 417 17.4 4 2 7.0 1.0 7 64.5 7 4 7 1.0 6	387	0,	53	226	56.25	0.30512	1713	٥	88	93	4268	184.4	± 2.0	5	51.3	1.390
1, 0 54 586 58, 59 0, 0, 0, 0, 0, 0 14, 4 14, 4 14, 5 14, 4 14, 4 14, 5 14, 4 14, 4 14, 5 14, 5	395	2.0	38	826	55.65	0.30734	1605	9	102	3	4241	181.1	4·0.4	7	64.5	1.374
1, 0 6.3 500,7 6, 9, 9, 0, 0, 0, 0, 275 14.4 19 187 117 175,3 175,3 1, 6, 0 2, 0, 4 1, 0 2, 0, 4 1, 0 2, 0, 4 1, 0 2, 0, 4 1, 0 2, 0, 4 1, 0 2, 0 2, 0	376	3.0	3	896	55.90	0.31066	1565	9	128	26	4123	6.671	8.0 ±	8 2	66,3	1.404
2.0 6.7 646.5 6.20 0.10544 1472 19 229 111 4137 174.4 † 1.9 4.2 73.1 1.1 1.1 1.1 1.1 1.1 1.1 1.1 1.1 1.1	412	0.	53	500.7	9.93	0.07375	1424	61	187	5	4175	175.3	± 0.2	9.0	75.3	1.350
3.0 5.5 47.1 26.75 0.15446 1481 20 311 105 4119 17.3 4.1 1.9 4.8 7.0 1.0 5.5 47.28 5.5 0.30440 1656 17 182 86 4.01 173.4 4.1 1.9 4.8 7.0 2.0 6.0 457.5 5.3,0 0.30440 1684 18 7.2 4.2 1.9 4.8 7.0 3.0 6.0 457.5 54.10 0.30440 1684 18 7.2 4.7 17.5 4.4 1.9 4.8 1.9 7.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 1.0 4.0 4.0 1.0 4.0	38	2.0	29	468.5	26.30	0.15084	1472	61	229	Ξ	4137	174.4	6. 1.9	4.2	73.1	1,356
1,0 56 472,8 53.00 1,004 170 17 182 86 430 178,5 4.47 1.1 39.4 2,0 6,0 457,5 53.90 0,30440 1436 148 185 73 4221 177.1 4.22 14.8 69.5 3,0 6,0 457,5 54,10 0,30451 147 18 759 110 4144 422 177.1 4.22 14.8 69.5 1,0 6,0 226,9 12,33 0,0731 147 18 759 110 4144 489 14.1 1.1 3.0 63.9 1,0 70 247,3 24,38 0,7440 1400 13 400 128 419 4	382	3.0	55	477.1	26.75	0.15426	1481	8	311	202	4119	173.4	4. 1.9	4 .8	74.0	1.354
2.0 6.3 6.50 6.50 5.3.70 0.30440 1636 16 163 73 4221 177.1 ± 2.2 14.8 67.6 17.0 1.0. 1.0. 1.0. 1.0. 1.0. 1.0. 1.0.	383	0,1	38	472.8	55.30	0,30981	1770	17	182	8	1301	178.5	+ 4.7	<u>:</u>	39.6	1.335
3.0 6.0 457.5 54.10 0.30451 1584 18 27.2 71 4200 176.5 ± 2.4 19.0 69.5 1.0 6.0 226.9 12.3 0.03731 1477 19 70 113 163.1 ± 17.5 10.0 69.5 3.0 7.1 21.2 1.2.16 0.07444 1333 14 99.5 142 186.7 ± 17.5 10.0 63.9 3.0 7.1 21.2 1.2.16 0.07444 1833 14 99.5 142 39.5 162.1 ± 17.5 1.0 63.9 1.0 7.0 247.3 24.58 0.15440 1600 13 420 90 444 19.2 11.7 2.4 41.0 2.4 19.2 11.7 2.4 41.0 2.4 19.2 11.7 2.4 41.0 41.0 41.0 41.0 41.0 41.0 41.0 41.0 41.0 41.0 41.0 41.0	363	2.0	જ	455.9	53,90	0.30440	1636	9	185	ĸ	4221	1.77.1	± 2.2	14.8	9.79	1,350
1,0 6,0 226,9 12,33 0,0731 147 19 769 110 4134 1867 417.5 1.0 63.9 2,0 3,9 227,3 12,16 0,00750 132 18 973 142 9565 161.1 2 + 1.1 3.0 78.7 3,0 2,0 2,0 2,1 2,1 2,1 2,1 2,1 2,1 3.5 1.0 43.9 4,0 2,0 2,0 2,1 2,1 2,1 2,1 3.5 1.0 4.90 4.96 162.1 2 + 1.1 3.5 2.8 8.9 3,0 3,0 2,0 2,1 2,1 2,1 2,1 2,1 2,1 2,1 2,1 2,1 2,1 3,0 3,0 2,0 2,0 3,0905 1,7 2,1 2,1 2,1 2,1 2,1 2,1 4,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 2,0 5,0 2	373	3.0	8	457.5	54.10	0.30651	1584	82	2/2	<u>_</u>	4207	176.5	± 2.4	0.61	69.5	1,350
2.0 58 227.3 12.16 0.07550 1402 24 907 128 4010 161.1 ± 1.1 3.0 78.7 3.0 71 221.7 12.10 0.0744 1333 18 955 142 9556 162.1 ± 1.1 3.0 78.7 1.0 70 247.3 24.38 0.15440 160 13 40 161 ± 1.1 3.0 78 2.0 55 25.3 25.36 0.1574 1461 22 760 80 4066 163.1 ± 2.2 7.4 64.8 1.0 53 219.7 51.00 0.30169 172 16.9 400 165.1 ± 2.2 7.4 64.8 1.0 53 219.7 51.00 0.30169 172 2.4 400 16.1 17.2 17.4 64.8 1.0 53 21.0 51.0 0.30169 172 24 64.9 4150 16.7	4	0.1	8	226.9	12.33	0.07311	1477	6	769	0.	4134	168.7		0,1	63.9	1.312
3.0 71 221,7 12.10 0.00444 133 18 935 142 3956 162.1 ± 3.5 2.8 81.0 1.0 70 247.3 24.8 0.15440 1600 13 420 904 4246 197.2 ± 11.7 2.4 2.0 53 223.4 25.15 0.15342 1487 21 60 4086 163.1 ± 2.2 7.4 40.8 1.0 53 223.6 25.16 0.15342 1487 21 60 4086 163.1 ± 2.2 7.4 436 169.4 ± 10.5 17.4 43.0 2.0 53 219.7 51.00 0.30103 1726 15 40 436 16.7 ± 17.7 23.4 43.0 2.0 57 211.3 50.25 0.30095 1578 24 41 436 16.7 415 27.7 43.0 14.3 41.3 41.3 41.3 4	5	2.0	58	227.3	12.16	0.07550	1402	24	206	128	4010	1.16		3.0	7.8.7	1.292
1.0 70 247.3 24.58 0.15440 1600 13 420 80 4246 195.2 ±11.7 2.4	704	3.0	71	7.122	12.10	0.07464	1353	82	935	142	3956	162.1	+ 3,5	2.8	83.0	1.318
2.0 55 223.7 25.15 0.15242 1457 21 618 84 4137 145.1 ± 2.2 7.4 64.8 3.0 53 225.8 25.40 0.15574 1481 22 760 80 4066 163.1 ± 2.2 7.4 64.8 1.0 53 219.7 51.00 0.30103 1726 15 64 4366 169.4 ± 10.5 11.2 75.1 2.0 57 211.3 50.25 0.30095 1726 24 547 61 4202 167.0 ± 1.7 23.4 57.1 4.3 4.5 57.1 4.3 4.3 57.1 4.3 4.	392	1.0	02	247.3	24.58	0.15440	1600	13	420	8	4246	159.2	± 11.7	7.4	•	1.208
3.0 5.3 225.8 25.40 0.15574 1481 22 760 80 4086 163.1 ± 2.2 11.2 75.1 1.0 5.3 219.7 51.00 0.30103 1726 15 336 64 4368 163.1 ± 1.2.4 43.0 2.0 5.7 211.3 50.25 0.30095 1578 24 51 167.9 ± 1.2.4 43.0 12.4 ± 0.5 1.2.4 43.0 12.2 12.4 43.0 12.4 51.7 32.4 51.3 4.5 12.4 52.4 71.5 20.2 1.2.4 4.5 22.4 71.5 1.2.4 4.2 12.5 32.4 72.5 4.5 12.5 24.0 12.4 4.1 12.1 4.5 2.0 51.5 22.20 0.07391 138 19 200 4.1 14.7 1.7 4.5 2.0 13.9 4.1 14.7 1.4 1.7 3.4	388	2.0	92	223.7	25.15	0.15242	1457	21	819	æ	4137	1.65.1	± 2.2	7.4	2 .	1.283
1,0 53 19,7 51,00 0,30103 1726 15 336 64 4368 169,4 ± 10.5 12.4 43.0 2,0 57 211,3 50.25 0,30095 1578 24 547 61 4202 16.5 ± 1.7 23.4 52.3 3,0 79 220,7 52.00 0,31819 1570 2 200 122 4193 151,3 ± 4.5 2.0 51.8 1,0 59 10,71 11.00 0,07154 1422 2 2400 122 4199 154,0 ± 1.5 3.0 71.8 2,0 60 105,2 20,07154 1422 2 2400 122 4199 154,0 ± 1.9 5.0 7.8 2,0 60 105,2 20,07154 1422 2 2400 122 4194 147,2 2.9 3.0 7.8 2,0 60 105,2 1492 14 417	38	3.0	53	225.8	25.40	0,15574	1481	22	760	8	4086	163.1	± 2.2	11.2	75.1	1.284
2.0 57 211.3 50.25 0.30095 1578 24 547 61 4202 167.0 ± 1.7 23.4 52.3 3.0 79 220,7 52.80 0.31819 1570 20 789 55 4151 165.9 ± 2.7 38.4 71.5 1.0 59 110,7 11.20 0.07401 1538 19 2800 102 4193 151.3 ± 4.5 2.0 51.8 2.0 63 107.1 11.02 0.0744 1422 27 2400 122 4219 154.0 ± 2.7 3.0 51.8 2.0 67 107.4 11.02 0.07393 1432 14 4174 147.2 ± 1.9 6.2 79.8 2.0 67 107.4 11.02 0.07393 1482 14 4174 147.2 ± 1.9 6.2 79.8 2.0 60 107.4 1422 24 2300 6.3 4	378	1.0	53	219.7	51.00	0,30103	1726	15	336	3	4368	169.4	± 10.5	12.4	43.0	1.248
3.0 79 220,7 52,80 0,31819 1570 20 789 55 4151 165,9 ± 2.7 38.4 71.5 1.0 59 110,7 11,20 0,07401 1538 19 2800 102 4193 151.3 ± 4.5 2.0 51.8 2.0 63 107.1 11,02 0,07343 1338 19 2800 122 4219 154.0 ± 2.0 51.8 3.0 67 107.4 11,08 0,07343 1338 19 2300 97 4095 149.9 ± 1.9 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 1.0 7.8 4.2 7.2 9.2 7.8 4.2 7.4 7.4 <	391	2.0	57	211.3	50.25	0.30095	1578	7.7	547	5	4202	167.0	± 1.7	23.4	52.3	1.278
1.0 59 110.7 11.20 0.07401 1538 19 2800 102 4193 151.3 ± 4.5 2.0 51.8 2.0 63 107.1 11.02 0.07154 1422 27 2400 122 4219 154.0 ± 2.9 3.0 70.8 3.0 67 107.4 11.08 0.07393 1338 19 3300 97 4095 149.9 ± 1.9 6.2 79.8 2.0 60 105.2 22.20 0.15685 1485 16 1735 64 4174 147.2 ± 2.1 13.9 64.2 3.0 54 120.0 26.15 0.17560 1492 24 2300 63 4090 148.9 ± 2.1 13.9 64.2 2.0 70 10.14 43 4167 153.1 ± 2.4 22.4 22.4 23.0 70.7 3.0 52.1 9.42 0.07390 1407 40 <t< td=""><td>37.2</td><td>3.0</td><td>79</td><td>220.7</td><td>52.80</td><td>0,31819</td><td>1570</td><td>8</td><td>789</td><td>55</td><td>4151</td><td>165.9</td><td>+ 2.7</td><td>38.4</td><td>71.5</td><td>1.286</td></t<>	37.2	3.0	79	220.7	52.80	0,31819	1570	8	789	55	4151	165.9	+ 2.7	38.4	71.5	1.286
2.0 6.3 107.1 11.02 0.07154 1422 27 2400 122 4219 154.0 ± 2.9 3.0 70.8 3.0 67 107.4 11.08 0.07393 1338 19 3300 97 4095 149.9 ± 1.9 6.2 79.8 2.0 60 105.2 22.20 0.15685 1485 16 1735 64 4174 17.2 ± 2.1 13.9 64.2 3.0 54 120.0 26.15 0.17560 1492 24 2300 63 4090 148.9 ± 2.4 22.4 72.6 2.0 70 110.4 51.35 0.27569 1560 20 2780 38 4087 14.3 ± 1.9 6.5 70.7 2.0 50.18 9.42 0.07390 1407 40 3000 57 4220 12.4 ± 1.9 6.5 70.7 2.0 50.8 9.17 0.07371 <	Ę	0.1	59	110.7	11.20	0.07401	1538	6	2800	102	4193	151.3	+ 4.5	5.0	51.8	1.161
3.0 67 107.4 11.08 0.07393 1338 19 3300 97 4095 149.9 ± 1.9 6.2 79.8 2.0 60 105.2 22.20 0.15605 1465 16 1735 64 4174 147.2 ± 2.1 13.9 64.2 3.0 54 120.0 26.15 0.17560 1492 24 2300 63 4090 148.9 ± 2.4 22.4 72.6 2.0 70 110.4 51.35 0.13545 1627 19 1414 43 4167 153.1 ± 3.5 46.5 39.7 2.0 74 89.0 39.56 20 2780 38 4087 14.3 ± 1.9 60.7 70.7 2.0 52.1 9.42 0.07390 1407 40 3000 57 408 124.4 ± 2.7 11.0 78.7 2.0 69 52.1 19.55 0.14728 1472 2	405	2.0	3	107.1	11.02	0.07154	1422	D)	2400	122	4219	154.0	± 2.9	3.0	70.8	1.175
2.0 60 105.2 22.20 0.15685 1485 16 1735 64 4174 147.2 ± 2.1 13.9 64.2 3.0 54 120.0 26.15 0.17560 1492 24 2300 63 4090 148.9 ± 2.4 22.4 72.6 2.0 70 110.4 51.35 0.23545 1620 20 2780 38 4087 143.3 ± 1.9 60.7 70.7 3.0 74 89.0 0.27569 1560 20 2780 38 4087 143.3 ± 1.9 60.7 70.7 2.0 69 52.1 9.42 0.07390 1407 40 3000 57 4220 124.4 ± 2.7 11.0 78.7 2.0 69 52.1 19.55 0.16138 150 5 4088 121.1 ± 5.0 22.8 52.0 3.0 64 46.6 17.10 0.14728 1472 <td< td=""><td>904</td><td>3.0</td><td>29</td><td>107.4</td><td>1.08</td><td>0.07393</td><td>1338</td><td>6</td><td>3300</td><td>6</td><td>4095</td><td>149.9</td><td>6 I +</td><td>6.2</td><td>79.8</td><td>1.17</td></td<>	904	3.0	29	107.4	1.08	0.07393	1338	6	3300	6	4095	149.9	6 I +	6.2	79.8	1.17
3.0 54 120.0 26.15 0.17560 1492 24 2300 63 4090 148.9 ± 2.4 22.4 72.6 2.0 70 110.4 51.35 0.33545 1627 19 1414 43 4167 153.1 ± 3.5 46.5 39.7 3.0 74 89.0 39.50 0.27569 1560 20 2780 38 4087 14.3 ± 1.9 60.7 70.7 2.0 69 52.1 9.42 0.07390 1407 40 3000 57 4220 124.4 ± 4.8 7.2 65.7 3.0 50.8 9.17 0.07371 1362 15 5100 68 4125 124.4 ± 2.7 11.0 78.7 2.0 69 52.1 19.55 0.16138 1599 22 3000 55 4088 121.1 ± 3.0 34.9 77.4 Avverage of two flowmeters in series. 17.10 0.14728 <td>Q</td> <td>2.0</td> <td>8</td> <td>105.2</td> <td>22.20</td> <td>0.15085</td> <td>1485</td> <td>9</td> <td>1735</td> <td>3</td> <td>4174</td> <td>147.2</td> <td>± 2.1</td> <td>13.9</td> <td>64.2</td> <td><u>-</u>.</td>	Q	2.0	8	105.2	22.20	0.15085	1485	9	1735	3	4174	147.2	± 2.1	13.9	64.2	<u>-</u> .
2.0 70 110.4 51.35 0.33545 1627 19 1414 43 4167 153.1 ± 3.5 46.5 39.7 3.0 74 89.0 39.50 0.27569 1560 20 2780 38 4087 143.3 ± 1.9 60.7 70.7 2.0 69 52.1 9.42 0.07371 1362 15 5100 68 4125 124.4 ± 4.8 7.2 65.7 2.0 69 52.1 19.55 0.16138 1509 55 4088 121.1 ± 5.0 22.8 52.0 2.0 64 46.6 17.10 0.14728 1472 23 2200 48 4006 116.11 ± 3.0 34.9 77.4 Average of two flowmeters in series. 17.10 0.14728 1472 23 2200 48 4006 116.11 ± 3.0 34.9 77.4 Average of two flowmeters in series. 15 set electrodition of contribute of contribute chamber pressu	380	3.0	54	120.0	26.15	0.17560	1492	54	2300	প্ত	4090	148.9	± 2.4	22.4	72.6	1.17
3.0 74 89.0 39.50 0.27569 1560 20 2780 38 4087 143.3 ± 1.9 60.7 70.7 2.0 69 52.1 9.42 0.07371 1362 15 5100 68 4125 124.4 ± 4.8 7.2 66.7 3.0 50.8 9.17 0.07371 1362 15 5100 68 4125 124.4 ± 2.7 11.0 78.7 2.0 69 52.1 19.55 0.16138 1509 22 3000 55 4088 121.1 ± 5.0 22.8 52.0 3.0 64 46.6 17.10 0.14728 1472 23 2200 48 4006 116.1 ± 3.0 34.9 77.4 Average of two flowmeters in series. 10.8 of steady state chamber pressure. (4) Time from chamber pressure start decay to 10% of steady state chamber pressure. (5) See level conditions or start decay to 22.01 10.4.9 17.14 1.7.10 1.7.10 1.7.10 1.7.10	397	2.0	70	110.4	51,35	0,33545	1627	61	111	Q	4167	153.1	+ 3.5	46.5	39.7	1.182
2.0 69 52.1 9.42 0.07390 1407 40 3000 57 4220 127.48 ± 4.8 7.2 66.7 3.0 79 50.8 9.17 0.07371 1362 15 5100 68 4125 124.4 ± 2.7 11.0 78.7 2.0 69 52.1 19.55 0.16138 1509 22 3000 55 4088 121.1 ± 5.0 22.8 52.0 3.0 64 46.6 17.10 0.14728 1472 23 2200 48 4006 116.1 ± 3.0 34.9 77.4 Average of two flowmeters in series. (4) Time from chamber pressure start decay to 10% of steady state chamber pressure. (5) See level conditions at expansion ratio of 20.01.1 ± 3.0 34.9 77.4 11ine from propellant entry into chamber pressure. (5) See level conditions at expansion ratio of 20.01.1 4.04.0 4.04.0 4.04.0 4.04.0 4.04.0 4.04.0 4.04.0 4.04.0 4.04.0 4.04.0 4.04.0 4.04	375	3.0	74	89.0	39.50	0.27569	1560	8	2780	8	4087	143.3	4 - 1.9	7.09	7.07	1.128
3.0 79 50.8 9.17 0.07371 1362 15 5100 68 4125 124.4 ± 2.7 11.0 78.7 2.0 69 52.1 19.55 0.16138 1509 22 3000 55 4088 121.1 ± 5.0 22.8 52.0 3.0 64 46.6 17.10 0.14728 1472 23 2200 48 4006 116.1 ± 3.0 34.9 77.4 Average of two flowmeters in series. (4) Time from chamber pressure start decay to 10% of steady state chamber pressure. (5) Sea (level conditions at expansion ratio of 2.0.1.1 ± 3.0 34.9 77.4 Time from propellant entry into chamber to 1% of steady state chamber pressure. (5) Sea (level conditions at expansion ratio of 2.0.1.1 4.0 4.0 4.0 4.0 4.0 4.0 4.0 77.4 4.0	904	2.0	69	52.1	9.45	0.07390	1407	9	3000	23	4220	127.48	+ 4.8	7.2	66.7	0.9718
2.0 69 52.1 19,55 0.14728 1509 22 3000 55 4088 121.1 ± 5.0 22.8 52.0 3.0 64 46.6 17.10 0.14728 1472 23 2200 48 4006 116.1 ± 3.0 34.9 77.4 Average of two flowmeters in series. (4) Time from chamber pressure start decay to 10% of steady state chamber pressure. (5) See level conditions an expansion ratio of 2.0:1. 22.8 77.4 Time from propellant entry into chamber to 1% of steady state chamber pressure. (5) See level conditions an expansion ratio of 2.0:1. 4.0 <t< td=""><td>604</td><td>3.0</td><td>79</td><td>8'09</td><td>9.17</td><td>1.02.0</td><td>1362</td><td>15</td><td>5100</td><td>88</td><td>4125</td><td>124.4</td><td>± 2.7</td><td>0.1</td><td>7.8.7</td><td>0.9702</td></t<>	604	3.0	79	8'09	9.17	1.02.0	1362	15	5100	88	4125	124.4	± 2.7	0.1	7.8.7	0.9702
3.0 64 46.6 17.10 0.14728 1472 23 2200 48 4006 116.1 ± 3.0 34.9 77.4 Average of twu flowmeters in series. (4) Time from chamber pressure start decay to 10% of steady state chamber pressure (5) See level conditions at expansion ratio of 2.0.1. (5) Name and propellant entry into chamber to 1% of steady state chamber pressure. (6) Name and propellant entry into chamber to 1% of steady state chamber pressure. (7) Name and propellant entry into chamber to 1% of steady state chamber pressure. (8) Name and propellant entry into chamber to 1% of steady state chamber pressure.	402	2.0	69	52.1	19,55	0,16138	1509	22	3000	ઝ	4088	121.1	± 5.0	22.8	52.0	0.9533
Average of two flowmeters in series. Time from propellant entry into chamber to 1% of steady state chamber pressure. (4)	374	3.0	2	46.6	17.10	0.14728	1472	23	2200	₩	4006	1.6.1	+ 3.0	94.9	77.4	0.9324
Time from propellant entry into chamber to 1% of steady state chamber pressure. (5)		eroos of two	flowmeters in se	eries.						om chamber p	ressure start de	cay to 10% o	steady state	amber pressur	•	
The state of the s		e from prope	flont entry into	chamber to 1%	of steady sto	ne chamber p	essure.			el conditions	at expansion re	atio of 2.0:1.	now out own	in to nitroger	mole ratios.	

TABLE XV SUMMARY OF 0.5 Ibf ENGINE BED LOADING, CHAMBER PRESSURE, AND BED LENGTH STUDIES

	T 1987-0	,								Chomber			
Bed Ca ength Temp	Catalyst emperature	Chamber Pressure	Thrust	Flowrate	Ignition Delay	Response Time	Decay Time	Characteristic Velocity	Specific Impulse	Pressure Roughness	Catalyst Bed Pressure Drop	Ammonia Dissociation	Thrust Coefficient
	4	psia	<u>1</u>	lbm/sec	æ	SEE.	\$E	ft/sec	bf-sec/lbm	% peak-to-peak	psid	mole %	
,	-9	53.6	0.305	0.002562	0	880	148	4004	118,9	±7.3	10.1	63.0	0.9572
	02	107.5	0.335	0.002341	2	4	8	4914	143.0	+ 5.6	5.1	8.73	1.112
	35	238.3	0.410	0.002504	5	8 48	970	4182	163.7	+ 4.9	3.5	62.2	1,2593
	*8	485.5	0.426	0.002474	18	009	470	4246	172.5	± 1,2	0.1	57.5	1,3043
	2	1000	0.409	0.002341	2	317	510	1017	174.7	÷ 1.5	0	62.5	1,3705
	65	7. 701	0.740	0,004858	ۍ	300	4	4256	152.4	÷ 5,9	18.3	53,4	1.1558
	65	225.5	0.811	0.004913	S	317	3	4212	165.2	4.6.7	13.6	55.0	1.022
	S	473.7	0.880	0.004920	15	359	370	4250	179.2	+ 2.4	4.5	i	1,3540
	65	6.694	0.858	0,004939	13	294	285	4200	174.1	± 2.8	4.2	0.85	1 3308
	88	1000	0.922	0.005120	٥	283	9	4237	180.3	+ 2.5	0	8.98	1.3677
	83	205.1	1.580	0.009312	7	357	147	4212	169.5	+ 2.2	25.0	57.1	1,2958
	19	696	1.844	151010,0	S	174	185	4220	181.7	± 5.6		54.2	1.3870
	7	51.9	0.292	0,002522	-	2050	200	39.59	115.8	+ 3.7	19.4	81.5	0.9464
	ኧ	112.6	0.360	0.002511	7	1143	183	4085	143.4	± 2.2	11,3	1.19	1.1309
	63	240.1	0.414	0.002605	0	810	295	4069	0.651	. + 3.1	3.8	75.2	1,2568
	70	472.3	0.424	0.002578	7	1260	4	3973	1 <u>6</u> 4.8	± 0.7	3.2	72.4	1,3318
	51	1005	0.418	0.002364	7	323	510	4093	177.5	± 1.2	2.0	1.79	1.395
	19	52.9	0,643	0,005494	60	1400	8	3939	117.5	+2.6	56.0	1	196.0
	35	109.6	0.742	0.005252	νo	575	138	4004	141.5	+ 3.2	30.1	76.3	1.1388
	65	221.5	96.70	1	٥	930	1	ł	;	+3.6	16.6	79.2	1.2712
	וג	460.7	0.818	1	15	816	490	ł	;	±2.4	10.0	72.8	!
	8	475.7	0.841	0.004946	. 15	546	328	4218	170.5	± 2.1	7.6	1	1,3500
	79	1000	0.925	0.005198	=	358	;	4155	178.2	1.1.1	3.0	8.89	1.305
	29	245.2	;	0.011063	2	. 219	132	4239	:	± 2.0	17.5	1	;
	55	212.5	1,670	0,009938	6 0	495	\$	4090	1.89.	÷1.9	54.2	0.97	1.3219
	99	449.5	1.692	0.009699	0	330	615	4215	174.5	± 2.0	33.0	76.5	1,3315

TABLE XV (Cont'd)
SUMMARY OF 0.5 Ibf ENGINE BED LOADING, CHAMBER PRESSURE, AND BED LENGTH STUDIES

		Initial	Downstream								Chamber			
Test No.	Bed Length	Catalyst Temperature	Chamber	Thrust	Flowrate	Ignition Delay	Response Time	Decay Time	Characteristic Velocity	Specific impulse	Pressure Roughness	Catalyst Bed Pressure Drop	Ammonia Dissociation	Thrust Coefficient
	. <u>e</u>	y	psia	I₽€	tbm/sec	Ě	Ĕ	Ě		lbf-sec/lbm	% peak -to-peak	psid	% ejou	
421	1.25	85	957	0.820	0.01011	=	<u>ا</u>	380	ı	179.8	+2.5	17.0	69.5	1.385
455	2.0	86	52.8	0.307	0.002580	12	3800	130		119.2	4.6.+1	9.62	8.18	0.9780
75.4	2.0	23	113.3	0,358	0.002629	6	1770	255		136.3	4.1+	15.0	83.2	1,1177
448	2.0	73	241.7	0.430	0.002693	80	1202	300		0.091	+ 3.3	7.0	9.62	1,2967
450	2.0	23	471.9	0.42	0.002575	2	2020	320		 8	+0.7	3.0	71.2	345
452	2.0	65	1005	0.464	0.002428	<u>E</u>	323	286		180.5	9.0+	0.1	71.3	1.382
430	2.0	55	104.0	0.713	0,005008	۰	3200	3		142.5	0.1+	56.5	85.6	1,1532
42	2.0	8	226.9	0.817	0.005088	=	1010	009		8.091	8.1.4	28.6	82,5	1.27.37
425	2.0	73	466.3	0.854	0.005277	17	2350	137		162.0	+ 2.2	13.6	29.5	1,3353
428	2.0	19	1018	0.930	0,005184	=	378	9 5		179.5	+0.7	3,4	75.5	1,3552
418	2.0	88	434.5	1.640	0.009730	7	782	322		168.4	+2.1	43.4	7.77	1,3351
419	2.0	2	925	1.722	0.009958	Ξ	838	265		173.3	± 3.0	26.0	7.5.7	1.3569

7.3.1 Ammonia Dissociation

Analysis and correlation of the ammonia dissociation data indicated that diffusion of the reactants and products to and from the catalyst surface may be important in the amount of ammonia dissociation which occurs in the reactor. In view of the apparent importance of diffusion controlling dissociation of ammonia, a relation was developed relating fractional ammonia dissociation to temperature, bed loading, chamber pressure, residence time, and catalyst particle size for the limiting case of zero ammonia concentration at the catalyst surface. That is, it is assumed that chemical equilibrium is obtained if the ammonia reaches the catalyst surface. This relation developed is given as:

$$\int_{X}^{X_{1}} \frac{dX}{(1-X)(3+X)(5-4X)(1650-780X^{2})} = K_{d} d_{p}^{m} \frac{G^{0.71}}{P}$$

Where

X = Fractional ammonia dissociation

K_d = Experimental constant

d_p = Catalyst particle diameter, ft.

m = Experimental constant

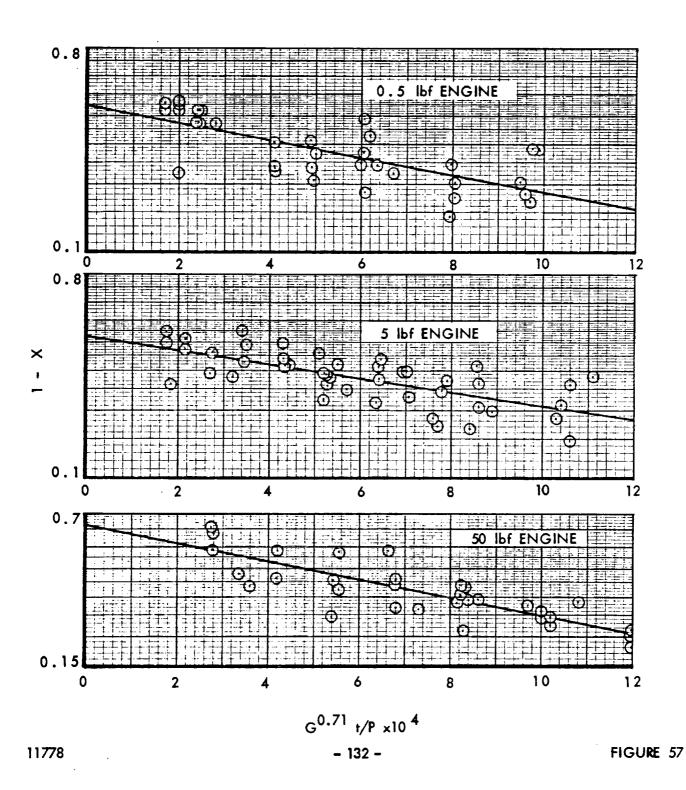
G = Superficial bed loading lbm/in²-sec

t = Residence time, ms

P = Average chamber pressure, psia

Examination of the above equation indicates that for a given particle size, the ammonia dissociation should be proportional to the parameters G^{0.71}t/P. Ammonia dissociation data obtained from the 0.5, 5, and 50 lbf engines is plotted against this group in Figure 57 to test its usefulness as a correlation parameter. As can be seen a quite consistent correlation is obtained at all three thrust levels.

FOR A DIFFUSION CONTROLLED REACTION



Additional correlation of the data was accomplished to develop an expression which includes the effect of particle size on an ammonia dissociation. The semi-empirical equation developed is given by:

In
$$\left(\frac{1-X_0}{1-X}\right) = -153.2 \, d_p^{-0.32} \, \frac{G^{0.71}t}{P}$$

Where previously undefined parameters are:

X₀ = Zero time intercept on plot of experimental data.

Ammonia dissociation data from all three thrust levels is plotted and compared to the above equation in Figure 58. Although there is some scatter in the data it does appear very useful for initial design purposes.

The 3 of deviation of the data from that given by the above equation is 6%.

7.3.2 Catalyst Bed Length Requirements

During the program, tests were conducted to define the minimum catalyst bed length requirements required for smooth and stable operation. This data was correlated and an empirical expression developed to relate catalyst bed length requirements to bed loading, chamber pressure, and catalyst specific surface area. This relation is given as:

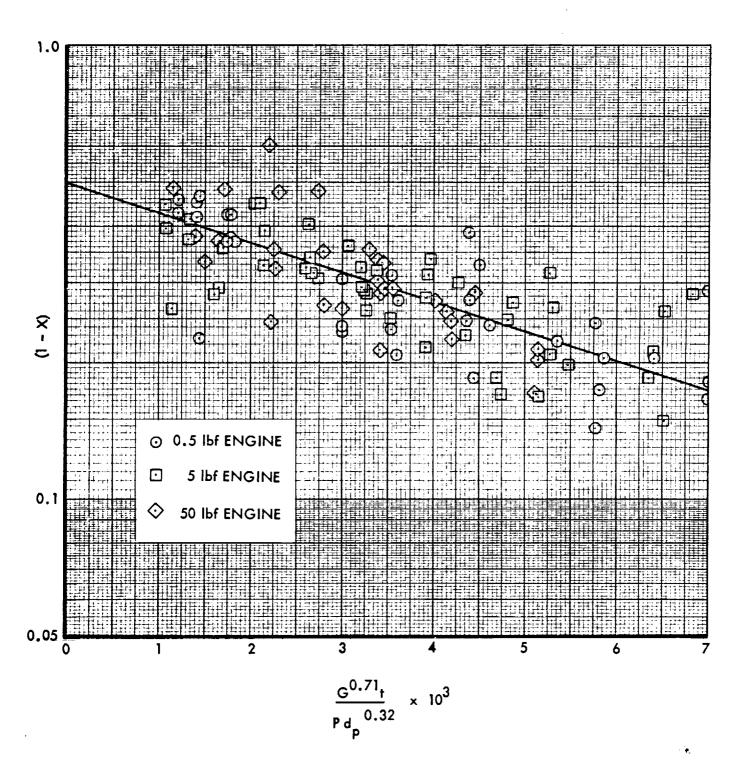
$$L_B = 0.2 + 145 \frac{G^{0.554}}{P_c^{0.306} A_s^{0.3}}$$

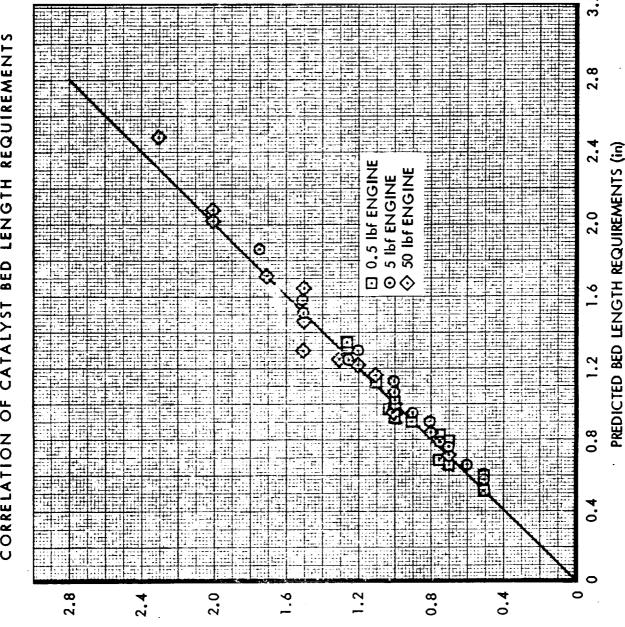
The bed length predicted by the above equation is compared with that found experimentally in Figure 59. It should be noted that the use of the above equation will result in an ammonia dissociation of 55 to 60%.

7.3.3 Catalyst Bed Pressure Drop

Experimental catalyst bed pressure drop data was compared to a relation developed by Grant (Reference 3) in his work with the nonspontaneous catalyst and with the Ergun equation (Reference 13) to see if those equations adequately predicted the measured catalyst bed pressure drop. Data obtained is compared with that predicted by Grants equation in

GENERAL CORRELATION OF AMMONIA DISSOCIATION DATA





EXPERIMENTAL BED LENGTH REQUIREMENTS (in)

Figure 60. As can be seen quite good correlation is obtained with all test data. The Ergun equation was found not to fit the experimental data throughout the full range of Reynolds number covered and is not recommended for use.

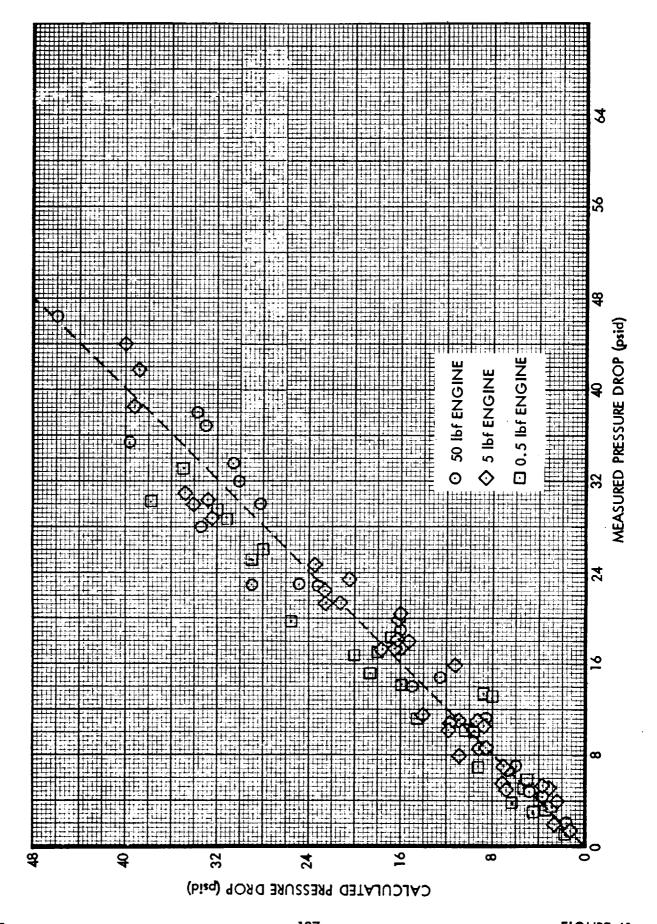
7.3.4 Chamber Pressure Response Time

Chamber pressure rise time is defined herein as the time for chamber pressure measured downstream of the catalyst bed to change from 1% of the steady state value to some specified higher percentage of the steady state pressure. An analytical model of the pressure rise time was developed by assuming complete decomposition during the start transient and then empirically modifying the model generated to account for kinetic effects (i.e., rate limitations imposed by propellant atomization process and/or decomposition reaction kinetics). The model was developed treating the pressure rise transient as a two stage process.

Stage 1 is treated as an isothermal pressurization process in which the accumulation of gas in the reactor void space is the predominant factor. The system temperature is assumed to be constant at the initial catalyst temperature during this relatively short portion of the pressure rise period. During Stage 2, the catalyst bed heat up as it affects the temperature of the gas entering the nozzle is considered to be the predominant factor. The result of this analysis is:

$$\uparrow_{1} \frac{\kappa_{c1} \bar{M}_{1} \vee_{c} P_{cd \infty}}{\dot{w}_{\infty} RT_{co}} \int_{0}^{\eta_{1}} \frac{d\eta}{\sqrt{\frac{(F-\eta)\eta}{(F-D)\eta + (D-1)Z} - \eta \sqrt{\frac{1}{Z}}}}$$

$$t_2 = K_c^2 \frac{C_c (F-D)^{3/2}}{C_{pg} \dot{w}_{\infty}} \int_{\eta_1}^{\eta} \frac{(2F-D\eta)\eta d\eta}{(F-D\eta)^{3/2} [F-D\eta - (F-D)\eta^2]}$$



Where:

$$\overline{M}_1$$
 = Average molecular weight, lbm/lb mole

$$V_{a} = Volume to be pressurized, in3$$

$$P_{cd \infty}$$
 = Steady state chamber pressure, psia

$$F = P_f/P_{cd} \infty$$
 (feed ratio)

D =
$$P_{cu}/P_{cd}$$
 (catalyst bed pressure drop ratio)

$$77 = P_{cd}/P_{cd} \infty \text{ (fractional approach of downstream chamber pressure to steady state)}$$

$$\gamma_0 = \text{Value of } P_{cd} / P_{cd} \infty \text{ at end of ignition delay}$$

$$K_{22}$$
 = Stage 2 empirical constant

$$\bar{C}_{pa}$$
 = Gas specific heat, Btu/16°F

The value of γ_1 is given by:

$$\eta_{1} = -\frac{DT_{co}}{2(F-D) T_{co}} + 1/2 \sqrt{\frac{DT_{co}}{(F-D) T_{co}}^{2} + \frac{4FT_{co}}{(F-D) T_{co}}}$$

From experimental test data the empirical constants in the above equations were developed as:

$$K_{c1} M_1 = \frac{3.69 \times 10^4}{P_{dm}}$$

$$\frac{K_c^2}{C_{pg}} = \frac{570}{P_f}$$

8.0 CATALYST DEGRADATION MEASUREMENTS

Catalyst changes as a function of accumulated engine burn time were correlated by three means. Periodic weight measurements were made of the catalyst from which catalyst loss rates could be calculated. Additionally, samples of catalyst were periodically removed from the engine and measurements were made of the total catalyst surface area and of the active metal surface area. Total catalyst surface area was measured using nitrogen adsorption techniques while the active metal surface area was measured by hydrogen chemisorption. For all surface area measurements, the catalyst was reduced in a hydrogen atmosphere at 500°F for one hour prior to the measurement being made.

Due to the nature of the program (i.e., investigation of many variables) it was not possible to obtain quantitative measurements of catalyst loss rates. However, several qualitative trends were noted which are discussed in the ensuing paragraphs.

Optimization tests were conducted with granular or pellet size catalyst all made on a Harshaw alumina carrier. The granular catalyst was made by breaking $1/8" \times 1/8"$ pellets into the desired mesh size. The loss rates for these granular pellets tended to be higher by a factor of at least 10 than that for the $1/8" \times 1/8"$ pellets. It is strongly felt that this method of manufacturing results in a catalyst structurally inferior to the $1/8" \times 1/8"$ pellets. Subsequent testing on the program employed granular catalyst made on the Reynolds RA-1 alumina carrier. This carrier is made in granular pellets and was found to have much lower loss rates (reduction by a factor of up to 10) than that of the Harshaw granular discussed above. During later phases of the program a granular catalyst which was prepared on the Reynolds alumina carrier and subsequently surface hardened (Shell Development Company Proprietary Procedure) was tested. Further reduction in loss rates were noted with this catalyst.

During the studies of the effect of bed loading upon reactor operation it was noted that loss rates increased with increasing bed loading. Although no quantitative numbers were obtained a definite correlation between loss rate and bed loading was noted.

As stated above, samples of the catalyst were periodically removed from the engine and surface area measurements made. In most cases the catalyst was removed from a point in the chamber just below the layer of fine mesh catalyst. Thermocouple measurements had indicated that the flame front was near this point, and thus, the surface area changes should be the greatest at this point of maximum temperature.

Results of the hydrogen chemisorption and nitrogen absorption measurements are summarized in Table XVI. A rather large drop-off in both carrier and metal surface area is noted with run time. This drop-off appears to occur after a short period of test time has been accumulated on the catalyst. After this drop-off the carrier and metal surface areas appear to stabilize at approximately 70% and 50% of their original values respectively. It should be noted that the engine testing with the catalyst summarized in Table XVI indicated essentially no change in reactor operation despite the rather large surface area changes.

ABLE XVI

	Measured H ₂ Chemisorption p mole/gm & 0°C	226	354	230	260	280	302	260
	Measured BET Area m ² /gm	78	81	74	68	115	86	&
CHANGES	Original H ₂ Chemisorption u mole/gm © 0°C	480	480	480	480	480	480	482
CATALYST SURFACE AREA CHANGES	Original BET Area m ² /gm	118	118	118	118	139.5	122.5	118
CATALYST SU	Accumulated Test Time sec	296	421	969	730	475	1420	2100
	Catalyst Size	1/8" × 1/8" Cylind- rical pellets				10-12 Mesh	20-25 Mesh	12-16 Mesh
	Engine Thrust 16f	20				5	5	5

	•	
•		

9.0 100 lbf ENGINE

9.1 Design

To test the validity of the design and scaling formulae at higher thrust levels a 100 lbf engine was designed and subjected to testing. The design criteria used was as outlined in Volume II of the subject report. Detailed analyses of the catalyst bed design are outlined in Volume II, Appendix I.

The design of the 100 lbf thrust engine is shown in Figure 61. Pertinent reactor design parameters and estimated engine performance are summarized in Table XVII.

The engine chamber is made of Haynes Alloy Number 25 to which is welded a 347 stainless steel nozzle of 4:1 expansion ratio. The showerhead injector, made of 347 stainless steel, is flanged to the chamber. Propellant is supplied to a distribution manifold in the injector through a single supply tube. The upper part of the catalyst bed contains 0.2 inches of 25-30 mesh granular catalyst contained in a 60 x 60 mesh molybdenum screen basket. The remainder of the catalyst bed is $1/8" \times 1/8"$ cylindrical pellets. A photograph of the engine assembly is shown in Figure 62.

9.2 Test Results

All tests with the 100 lbf engine were conducted at ambient temperature and pressure conditions. A total of six (6) steady state tests each of 30 seconds duration were conducted. The test data from the engine is summarized in Table XVIII. A gas sample of the decomposition products was taken during the last two tests and analyzed using a gas chromatograph. This data is also summarized in Table XVIII.

Very smooth start transient and steady state operation was achieved in all tests. Characteristic velocity average 4,240 ft/sec which is within 0.45 percent of the value predicted for the engine. Sea level specific impulse and thrust coefficient corrected to 193.5 psia chamber pressure averaged 166.80 and 1.265 respectively. Ammonia dissociation, as determined by gas sample analysis was 62.5% which is within 2.5% of the 60% predicted value.

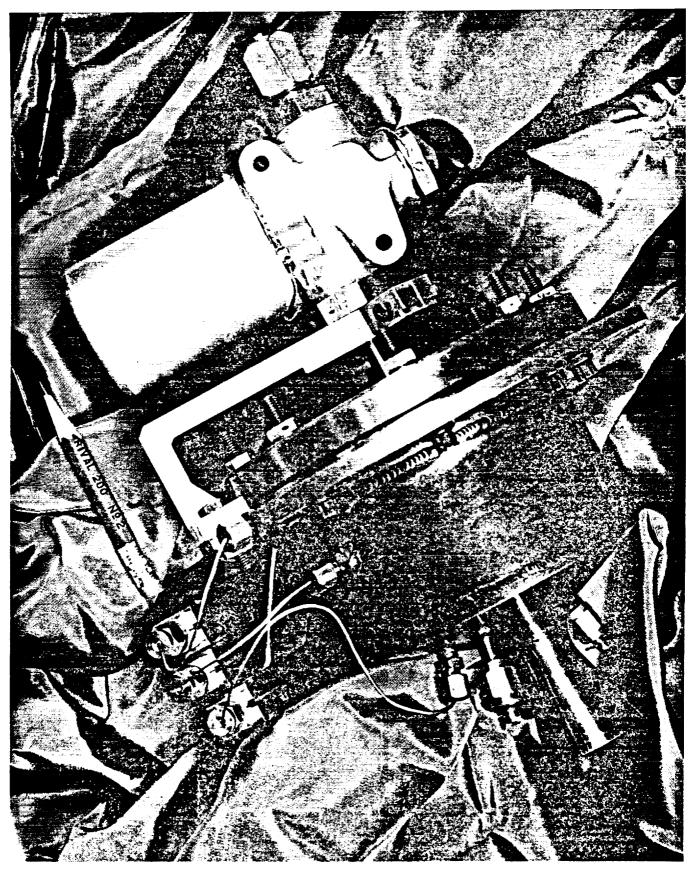
In summary, the test results obtained with the 100 lbf engine were virtually identical with that predicted using the design and scaling formula developed at the lower thrust levels. The validity of using the design and scaling formula at higher thrust levels was therefore clearly established.

1111 - 11

.

REVISIONS DATE APPROVED D SHELL DEVELOPMENT CORP EMERYVILLE , CALIF. DOW CORNING CORP. 3033 W. CATALYST NO 405 24 . LUBE 06-11 MISSION RD, ALHAMBRA, CALIF 23 22 Zί 2-41-E515-B PARKER SEAL CO. 20 "O"-RING 19 18 17 ے ا NAS 1351 15 8 14 M635769 13 GASKET -86 M621042 12 8 LOCKWIT . . 10 ANGLOCIOL WASHER 8 9 8 RIII -03360 SCREEN 7 6 5 24670-9 NOTELE ASSY INJECTOR BOOK 4 3 24-47-1 INJECTOR PL BED PLATE 24597-39 BACKET ASSY NOMENCLATURE OR DESCRIPTION ITEM NO. SPECIFICATION LIST OF MATERIALS ROCKET RESEARCH CORPORATION SEATTLE, WASHINGTON UNLESS OTHERWISE SPECIFIED 6-15-6 6-19/64 Z 1/1 Ju. 6/10/6 DO NOT SCALE DRAWING ROCKET ENGINE -100 LBF, HYDRAZINE, SHOWERHEAD INJECTOR 1 ENDITEM JPL 100 CODE IDENT. NO DWG DWG NO. PART MEIT PHAI NEIT ASSY USED ON 21562 D 24666 AFFLICATION DWG LEVE SCALE 1/1 RELEASE DATE 6-10-4 SHEET CHARGE NO. 171-31 2 7.5 - 145-A FIGURE 61

	-	
·		
·		



- 147 -

TABLE XVII 100 1bf ENGINE DESIGN PARAMETERS

Performance

100 lbf Vacuum Thrust 4262 ft/sec Predicted Characteristic Velocity 0.4255 lbm/sec Propellant Flow Rate 200 psia Downstream Chamber Pressure 230 psia Upstream Chamber Pressure $0.045 \, lb/in^2$ -sec **Bed Loading** 25 psid Injector Pressure Drop 4:1 Nozzle Area Ratio

Chamber Configuration

Predicted Ammonia Dissociation

Catalyst Bed Diameter

Catalyst Bed Length

Catalyst Type

Chamber Material

Nozzle Throat Diameter

3.470 in

2.0 in

0.2 in 25-30 mesh
1.8 in 1/8" x 1/8" pellets

Haynes Alloy No. 25

0.602 in

60%

Injector Configuration

Injector Type Showerhead

Number of Orifices 60

Orifice Diameter 0.0176 in

TABLE XVIII

∢
DAT
TEST
ENGINE
₫
8
Ö
SUMMARY

(3) Response Time	ě	99	999	8	909	455	495
(S) Thrust Coefficien		1,2005	1,2199	1.2468	1.2488	1,2542	1,2653
(6) Ammonia Dissociation	mole %	;	:	!	ţ	62.5	62.9
Catalyst Bed Pressure Drop	psid	29.0	31.6	33.0	33.9	8,48	32.8
Chamber Pressure Roughness P							
(5) Specific Impulse	lbf-sec/lbm	158.60	160.52	164.09	164.75	165.89	166.72
Characteristic Velocity	ft/sec	4250	4233	4234	4244	4255	4239
(4) Decay Time	Ě	29	S	ß	8	አ	, 8 8
(2) Ignition Delay	Ĕ	8	8	<u>\$</u>	8	82	61
Exit Gas Temperature	oF.	1772	1620	1595	1556	1601	1887
(1) Flowrate	lbm/sec	0.35121	0.36507	0,40222	0,41457	0,42317	0.42885
Thrust	IPĘ	55.7	9'85	0.99	6.89	70.2	71.5
Downstream Chamber Pressure		•					
Initial Catalyst Temperature	ያ-	7.3	6.5	69	88	7.3	2
Test No.		470	[2]	47.2	473	474	47.5

(1) Average of two flowmeters in series

(2) Time from propellant entry into chamber to 1% of steady state chamber pressure

(3) Time from propellant entry into chamber to 90% of steady state chamber pressure
(4) Time from chamber pressure start decay to 10% of steady state chamber pressure
(5) Sea level conditions at expansion ratio of 4:1
(6) Average value determined from ammonia to hydrogen and ammonia to nitrogen mole ratios

	٠			
			•	
	-			
-				
		-		

10.0 FLIGHTWEIGHT 5 lbf ENGINE

10.1 Design

The design of the flightweight 5 lbf engine was based on the results of the engine design criteria developed under Task I of the study. As described in Section 2.0, this engine was to be capable of pulse mode testing, throttling tests over a 10:1 thrust ratio, and tests with low freezing point propellant mixtures of hydrazine, hydrazinium nitrate and water. The design of the flightweight 5 lbf engine is shown in Figure 63. Pertinent reactor design parameters and estimated performance are summarized in Table XIX.

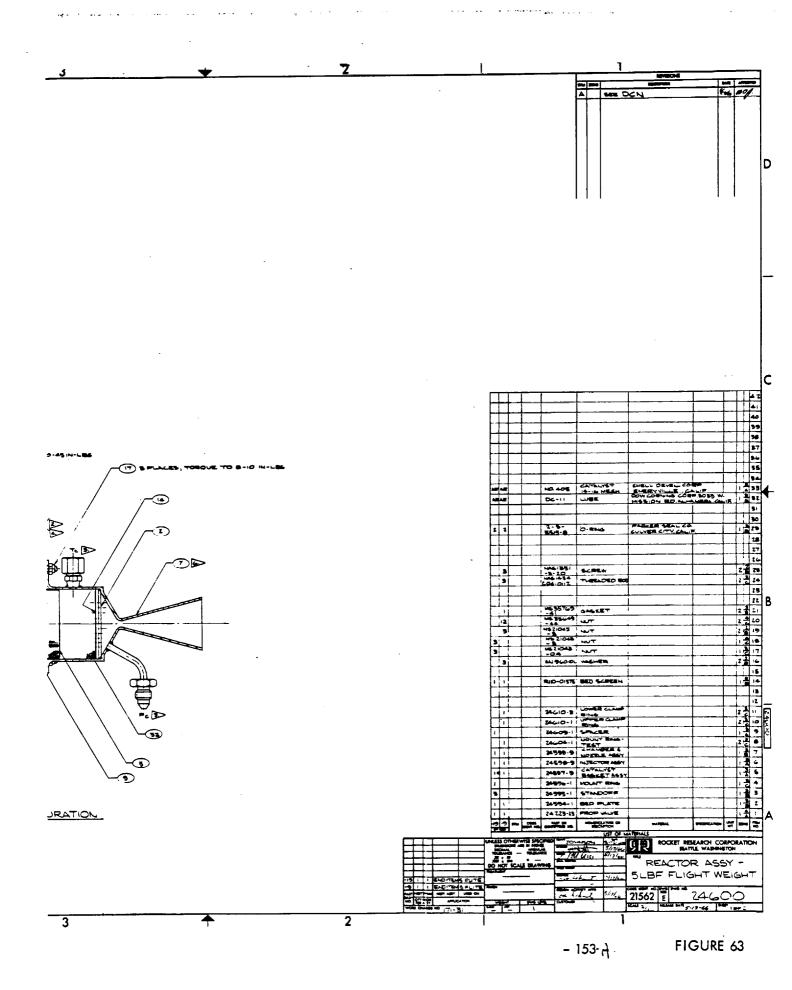
Significant design features of the engine design shown in Figure 63 are:

- Thermal standoffs between the injector and the propellant valve to provide thermal isolation between the chamber and the propellant valve.
- b. Propellant distribution by radial flow passages to each orifice which minimizes the propellant holdup and maintains adequate coolant velocities in the injector.
- c. A 0.3 inch deep 60 x 60 mesh molybdenum wire basket holding 25-30 mesh granular catalyst, in the upper part of the catalyst bed. The remainder of the catalyst bed is composed of 14-16 mesh granular catalyst.
- d. The nozzle of 50:1 expansion ratio and chamber are machined out of 347 stainless steel barstock.
- e. The engine is designed such that the injector can be flanged to the chamber and checkout firings conducted. A final meltdown weld of the chamber to injector is then performed following reactor acceptance tests.
- f. Differential thermal expansion between the thermal standoffs and the propellant feed tube is accommodated by the double "O"-ring seal on the propellant feed tube.
- g. The engine is mounted at the propellant valve thus minimizing heat input to mounting structure for possible flight applications and providing a propellant valve heat sink for maintenance of low valve seat temperatures under pulse mode, heat soak operating conditions.

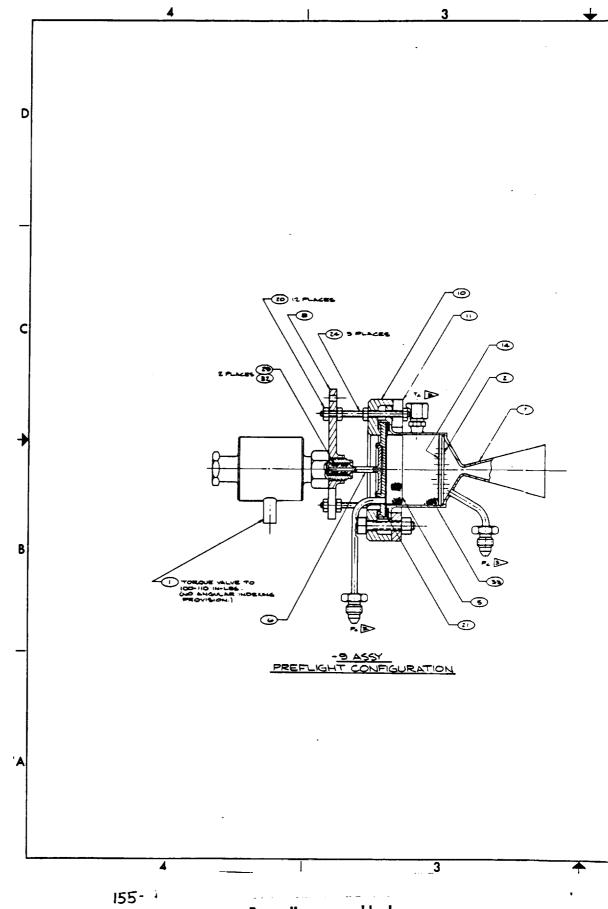
•			
			·
			÷
			•
•.			
	•		
	•		

Preceding page blank 153

		·
•		

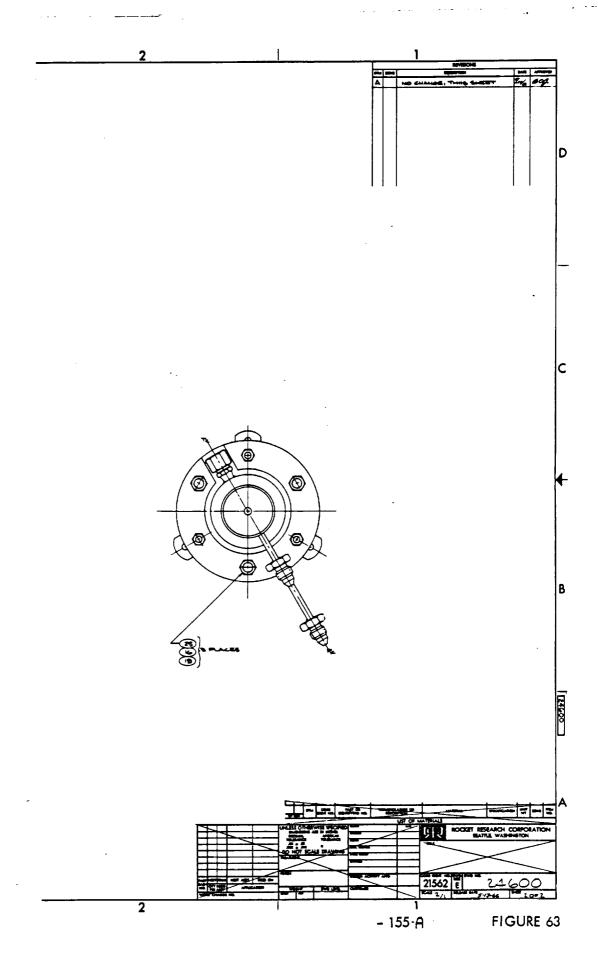


		•		



Preceding page blank

			-
		•	
		·	
		•	



•.			
	•		
		·	

TABLE XIX

5 lbf FLIGHTWEIGHT ENGINE DESIGN

Performance

retromatice	
Vacuum Thrust	5.0 lbf
Vacuum Specific Impulse	221.4 lbf-sec/lbm
Vacuum Thrust Coefficient	1.704
Characteristic Velocity	4180 ft/sec
Propellant Flow Rate	0.0227 lb/sec
Downstream Chamber Pressure	200 psia
Upstream Chamber Pressure	206 psia
Nozzle Area Ratio	50:1
Bed Loading	.015 lb/in ² -sec
Injector Pressure Drop	25 psid
Exhaust Gas Stagnation Temperature	1580°F
Chamber Operating Temperature	1600°F
Chamber Configuration	
Catalyst Bed Diameter	1.388 in.
Catalyst Bed Length	1.04 in.
Catalyst Type	0.3 inches 25–30 0.74 inches 14–16
Chamber Material	347 Stainless Steel
Chamber Safety Factor	1.5:1 at 300 psi
Engine Weight Breakdown	
Chamber and Nozzle	0.26 lbm
Injector	0.12 lbm
Thermal Standoffs	0.02 lbm
Valve Mounting Bracket	0.03 lbm
Catalyst	0.08 lbm
Total Engine Weight (less propellant valve)	0.41 lbm

h. The propellant valve can be removed and replaced without disassembly of the engine.

A photograph of the engine assembly is shown in Figure 64.

10.2 Low Freezing Point Propellant Mixture Tests

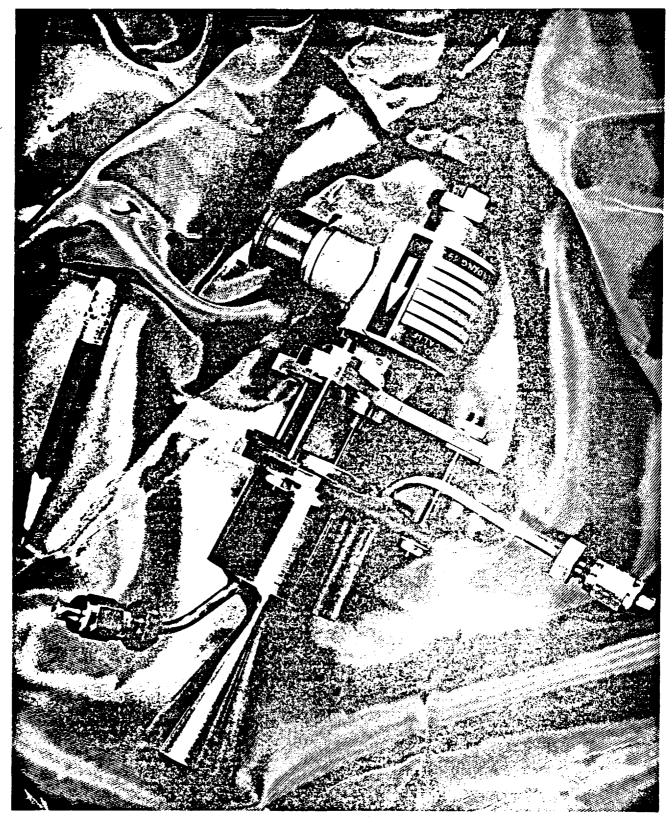
10.2.1 Propellant Selection

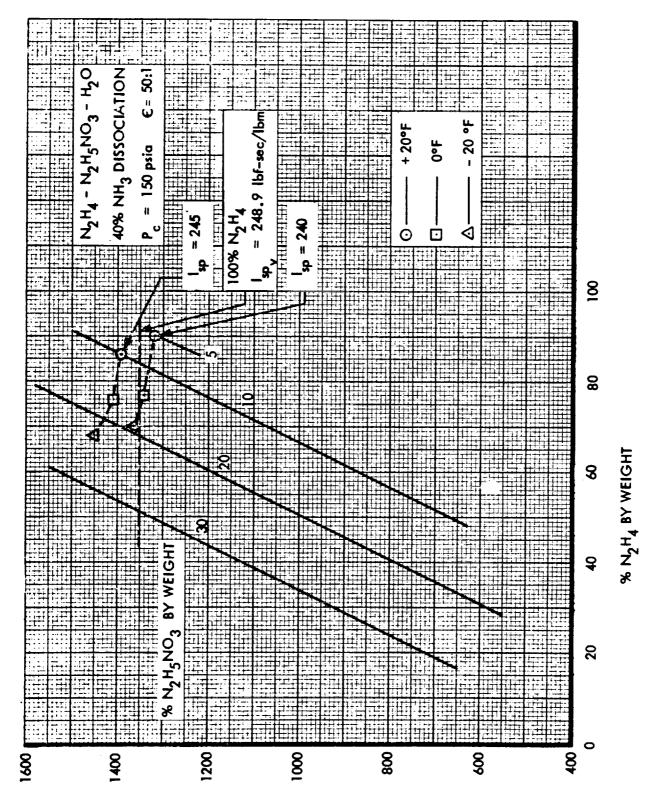
Three low freezing point propellant mixtures of hydrazine, hydrazine nitrate, and water which had freezing points of +20°F, 0°F, and -20°F were selected for study. The criteria for selection was that the theoretical flame temperature of the propellant mixture be no greater than that of neat hydrazine. A point of comparison at 40% ammonia dissociation was selected. At 40% ammonia dissociation neat hydrazine has a theoretical flame temperature of 1,355°K. Figure 65 is a plot of theoretical flame temperature versus the percent hydrazine in a mixture of hydrazine, hydrazinium nitrate, and water. Figure 66 is a ternary diagram of the hydrazine, hydrazinium nitrate, water propellant system. Lines of constant freezing point and vacuum specific impulse have been plotted on the diagram. The line of a constant vacuum specific impulse of 240 lbf-sec/lbm is plotted on Figure 65 for freezing point mixtures of +20°F, 0°F, and -20°F. This line falls very close to the theoretical flame temperature of neat hydrazine and mixtures falling on this line were selected for the propellant mixture tests.

The propellant mixtures were prepared by adding ammonium nitrate and water in the required quantities to hydrazine. The resulting ammonia in solution was removed by evacuating the propellant mixture, causing the ammonia to boil off. Table XX lists the desired and actual propellant mixtures as determined by chemical and analytical analysis.

10.2.2 Test Results

All propellant mixture tests were conducted at ambient temperature and pressure conditions. A flightweight engine with a sea level nozzle of 1.5:1 expansion ratio was utilized for the tests. Steady state tests of 30 seconds duration were conducted with the engine. Five (5) tests were conducted with the +20°F and 0°F freezing point propellant mixtures and four (4) tests were conducted with the -20°F propellant mixture.





CHAMBER TEMPERATURE (°K)

HYDRAZINE-HYDRAZINE NITRATE – WATER TERNARY DIAGRAM SHOWING FREEZING POINT AND VACUUM SPECIFIC IMPULSE

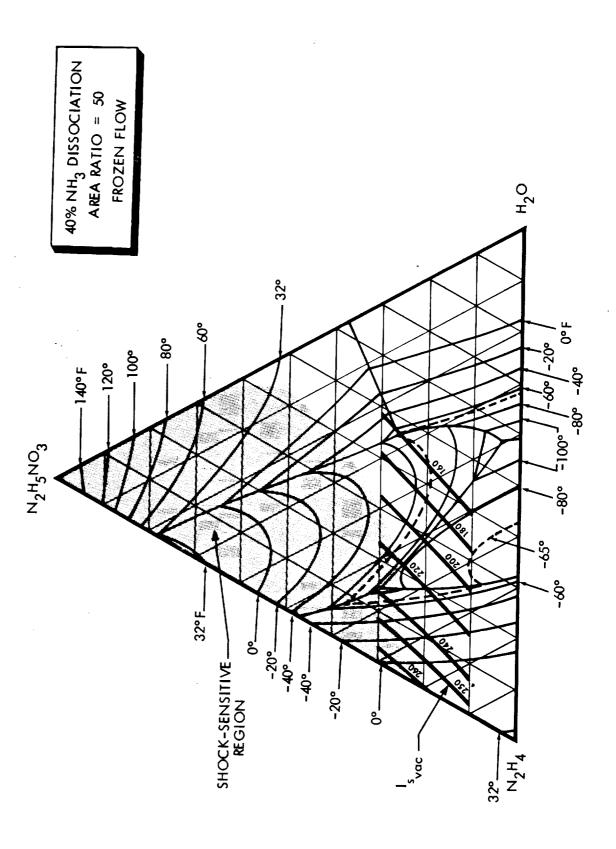


TABLE XX LOW FREEZING POINT PROPELLANT MIXTURES

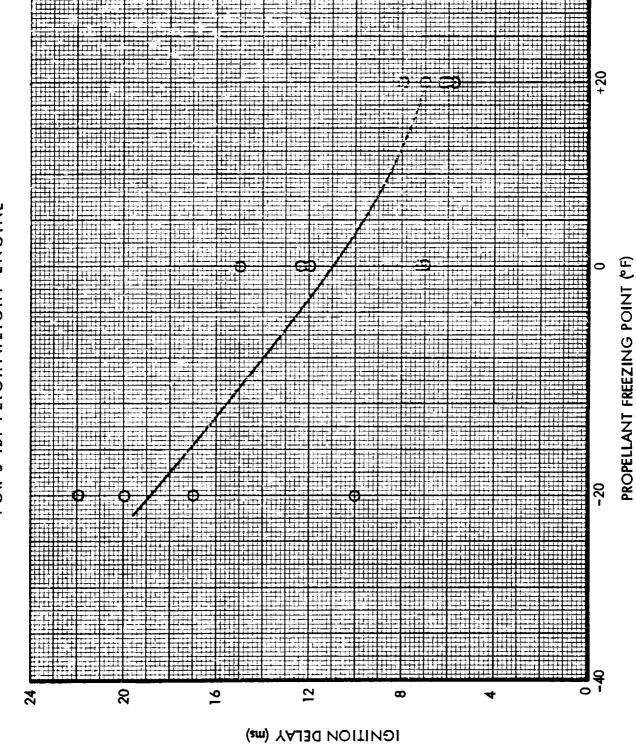
	+ 20°F Mixture	
	Desired	Actual
Hydrazine	89.0%	87.18%
Hydrazine Nitrate	9.0%	9.01%
Water	2.0%	3.15%
Ammonia	0%	0.66%
	0°F Mixture	
	Desired	Actual
Hydrazine	76.0%	75.14%
Hydrazine Nitrate	18.0%	17.87%
Water	6.0%	5.41%
Ammonia	0%	0.79%
	- 20°F Mixture	
	Desired	Actual
Hydrazine	69.0%	67.2%
Hydrazine Nitrate	23.0%	22.9%
Water	8.0%	9.0%
Ammonia	0%	0.9%

Data obtained from the testing is summarized in Table XXI.

Smooth start transient and steady state operation were achieved during all tests. No significant engine performance difference was noted between the three propellant mixtures. Characteristic velocity averaged 4,189 ft/sec for the 14 tests conducted which is virtually identical to the predicted value of 4,180 ft/sec. Two major trends were noted in the test data. Ignition delay times and chamber pressure roughness both increased slightly as the propellant freezing point was lowered. This trend is shown in Figures 67 and 68 wherein ignition delay times and chamber pressure roughness are plotted versus the propellant freezing point.

Pre- and post test catalyst bed weights were virtually identical with no indication of any catalyst loss during the tests of 420 seconds total test duration.

IGNITION DELAY TIME VS PROPELLANT FREEZING POINT FOR 5 16F FLIGHTWEIGHT ENGINE



± 2

(PERCENT PEAK-TO-PEAK)

PROPELLANT FREEZING POINT (°F)

-20

PROPELLANT FREE FOR 5 1bf FLIGHTWEI

CHAMBER PRESSURE ROUGHNESS
VS
PROPELLANT FREEZING POINT
FOR
5 1bf FLIGHTWEIGHT ENGINE

TABLE XXI

SUMMARY OF 5 IM FLIGHTWEIGHT ENGINE PROPELLANT MIXTURE TESTS

Chamber	Roughness	% peak-to-peak	+2.1	•	+ 1.0	0,1+	0.1+	6.1+	6+	+ 2,0	+ 1.2	+2.9	+ 3.0	+2.4	0 6 +	; + ; ; + ;
C, (5)	-		1,250	1,251	1,234	1,239	1,241	1,243	1.249	1.239	1.238	1,245	1.241	1,236	1,241	1,225
(5)		2	164.9													
	٠,	ft/sec	4243	4145	4217	4198	4181	4170	4161	4196	4194	4230	4162	4182	4172	4208
₹)	Thrust Flowrate	lbf lbm/sec	3,980 0,02414	3.740 0,02321	3.710 0.02299	3,750 0,02324	3.745 0.02322	3,760 0,02337	3,740 0,02319	3,710 0,02294	3,735 0,02313	3.730 0.02279	3.725 0.02328	3,710 0.02310	3.685 0.02290	3,540 0,02209
Downstream Chamber	Pressure	psia	214.5	201.5	202.5	204.3	203.3	204.1	202.1	7.102	203.1	501.9	202.3	202.3	200.1	194,7
Upstream Chamber	Pressure	psio	217.5	206.7	206.3	507.9	506.9	208.1	205.7	205.1	206.5	205.8	205.3	205.5	206.1	1.8.1
(3) · Response	Time	žĒ	545	220	450	250	520	490	435	480	250	287	270	99	515	710
(2) Response	Tine	Ē	195	195	175	202	200	2	0/1	15	17.5	222	235	235	185	230
(gairion	Deloy	Ē	•	•0	•	7	6 0	7	7	12	15	12	2	8	11	8
Fuel	Temperature	<u>.</u>	79	8	88	83	99.	2	જ	65	88	ß	\$	63	65	\$9
Initial Catalyst Bed																
Propellant Freezing	Point	<u>.</u>	+20	2	Q	£	Ŗ	0	0	0	0	0	.	Ŗ	Ŗ	-20
7 20 156 17 18 18			456	457	458	426	9	. 5	462	£63	\$	465	\$	79	4 68	69

Time from propellant entry into chamber to 1% of steady state chamber pressure
 Time from propellant entry into chamber to 80% of steady state chamber pressure
 Time from propellant entry into chamber to 90% of steady state chamber pressure
 Average of two flowmeters in series
 Sea level conditions at expansion ratio of 1,5:1